

A Methodology to Identify the Most Promising Concentrating Solar Power Layouts to be Integrated with Supercritical CO₂ Power Cycles

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ABSTRACT

The integration of compact and high-efficient supercritical CO₂ (sCO₂) power blocks has been identified as one of the key alternatives for enhancing the economic viability, and the flexibility of Concentrating Solar Power (CSP) plants. The present work aims at identifying and selecting the most promising CSP plant configurations that can be integrated with sCO₂ power blocks. Several sCO₂ – CSP layouts are identified, classified by the receiver heat transfer fluid and storage design, and benchmarked through a methodology developed by the authors. An analytical approach, based on purposely defined techno-economic criteria, is defined to benchmark each layout with an overall score. The following criteria are considered: maturity, low-cost potential, maximum temperature, safety, and system complexity. The overall score is then derived by combining the mentioned criteria and weighting factors. A comparative analysis is proposed, in which the higher the resulting overall score, the more attractive the layout was deemed. The CSP layout employing molten salts results in being the most attractive one, standing out for its maturity. The air- or particle-based configurations combined with packed beds or particle silos as storage are promising for their low-cost potential and high operating temperatures.

INTRODUCTION

The integration of compact and high-efficient sCO₂ power blocks can boost the CSP deployment by increasing the overall thermal efficiency and reducing costs [1]. A possible outline of the next generation of CSP systems is the state-of-the-art molten salt solar tower coupled with a sCO₂ power block as shown in Figure 1. Due to the industry experience, operating flexibility, and energy-storage efficiency, this configuration is a leading contender. However, owing to molten salt's decomposition around 580 °C, new development of advanced heat transfer fluids and storage technologies are necessary to evolve to higher temperatures to be able to reach thermal efficiencies superior to 50%. The present work introduces a novel methodology to identify and select the most promising CSP plant configurations that can be integrated with sCO₂ power blocks. Twenty-one sCO₂ – CSP layouts have been outlined and compared focusing on the receiver heat transfer fluid (HTF), and the storage technologies, while all layouts include a Brayton cycle with recompression and reheat. The considered HTFs are air, CO₂, molten salt, chloride salt, sodium, and particles. The storage designs included are molten salt tanks, chloride salt tanks, air/nitrogen/CO₂ packed- beds, encapsulated (or contained) Phase Change Materials (PCMs), thermochemical, and particle silos.

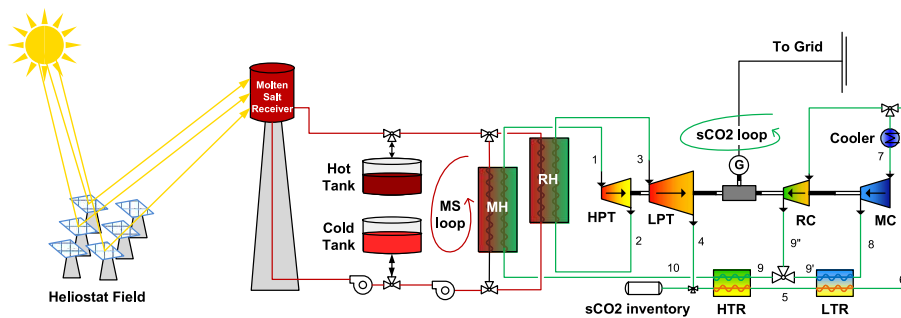


Figure 1: Schematic of the molten salt sCO₂-CSP layout

METHODOLOGY

To highlight the most promising layouts, an analytical approach, based on techno-economic criteria, has been built to benchmark each layout analyzed with an overall score (between 1 and 5). The higher the overall score, the more attractive will be the layout under investigation. Figure 2 shows the methodology developed to benchmark and support the selection of the 3 best configurations. Five scores are defined for each layout, namely the maturity score (S_{mat}), the potential low-cost score (S_{cost}), the safety score (S_{safe}), the complexity score (S_{comp}), and the maximum temperature score (S_{temp}). The overall score (S_o) can be calculated as the weighted average between all the aforementioned scores:

$$S_o = S_{mat} \cdot w_{mat} + S_{cost} \cdot w_{cost} + S_{safe} \cdot w_{safe} + S_{comp} \cdot w_{comp} + S_{temp} \cdot w_{temp} \quad (1)$$

where w_i indicates the weight for each score. The choice of the set of weights represents a key factor in the definition of the overall score and strongly influences the classification of the layouts. Therefore, for this purpose, three different weight combinations are considered and reported in Table 1. In this approach, maturity and cost are prioritized to guide the selection of the best CSP+sCO₂ system layouts. The combination Cost/Maturity represents the average between the combinations *Best for Maturity* and *Best for Cost*.

Table 1: Weight combinations for the overall score calculation

	Best for Maturity	Cost/Maturity	Best for Cost
Maturity Weight	0.5	0.4	0.3
Cost Weight	0.3	0.4	0.5
Temperature Weight	0.05	0.05	0.05
Safety Weight	0.1	0.1	0.1
Complexity Weight	0.05	0.050	0.050

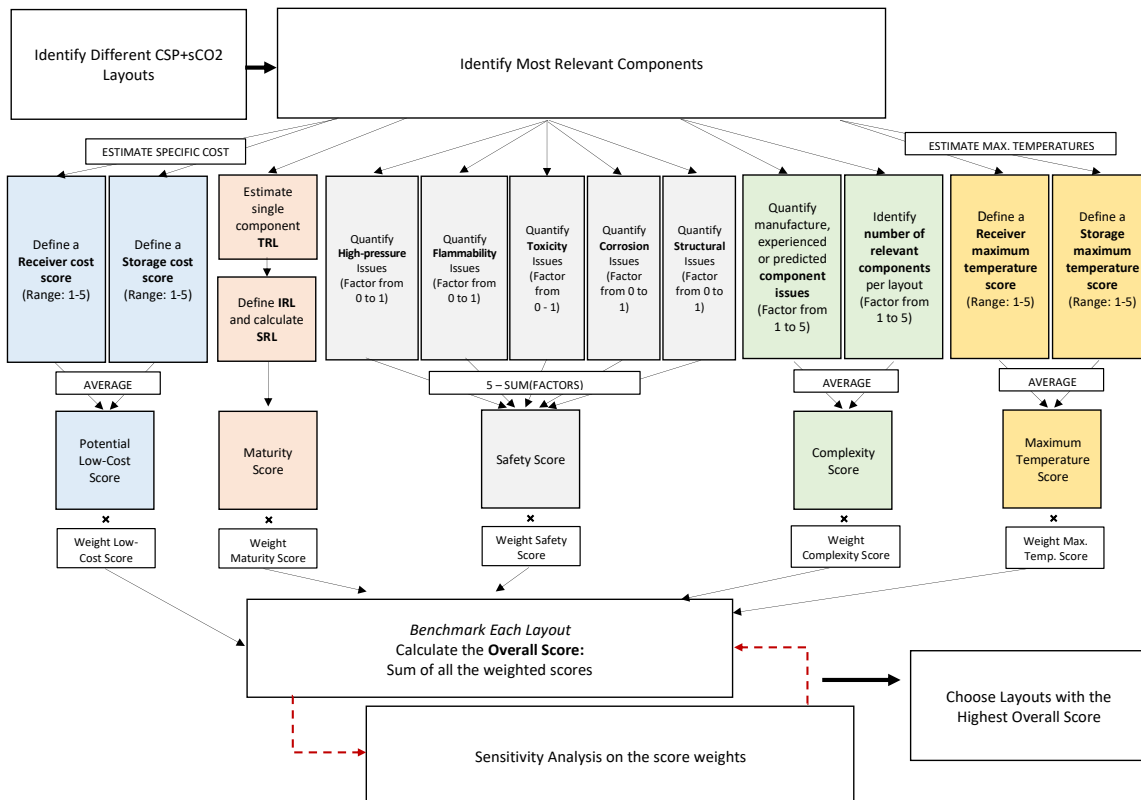


Figure 2: Schematic representation of layout selection methodology

The potential low-cost score (S_{cost}) is defined to compare the set of CSP+sCO₂ layouts based on their expected capital expenditure. The highest score corresponds to the cheapest system. Assuming comparable solar field layouts and having adopted identical power block configurations only the receiver and tower and storage subsystems are considered for comparing the different layouts. The receiver cost score and the storage cost score have been defined based on the subsystem costs identified in the literature and reported in Table 2. The cost score for the receiver and the storage subsystems is calculated as shown in Equation (2) and (3) based on the lowest and the highest specific cost values (c_{min} and c_{max}). The potential low-cost score is calculated as the average between the aforementioned scores.

$$S_{cost,REC} = \frac{4 \cdot (c_{REC} - c_{REC,max})}{c_{REC,min} - c_{REC,max}} + 1 \quad (2) \quad S_{cost,TES} = \frac{4 \cdot (c_{TES} - c_{TES,max})}{c_{TES,min} - c_{TES,max}} + 1 \quad (3)$$

The maturity of a system can be estimated by adopting the System Readiness Assessment (SRA) methodology [2]. The SRA approach defines the System Readiness Level (SRL), and it is based on the Technology Readiness Level (TRL) and the Integration Readiness Level (IRL) matrix. The TRL of the components has been estimated by the authors according to literature and coherently to the European Union (EU) TRL scale [3]. The assumed values are reported in Table 2, Table 3, and Table 4. The IRL is a metric to measure the integration maturity between two or more components. For a given system with n components, an IRL matrix ($n \times n$) is defined to consider the integration of the different components with each other. The IRL values ($IRL_{i,j}$) in the matrix range from 0 to 9, where zero is assigned for no integration between two specific components, while 9 is adopted for the integration of a component to itself ($IRL_{i,i}$).

The array of component SRL (SRL_c) is obtained by calculating the matrix product between the IRL and TRL and dividing each element by the number of integrations (m_i) of component i with every other component as shown in Equation (4). Each element of the array represents the readiness level of the component included in a specific system.

$$\begin{bmatrix} SRL_{c,1} \\ \vdots \\ SRL_{c,n} \end{bmatrix} = \begin{bmatrix} SRL_1/m_1 \\ \vdots \\ SRL_n/m_n \end{bmatrix} \text{ where } \begin{bmatrix} SRL_1 \\ \vdots \\ SRL_n \end{bmatrix} = \begin{bmatrix} IRL_{1,1} & \cdots & IRL_{1,n} \\ \vdots & \ddots & \vdots \\ IRL_{n,1} & \cdots & IRL_{n,n} \end{bmatrix} \times \begin{bmatrix} TRL_1 \\ \vdots \\ TRL_n \end{bmatrix} \quad (4)$$

Table 2: Assumptions for receiver and storage subsystems

	Type	TRL	Max T [°C]	Specific Cost [€/kW _e]	Toxicity	Flammability	High-pressure	Corrosion	Structural
Receiver/Tower	Molten Salt	9	600 [4]	128 [5]	0.10 [6]–[8]	0.00 [9]	0.00 [9]	0.25 [6]–[8]	0.00 [9]
	Air	6 [10]–[12]	1400 [9]	97 [1]	0.00	0.00	0.50	0.00	0.25
	Chloride Salt	3 [13]	800 [14]	205 [5]	0.25 [6]–[8]	0.00 [9]	0.00 [9]	1.00 [6]–[8]	0.00 [9]
	Sodium	6 [15]	850 [9]	199 [16]	0.25 [9]	1.00 [15]	0.00	0.25 [9]	0.00
	Particle	5 [17]	1000 [18]	105 [19]	0.00	0.00	0.00	0.00	0.25
	High-T CO ₂	3 [20]	1200 [9]	130 [1], [5]	0.00	0.00	0.50	0.50 [9]	0.25
	sCO ₂	2 [21], [22]	900 [9]	164 [5]	0.00	0.00	1.00	0.50 [9]	1.00 [23]
	Type	TRL	Max T [°C]	Specific Cost [€/kWh _e]	Toxicity	Flammability	High-pressure	Corrosion	Structural
Storage	Air Packed Bed	6 [24]	1000 [25]	8 [9]	0.00	0.00	0.80	0.00	0.30
	Moving Packed bed with particle bins	5 [5], [18]	1000 [9]	16 [19]	0.00	0.00	0.00	0.00	0.50 [18]
	Molten Salt Tanks	9 [24]	600 [9]	22 [5]	0.25 [26]	0.00	0.00	0.25 [26]	0.10 [26]
	Chloride Salt Tanks	4 [4]	800 [14]	52 [5]	0.25 [6]–[8]	0.00	0.00	1.00 [6]–[8]	0.25 [9]
	Nitrogen Packed Bed	6 [24]	1000 [25]	8 [9]	0.00	0.00	0.80	0.00	0.30
	CO ₂ Packed Bed	5	1000 [25]	8 [9]	0.00	0.00	1.00	0.50 [9]	1.00
	Phase-Change Material (PCM - AlSi)	4 [24]	600 [5]	33 [5]	0.00	0.00	0.00	1.00	0.50
	Thermochemical	5 [24]	600	67 [27]	0.25	0.00	0.00	0.25	0.50
	Particle Silos	6 [17]	1000 [9]	8 [9]	0.00	0.00	0.00	0.00	0.40

Table 3: Assumptions for the heat exchangers

Type	TRL	Complexity Factor	
Heat Exchangers	Molten Salts - sCO ₂	4	0.40
	Chloride Salts - sCO ₂	3	0.80
	Sodium - Chloride Salts	3 [16]	0.90 [16]
	Sodium - Nitrogen	1	0.80
	Sodium - CO ₂	1	0.80
	Particle - sCO ₂	3 [28], [29]	0.60 [17]
	Air - sCO ₂	4	0.40
	Sodium - sCO ₂	3	1.00
	Particle - Air	4 [18]	0.50 [30], [31]
	CO ₂ - sCO ₂	4	0.40
	Nitrogen - sCO ₂	4	0.40

Table 4: Assumptions for the other components

Type	TRL	Complexity Factor	
Other Components	Molten Salt EH	4 [32]	0.50
	Heliostats Field / PV	9	0.00
	Air/N Electric Heater	9 [9]	0.20 [9]
	CO ₂ Electric Heater	8	0.30
	Burner for sCO ₂	5	0.70
	Low/High Temp. Fan	9	0.00/0.25
	Molten Salts Pump	9	0.25
	Sodium Pump	6 [33]	0.60
	Chloride Salts Pump	4	1.00
	Particle lifting system	8 [17]	0.50 [17]
	sCO ₂ Power Block	4 [34], [35]	0.75

The SRL is calculated as the average of the component SRL values. The maturity score is calculated using Equation (5) identifying the SRL_{max} and SRL_{min} in the set of layouts analysed.

$$S_{mat} = \frac{4 \cdot (SRL - SRL_{min})}{SRL_{max} - SRL_{min}} + 1 \quad (5)$$

The safety score (S_{safe}) benchmarks a specific CSP+sCO₂ layout based on the safety issues. Five main safety concerns have been considered based on the media employed in the receiver and the storage: toxicity (f_{tox}), flammability (f_{flam}), high-pressures (f_{hp}), corrosion (f_{corr}), and structural concerns (f_{struc}). Each of these factors is calculated as the average between the two factors defined for the receiver and the storage, reported in Table 2. The higher the factor, the more critical is the problem related to the medium employed. The safety score is calculated as shown in Equation (6) and the higher the value, the safer is the configuration analyzed.

$$S_{safe} = 5 - \sum_{i=1}^5 f_i \quad (6)$$

The complexity of a configuration is defined based on the number of components per layout (number of components factor (f_{nc})) and the manufacturing issues and/or lack of experience for each component (component complexity factor (f_{cc})). On one side, the first factor is defined assuming that the higher the number of components (nc), the higher the complexity of the system, as well as the risk of failures (Equation (7)). On the other side, the components complexity factor is calculated as the average between all the component factors of the components employed in a specific system layout (Equation (8)). The assumed values for these factors are reported in Table 3 and Table 4. Therefore, the complexity score is calculated as shown in Equation (9).

$$f_{nc} = \frac{4 \cdot (nc - nc_{min})}{nc_{max} - nc_{min}} + 1 \quad (7) \quad f_{cc} = \frac{\sum_{i=1}^n \text{component factor}_i}{n} \quad (8) \quad S_{comp} = 5 - \frac{f_{nc} + f_{cc}}{2} \quad (9)$$

The maximum temperature score (S_{temp}) quantifies the potential energy-conversion efficiency that can be achieved by employing a specific receiver and/or storage type. The highest score corresponds to the highest temperature theoretically achievable in the two subsystems. For a given plant layout, the Receiver Temperature Score and the Storage Temperature Score have been defined based on the subsystem theoretical temperatures identified in the literature and reported in Table 2. The temperature scores are then calculated as shown in Equation (10) and (11) based on the lowest and the highest temperature values (T_{min} and T_{max}). The maximum temperature score is calculated as the average between the scores.

$$S_{temp,REC} = \frac{4 \cdot (T_{REC} - T_{REC,min})}{T_{REC,max} - T_{REC,min}} + 1 \quad (10) \quad S_{temp,TES} = \frac{4 \cdot (T_{TES} - T_{TES,min})}{T_{TES,max} - T_{TES,min}} + 1 \quad (11)$$

RESULTS AND DISCUSSIONS

A comparison between the proposed CSP+sCO₂ layouts and the selection of the most attractive ones is presented in this section. Figure 3 shows the maturity, potential-low cost, maximum temperature, safety, and system complexity scores for the configurations investigated classified by the receiver HTF. As expected, the point of strength of molten salt-based layouts is their maturity, while due to the limits on the medium chemical stability, they are characterized by the lowest maximum temperature score. Air-based systems coupled with packed-bed TES stand out for their potential low cost and the highest maximum temperature achievable, while their points of weakness are system complexity and low maturity. The layouts employing particles share the same weaknesses with the air-based layouts but they have been benchmarked as the safest and as low-cost systems. Sodium-based configurations have been classified as mature as particle-based systems, but more complex, with more safety issues, more expensive, and with lower operating temperatures. The configurations employing chloride salt and CO₂ as HTF in the receiver have been classified as the least mature in this analysis. Additionally, the chloride salt-based layouts are the most expensive configurations. The CO₂ systems stand out for their relatively high temperature and potentially low cost.

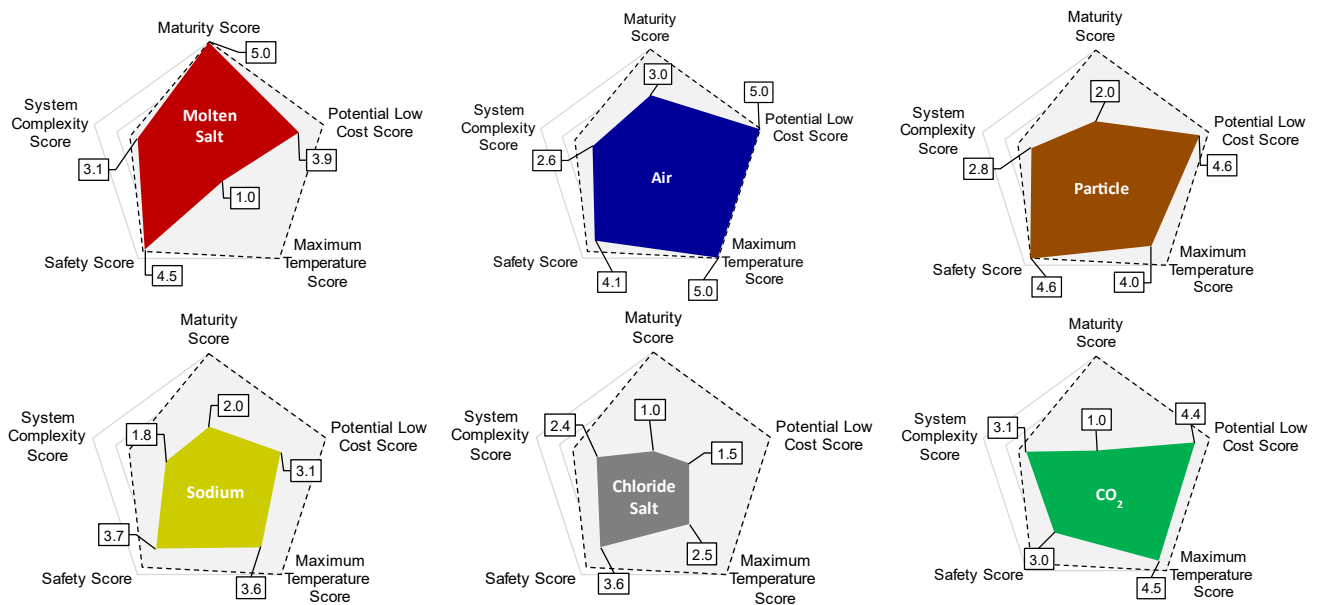


Figure 3: Intermediate scores of the layouts investigated classified by the receiver HTF

The intermediate scores have been combined in an overall score by using the three combinations of weights identified in the methodology: *Best for Maturity*, *Best for Cost*, and *Maturity/Cost*. Figure 4 shows the overall score values for the best layouts for each receiver heat transfer fluid as a function of the three considered weight combinations. The molten salt layout would be the most attractive one if maturity was prioritized, while the air-based systems would stand out if the cost was prioritized. Layouts employing particles reach the third-highest score regardless of the weights combinations. Comparing the sodium and CO₂ score values, sodium has a higher overall score if maturity is prioritized, otherwise, the opposite can be stated. The chloride salt is the least attractive configuration for the three combinations of weights.

The Maturity/Cost combination offers an average trend that takes into account the spread of the overall scores as a function of the two extreme weight combinations and it has been chosen to benchmark the proposed layouts. The overall scores of the layouts proposed in this analysis are presented in Figure 5, highlighting the share of each intermediate score.

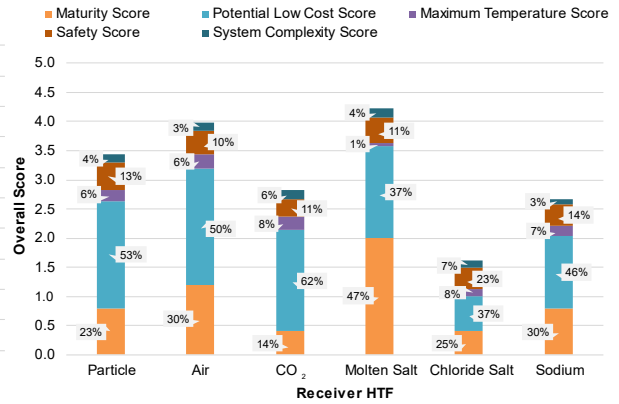
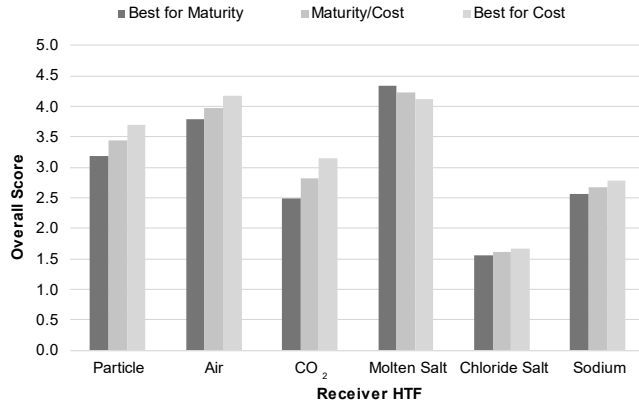


Figure 4: Sensitivity Analysis of the score weights Figure 5: Overall score breakdown - Maturity/Cost

Therefore, through the defined analytical approach, based on techno-economic criteria and the definition of an overall score for each layout investigated, the best three CSP+sCO₂ plant configurations have been selected. The molten salt layout has been identified as the most attractive configuration with the highest overall score equal to 4.2. This configuration is the closest to the state-of-the-art and it represents the first step towards a new generation of CSP plants. Air and particle layouts are the second and the third layout with the highest overall score, respectively equal to 4.0 and 3.8. They have similar shares for the potential low-cost score, while the air has a larger share for the maturity score (30% vs 23%). Air- and particle-based systems are the other two most attractive CSP+sCO₂ configurations that can drive towards a lower cost of electricity thanks to their lower costs and better energy performances. The low weight assigned to the temperature score implies that maturity and costs have been deliberately favored over efficiency. Consequently, the potential of the air- and particle-based systems, which have the highest operating temperatures, could have been underestimated. In addition, the circularity and the environmental impact of the systems in this analysis have been only partially included and limited to toxicity and flammability. Strengthening this criterion, particle systems would be favored, followed by air ones, which can leverage by the use of harmless and free HTF, and waste media in the TES.

CONCLUSIONS

In this work, a methodology to identify the most promising CSP layouts to be Integrated with sCO₂ power cycles has been introduced. Twenty-one sCO₂ – CSP connection layouts have been identified, classified by the receiver heat transfer fluid and storage design, and benchmarked with an overall score based on techno-economic criteria. Results show that the layout with a molten salt receiver and a double tank molten salt storage is the most attractive. This configuration stands out for its maturity and covers a gap between the state-of-the-art and the new generations of CSP plants. The main limitation of this layout is the relatively low maximum temperature that can be achieved by conventional molten salts. The other two most attractive configurations are the air- and particle-based systems including air packed bed or particles silos TES. The potential low cost and the maximum operating temperatures are the main drivers for these systems, that can enhance the economic competitiveness of CSP plants. Techno-economic models will be implemented for the most promising layouts identified in this study, including hybridization with PV field and with the grid to make the most of the TES included in the CSP plant.

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