



*7th International*  
Supercritical CO<sub>2</sub> Power Cycles Symposium  
San Antonio, TX U.S.A.  
February 21-24, 2022

# Design, Fabrication and Testing of Novel Compact Recuperators for the Supercritical Carbon Dioxide Brayton Power Cycle

Lalit Chordia, PhD, Vahid Vahdat, PhD, Marc Portnoff



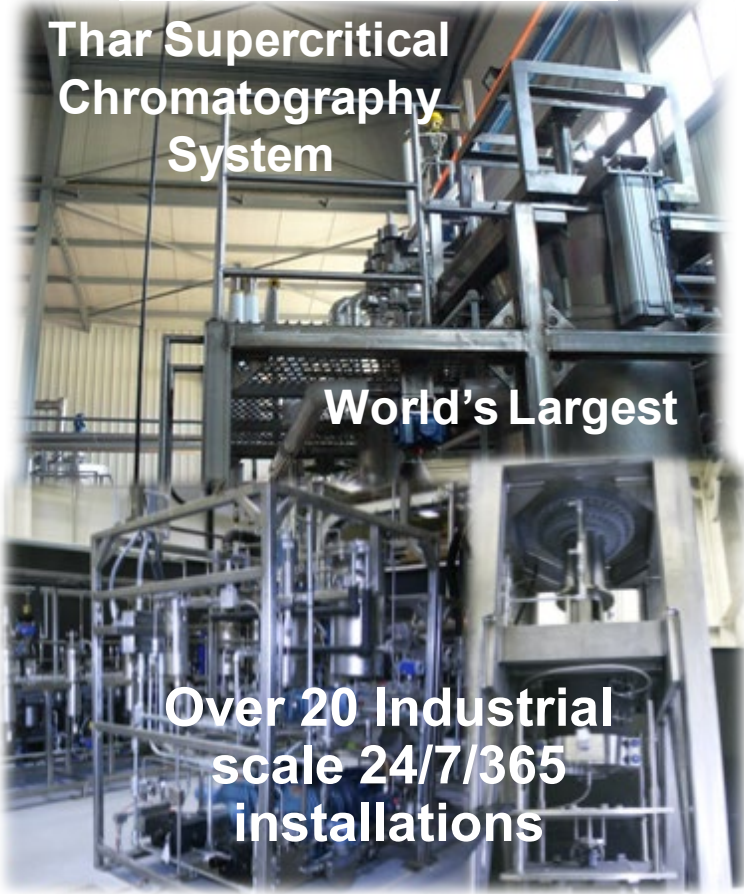
## Outline

- Introduction to **Thar Energy**
- **Stacked-Sheet Heat Exchanger (SSHX)**
  - Concept & Design Criteria
  - 3D printed SSHX (3D-SSHX)
  - Laser cut SSHX (Laser-SSHX)
- **sCO<sub>2</sub> Heat Exchanger Test Facility**
- **SSHX Test Data**
- **Summary**

## The Thar Brand - Over 30 years of Innovation with “Green” Supercritical Fluid Technologies

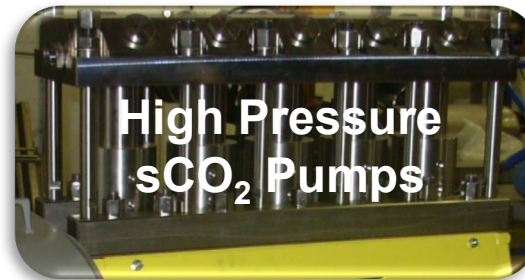
Design and commercialization of supercritical systems & major components

Thar Supercritical  
Chromatography  
System



World's Largest

Over 20 Industrial  
scale 24/7/365  
installations

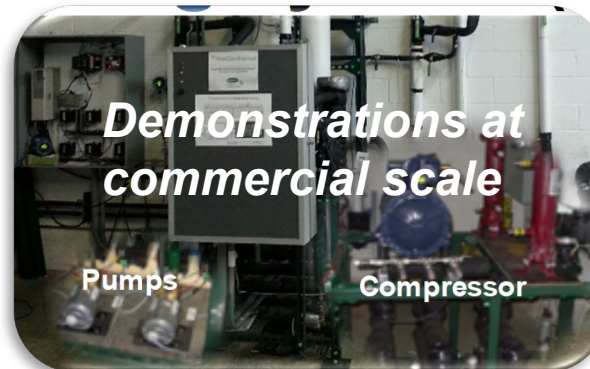


High Pressure  
sCO<sub>2</sub> Pumps



Over 5,000 scientific  
instruments installed

Direct Exchange, R744 (CO<sub>2</sub>)  
Geothermal Heating & Cooling



Demonstrations at  
commercial scale

Pumps

Compressor

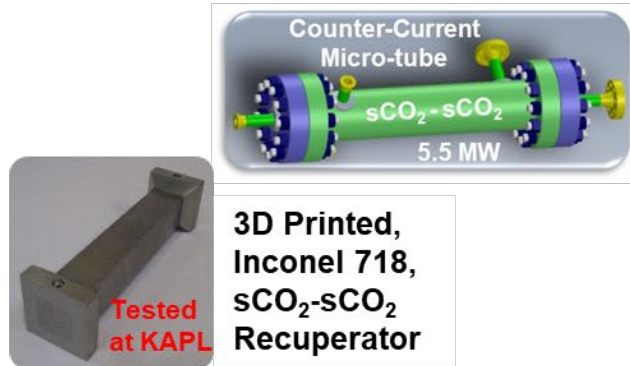


Heat  
Exchangers

### Timeline (recent past)

sCO<sub>2</sub> Brayton Power  
Cycle Development

**COMPACT** Heat Exchangers for sCO<sub>2</sub>  
Power Cycles



Design – Construct – Install  
**Primary Heater for Sunshot**  
One MWe sCO<sub>2</sub> Test Loop



Design – Construct – Operate  
**sCO<sub>2</sub> Heat Exchanger Test Loop**  
*Superior Thermal Performance Confirmed*



2014



Design – Construct –  
Operate Largest GMP  
sCO<sub>2</sub> Extraction  
System in USA

2015



2016

Oxy Combustion Test Facility  
Design – Construct – Operate  
Demonstrate auto-combustion



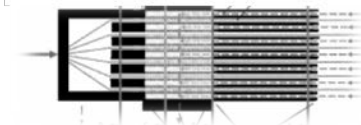
2017

UNITED STATES PATENT AND TRADEMARK OFFICE



Patent - Notice  
of Allowance

Counter Current Heat  
Exchanger/Reactor



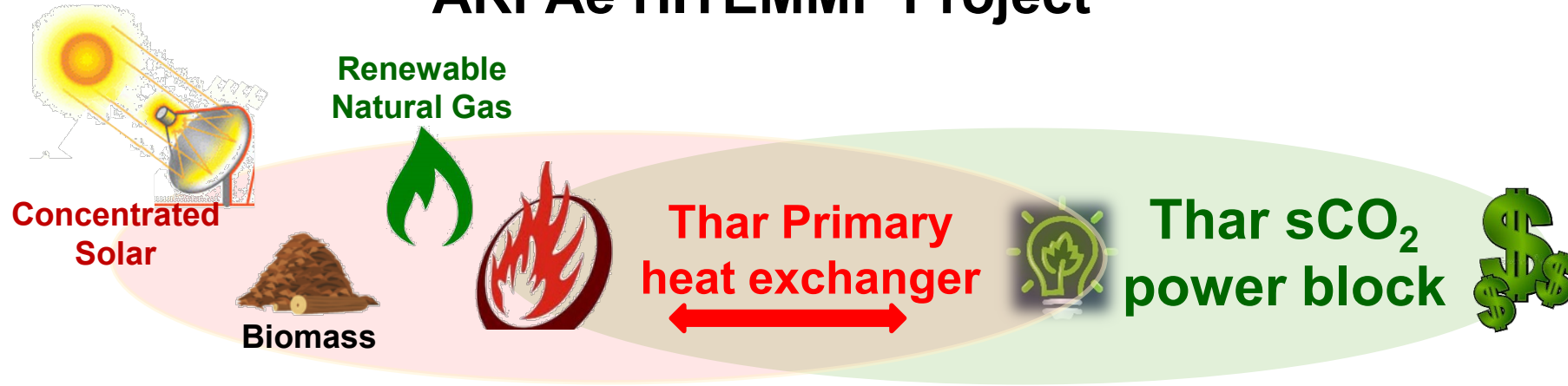
Thar  
Pharmaceuticals

sold to



Expands into Liquid Chromatography

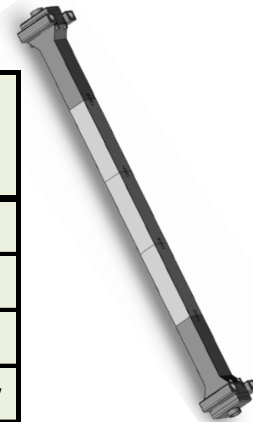
## ARPAe HITEMMP Project



**You bring the heat! We provide the power!**

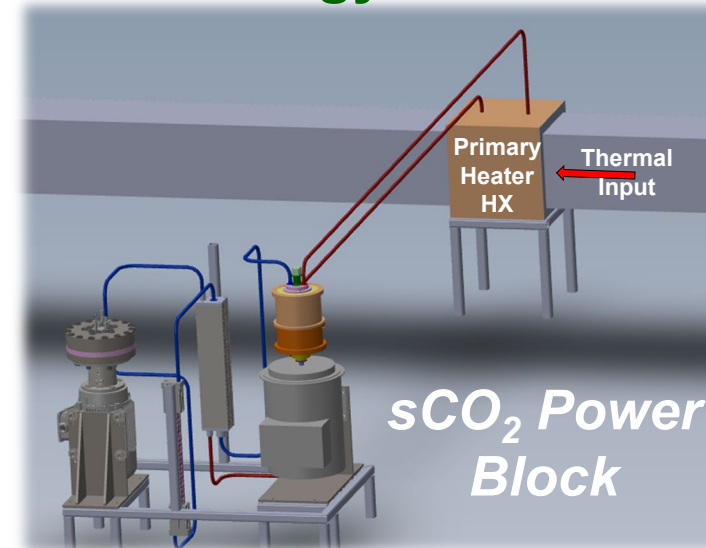
### > 800°C Recuperator

Criteria	ARPA-E Category A Target	Thar Project Goals
Thermal Effectiveness	≥ 80%	> 90%
Temperature Limit	≥ 800°C	> 800°C
Low Pressure	≥ 80 bar	≥ 80 bar
High Pressure	≥ 250 bar	≥ 300 bar
Pressure Loss	$\Delta P_h < 2\%$	$\Delta P_h < 2\%$
	$\Delta P_c < 2\%$	$\Delta P_c < 2\%$
Cost	\$2000/UA	< \$100/UA



Haynes 282  
y' strengthened  
Nickel Super-alloys

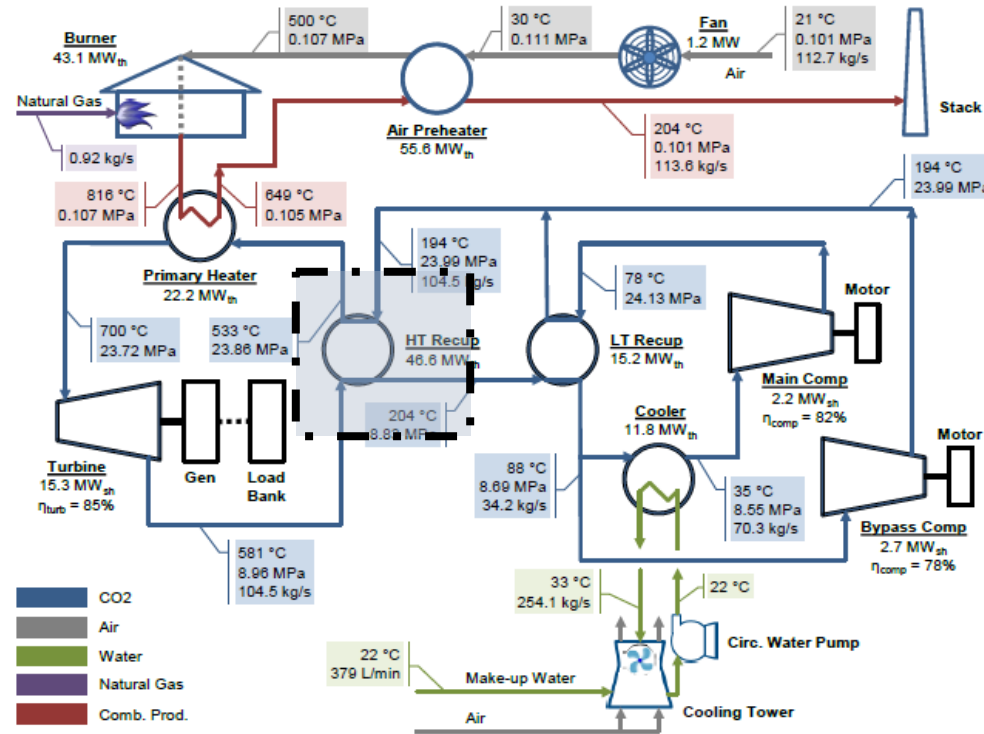
### Thar Energy's CHP sCO<sub>2</sub> Power Block



- **Efficient**  
Elec Efficiency: >45%  
CHP Efficiency: >70%
- **Modular & compact**
- **Low cost of ownership**
- **Reduced environmental impact**

## High Temperature Recuperator Design Criteria

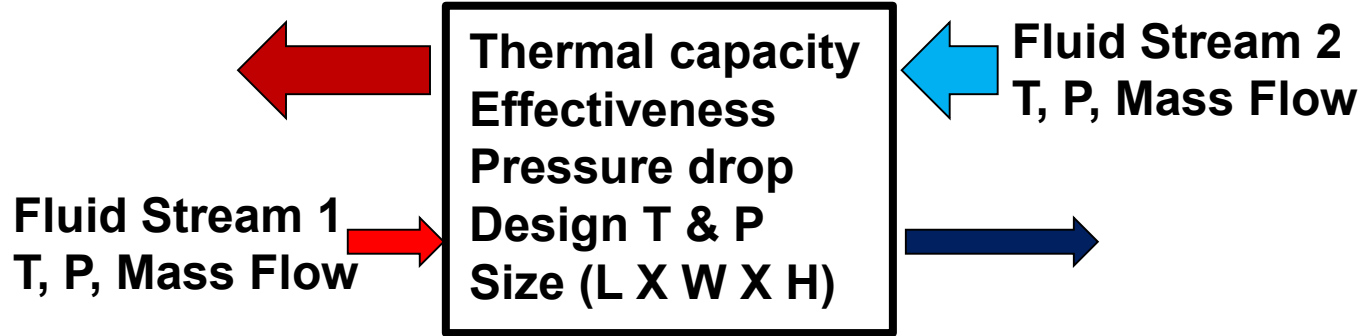
### STEP Conditions (2016)\*



Criteria	S.T.E.P. Target
Thermal Capacity	45.9 MWt
Thermal Effectiveness	97%
Pressure Loss	$\Delta P_h < 1.5\%$ $\Delta P_c < 0.6\%$
Temperature Limit	577°C
Differential Pressure	152 bar
Life	30,000 hr
Cost	< \$100 / kWt
Package Dimensions	8.8 x 3.6 x 2.6 m

\* Weiland, N, Updated Supercritical Transformational Electric Power (STEP) Cycle Conditions, NETL project communications, August 2016

## Recuperator Design



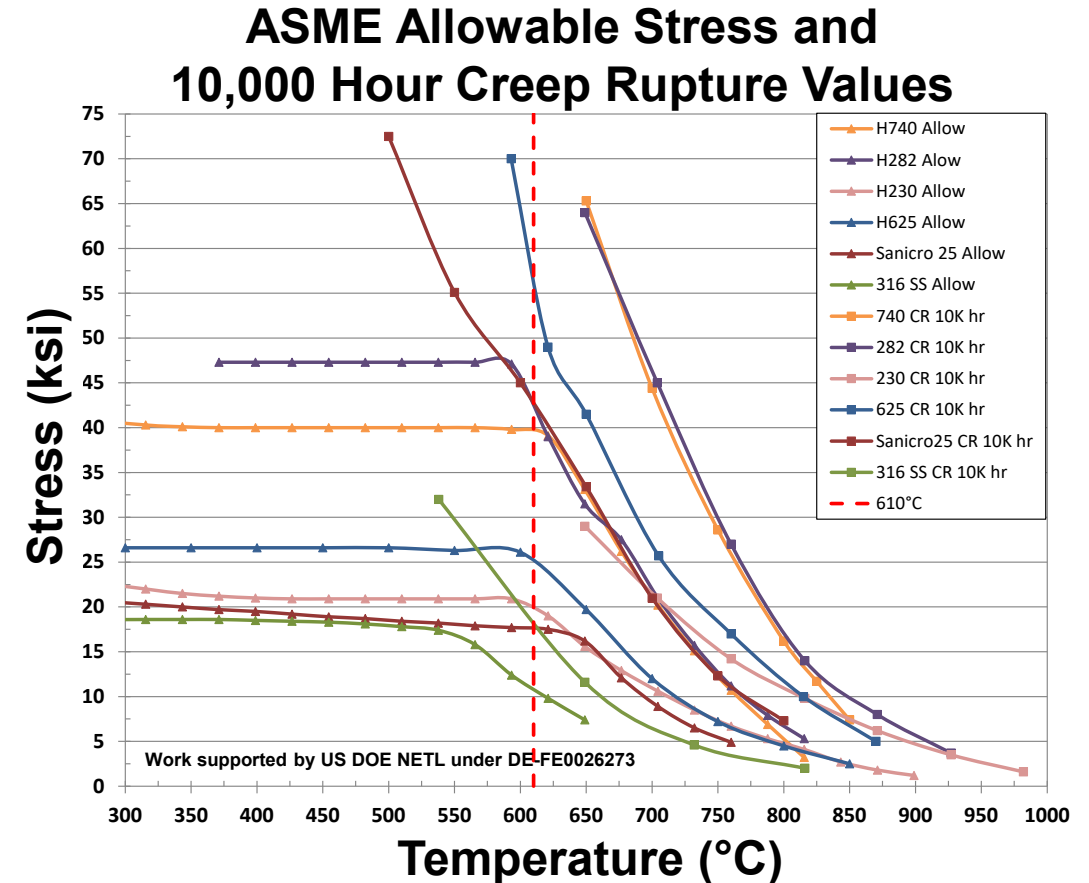
### Material of Construction

- Physical Properties
- Corrosion
- Contamination potential

### ASME Code Stamp/Design

### Fouling Factor

**Goal: Meet performance requirements and provide margin of safety while minimizing over design**



**Design T**



**\$**



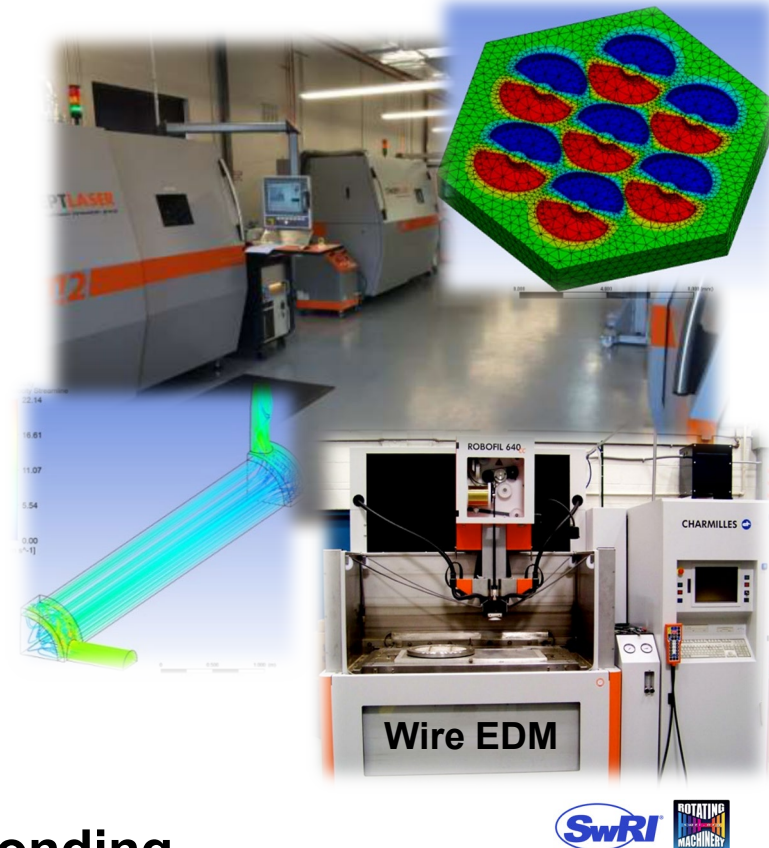
**As Design T increases, the material strength drops & corrosion rates increase**

## HTR Recuperator Concepts Engineering Analysis & Down Select

- Thermal-Hydraulic performance modeling and analysis
- Advanced manufacturing methods and tolerance
- Fabrication cost analysis

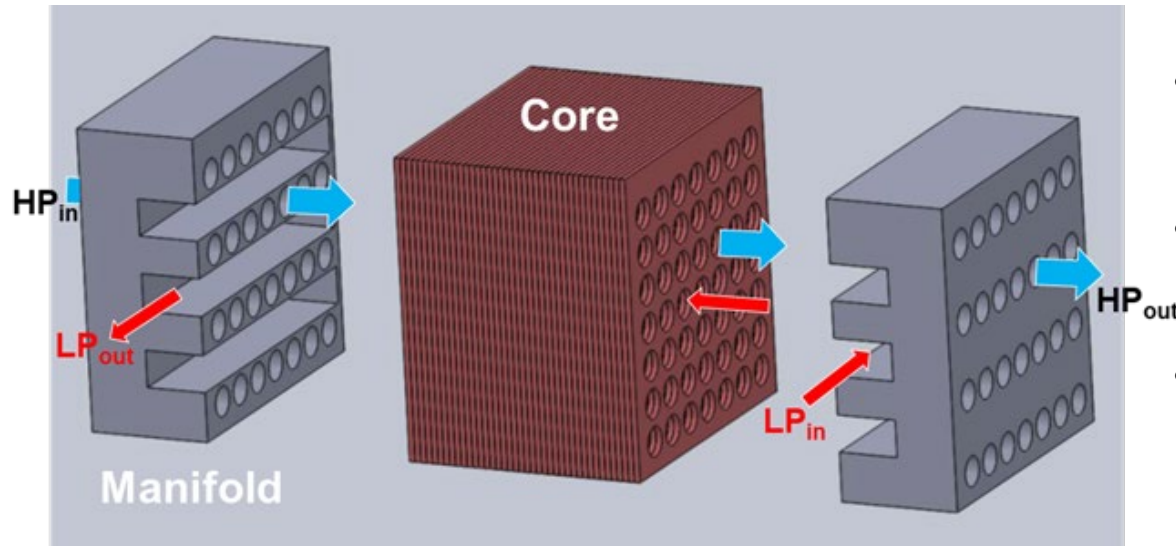
### *Subtractive vs. Additive Manufacturing*

- Laser cutting
- Laser welding
- Water jet cutting
- 3D metals printing
- Electrochemical etching
- Electrochemical machining (ECM)
- Electro discharge machining (EDM)
- EDM wire cutting
- Sheet bending/forming
- Metal plating
- Stamping
- Brazing
- Welding
- Diffusion bonding





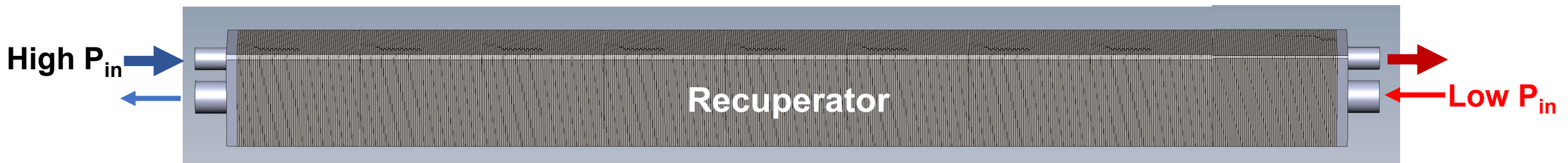
## Thar's Stacked Sheet Heat Exchanger (SSHX) Recuperator Concept



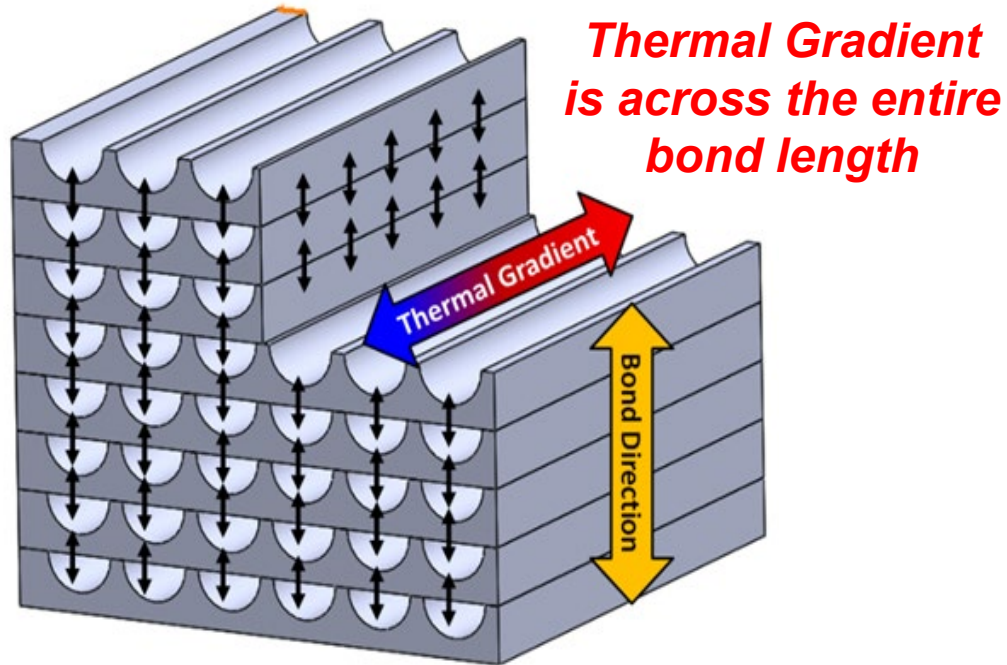
- Patterns cut, punched or etched into individual sheets
- Sheets are aligned, stacked and joined (brazed, diffusion bonded)
- Manifolds/headers are added to separate flow streams and ensure uniform flow distribution

***Opportunity for cost effective design enhancements***

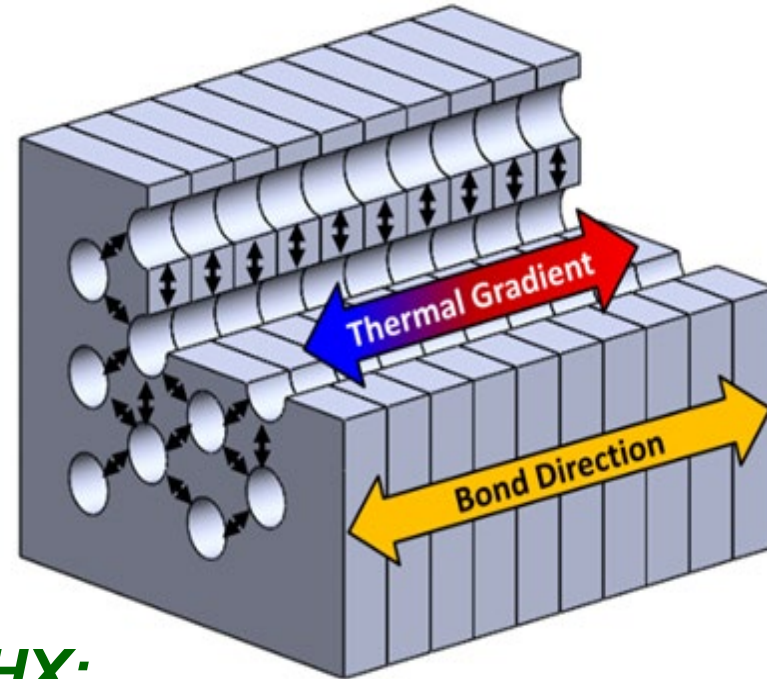
**Accommodates advances in Subtractive and/or Additive Manufacturing**



# Mechanical & Thermal Stress Analysis - Printed-Circuit HX vs. SSHX




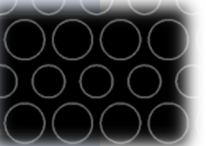
**Printed-Circuit HX:**  
The bond between sheets is: perpendicular to the mechanical stresses & parallel to the thermal stresses



**SSHX:**  
The bond between sheets is: parallel to the mechanical stresses & perpendicular to the thermal stresses

*Improves structural integrity and thermal compliance*

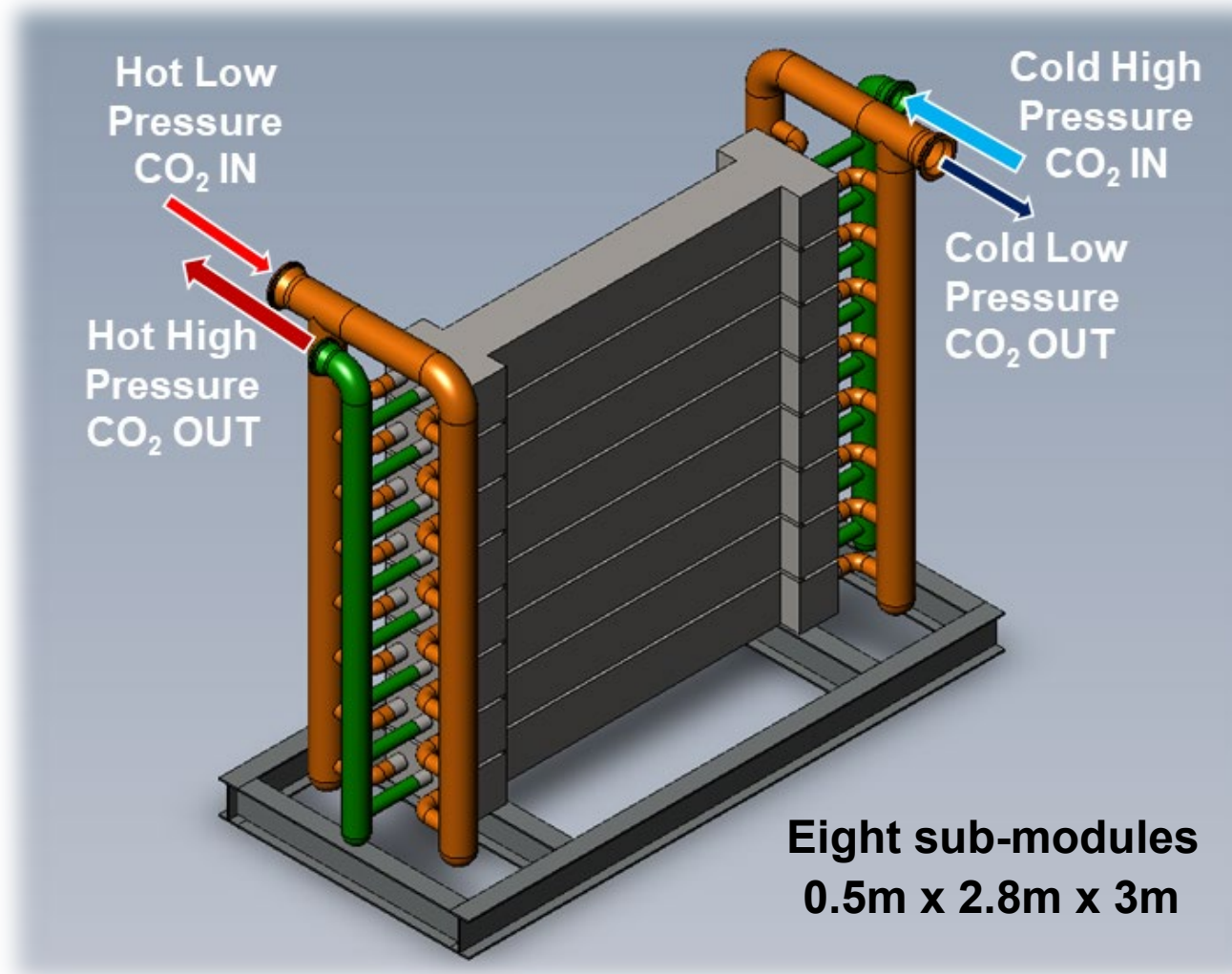
## Prototype Recuperators

Criteria	3D-SSHX Prototype	Laser-SSHX Prototype
Manufacturing Method	3D Printed	Laser Cut Sheets
Materials	Inconel 625	Stainless 347H
Channel Pattern	Circle-Star 	Circle-Circle 
Manifold Design	3D Printed	Laser Cut Sheets
Joining Method	Diffusion Braze	Diffusion Braze
Opacity	~46%	~73%

***Both methods passed hydro-tests***

## 46 MWt Laser-SSHX Recuperator

*Parallel Modular Design, Factory Fabricated*



**3D-SSHX**  
**57% volume**  
**decrease**

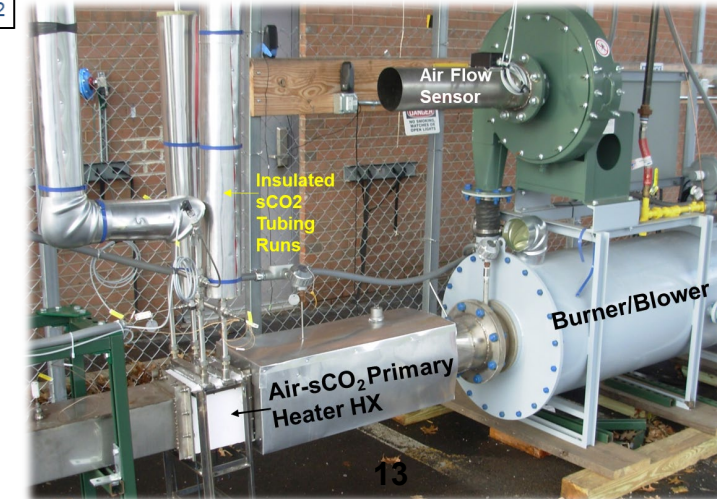
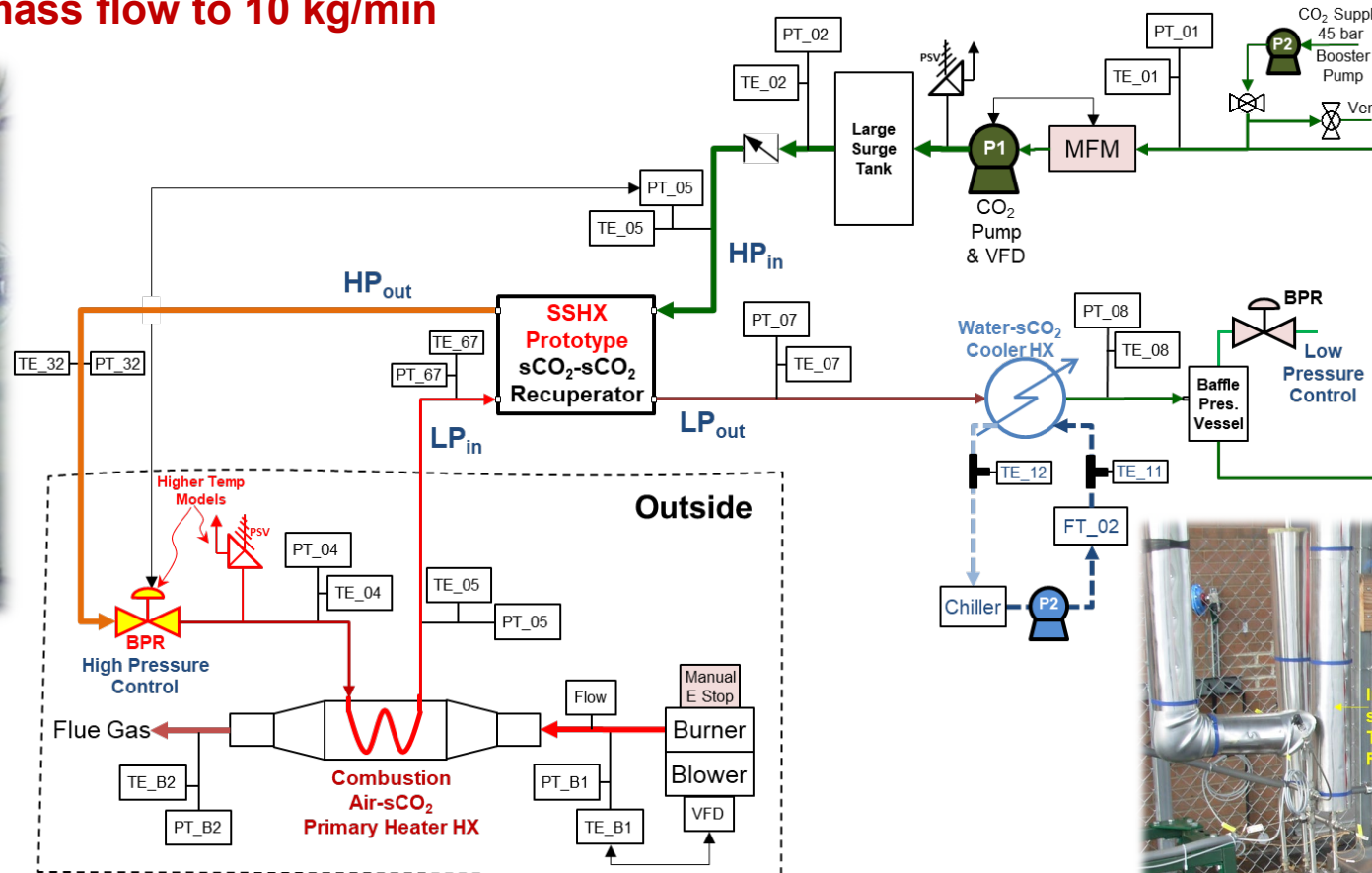
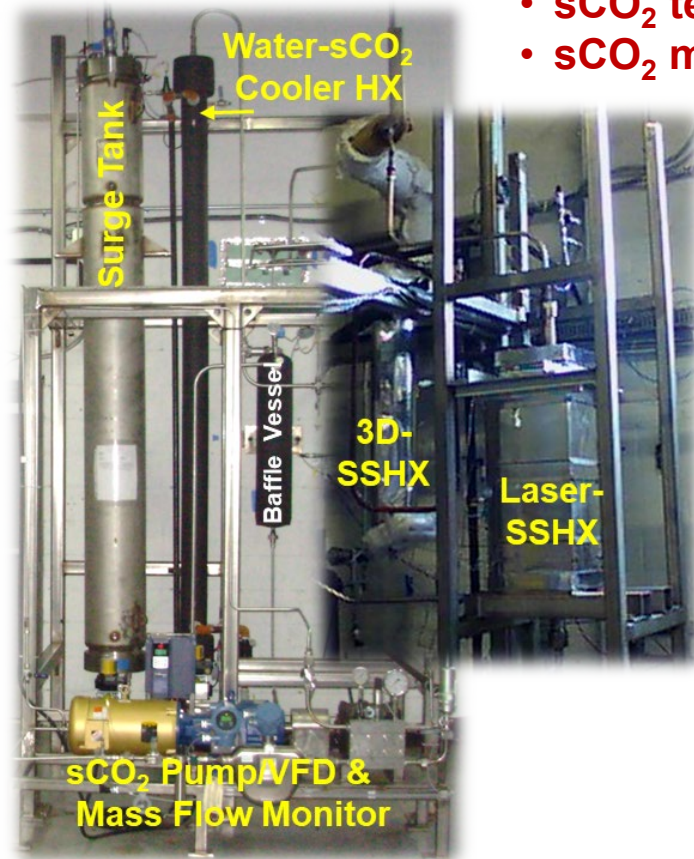
## sCO<sub>2</sub> Brayton Power Cycle Heat Exchanger Test Facility

### Reconfigurable Test Loop

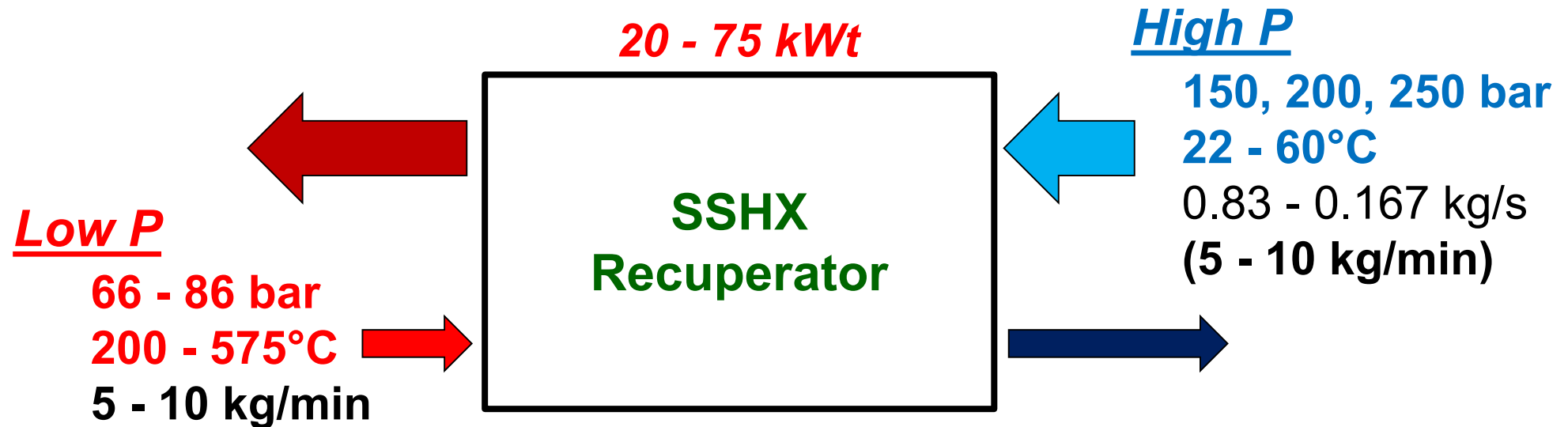
- sCO<sub>2</sub> pressures to 275 bar
- sCO<sub>2</sub> temperature to 700°C
- sCO<sub>2</sub> mass flow to 10 kg/min

### Simple Recuperated Cycle

High temperature valve in place of expander



## Test Conditions - SSHX Recuperator Prototypes



- Test thermal/hydraulic performance over a range of operating conditions
- Compare actual to predicted performance
- Rank prototypes by performance

## HX Model Heat Transfer Equations

Models selected from established heat transfer and pressure drop equations for the best accuracy compared to testing data

### 1 CO<sub>2</sub> Side Nusselt Number

Petukhov (1970)

$$Nu_{CO_2} = \frac{\left(\frac{f}{2}\right) \times Re \times Pr}{1.07 + \frac{900}{Re} - \frac{600}{1 + 10Pr} + 12.7 \left(\frac{f}{2}\right)^{\frac{1}{2}} (Pr^{\frac{2}{3}} - 1)}$$

### 2 Air Side Nusselt Number

Martin (2002)

$$Lq = \begin{cases} 0.92Hg \times Pr_{air}(i) \times \left(\frac{\frac{4X_T - 1}{\pi}}{X_L}\right) & X_L \geq 1 \\ 0.92Hg \times Pr_{air}(i) \times \left(\frac{\frac{4X_T X_L - 1}{\pi}}{X_L X_D}\right) & X_L < 1 \end{cases}$$

$$Nu_{air}(i) = 0.404 \times Lq^{\frac{1}{3}}$$

### 3 CO<sub>2</sub> Side Pressure Drop

Bhatti and Shah (1987)

$$f = 0.00128 + 0.1143Re^{-0.311}$$

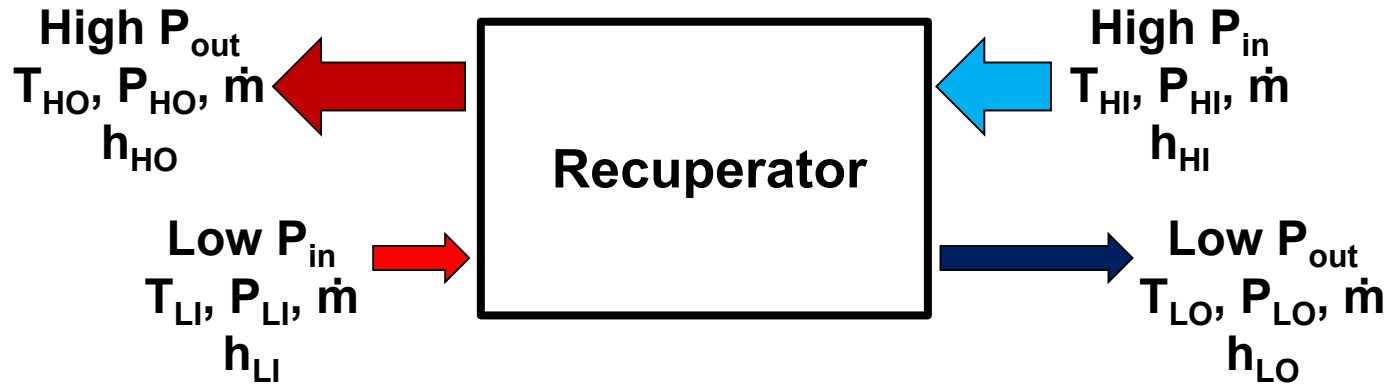
$$\Delta p_{CO_2} = f \frac{L}{d_o} \frac{\rho \mu^2}{2}$$

### 4 Air Side Pressure Drop

Zukauskas (1988)

$$\Delta p_{air} = N_r X \left(\frac{\rho u_m^2}{2}\right) f$$

## HX Performance Heat Transfer Equations



**Effectiveness,  $\epsilon = Q_{act} \div Q_{max}$**

$Q_{act} = \text{minimum}(Q_{HI-HO}, Q_{LI-LO})$

$Q_{HI-HO} = \dot{m} \times (h_{HO} - h_{HI})$

$Q_{LI-LO} = \dot{m} \times (h_{LI} - h_{LO})$

$Q_{max} = \text{minimum}(Q_{h\ max}, Q_{c\ max})$

$Q_{h\ max} = \dot{m} \times (h_{LI} - h(T_{HI}, P_{LO}))$

$Q_{c\ max} = \dot{m} \times (h(T_{LI}, P_{HO}) - h_{HI})$

**$UA = Q_{act} \div T_{Ln}$**

$T_{Ln} = (\Delta T_i - \Delta T_{ii}) \div LN(\Delta T_i \div \Delta T_{ii})$

$\Delta T_i = T_{LI} - T_{HO}$

$\Delta T_{ii} = T_{LO} - T_{HI}$

**Approach Temperature =  $T_{LO} - T_{HI}$**

**% Pressure Drop**

$\% \Delta P = (P_{in} - P_{out}) / P_{in}$

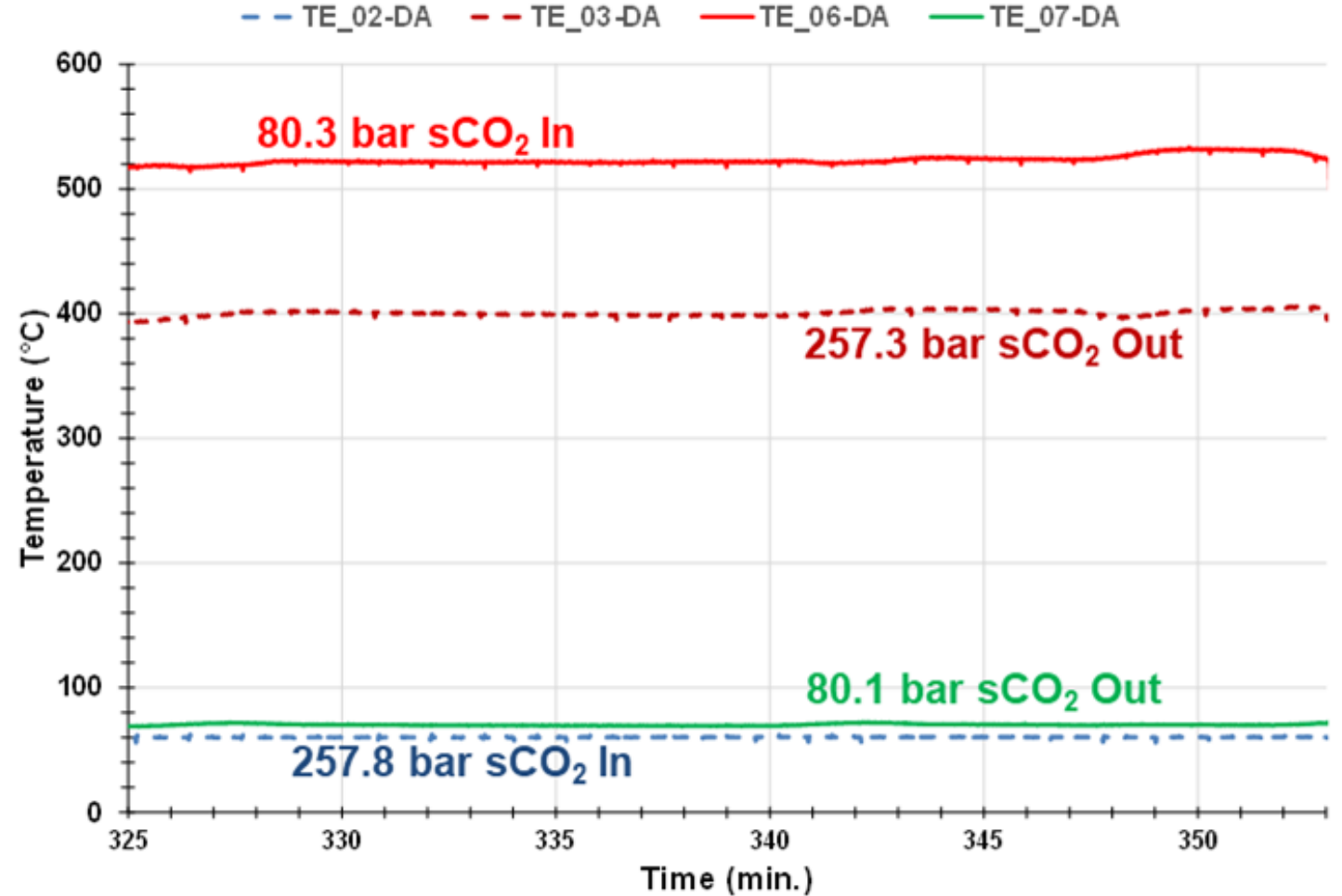


## Steady State Time vs. Temperature Plot

### Prototype SSHX Recuperators



### 3D-SSHX – Steady State Plot

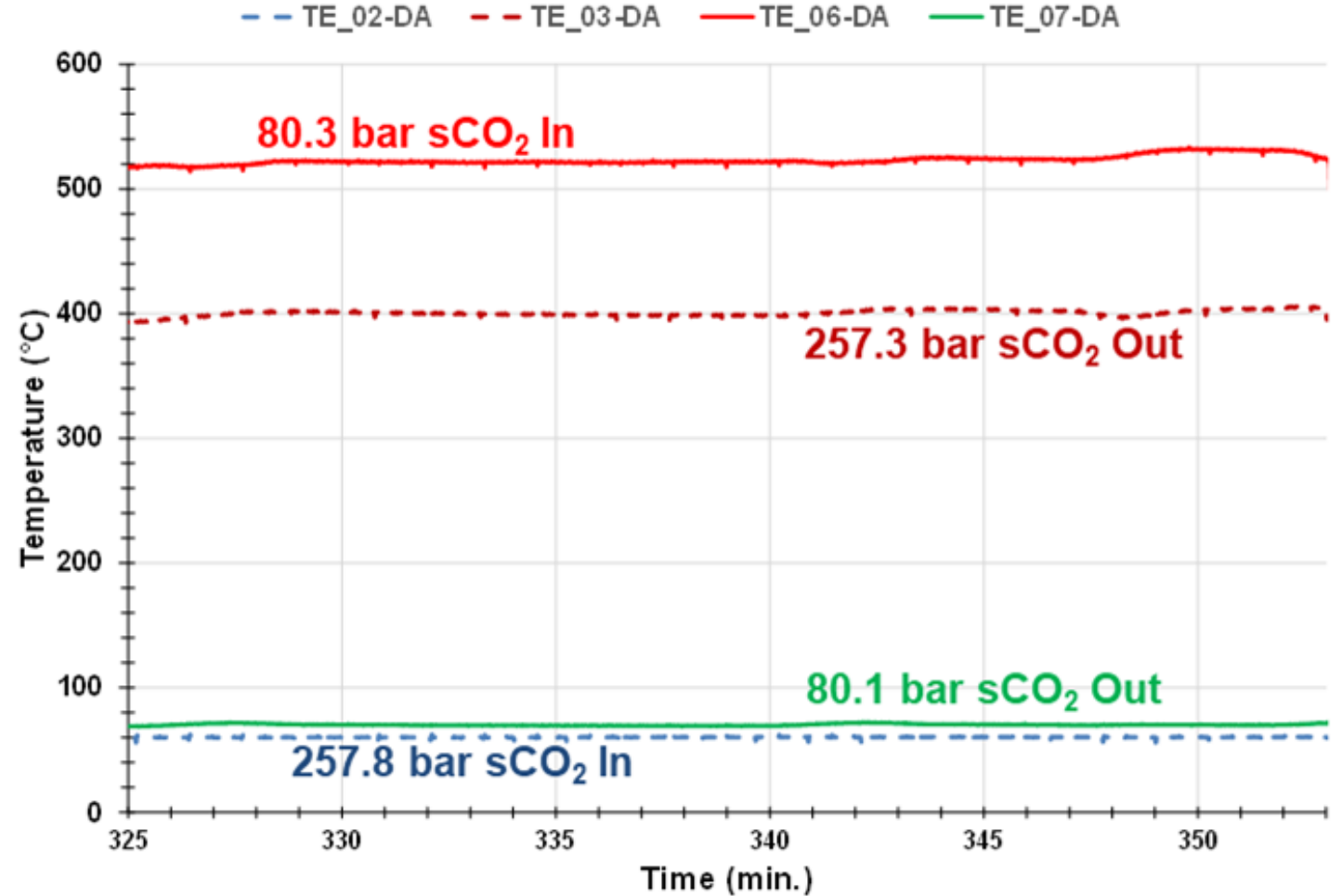


## Steady State Time vs. Temperature Plot

### Prototype SSHX Recuperators

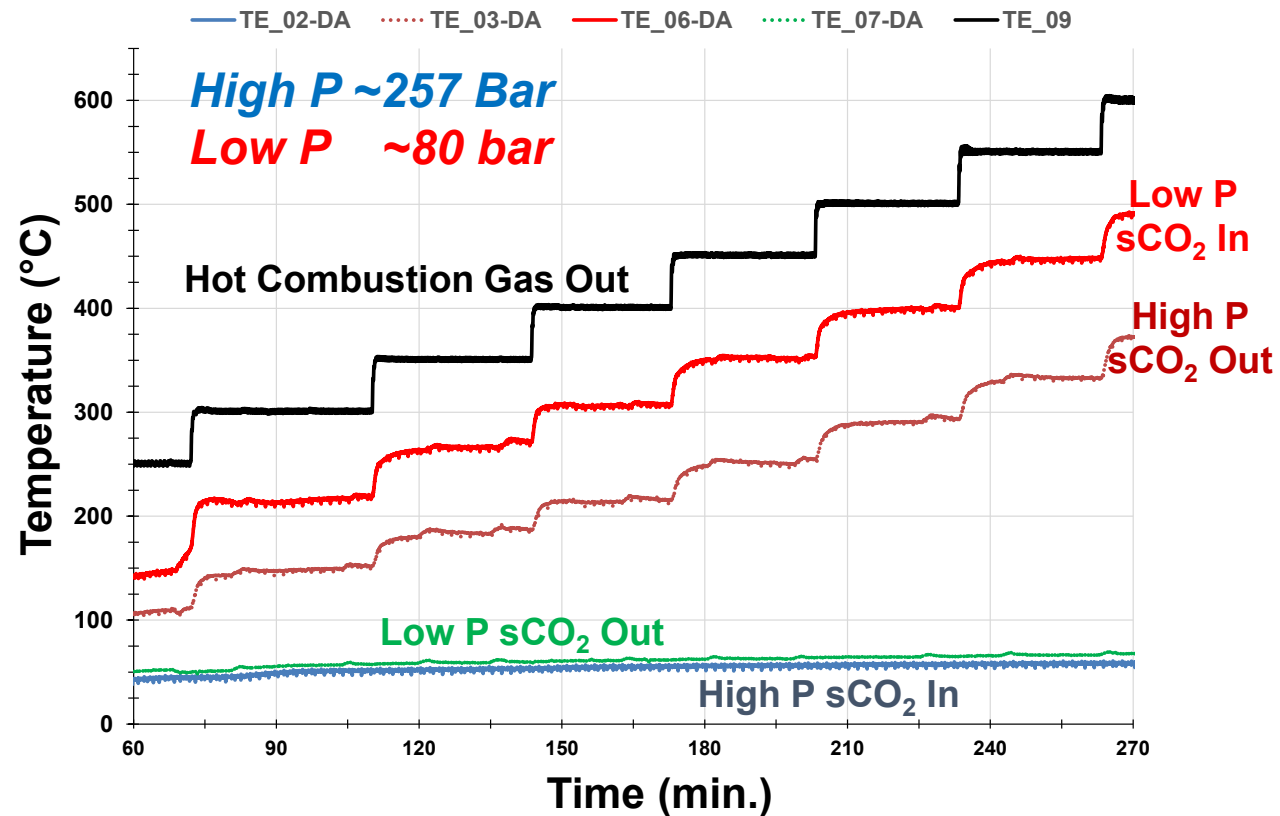


### 3D-SSHX – Steady State Plot



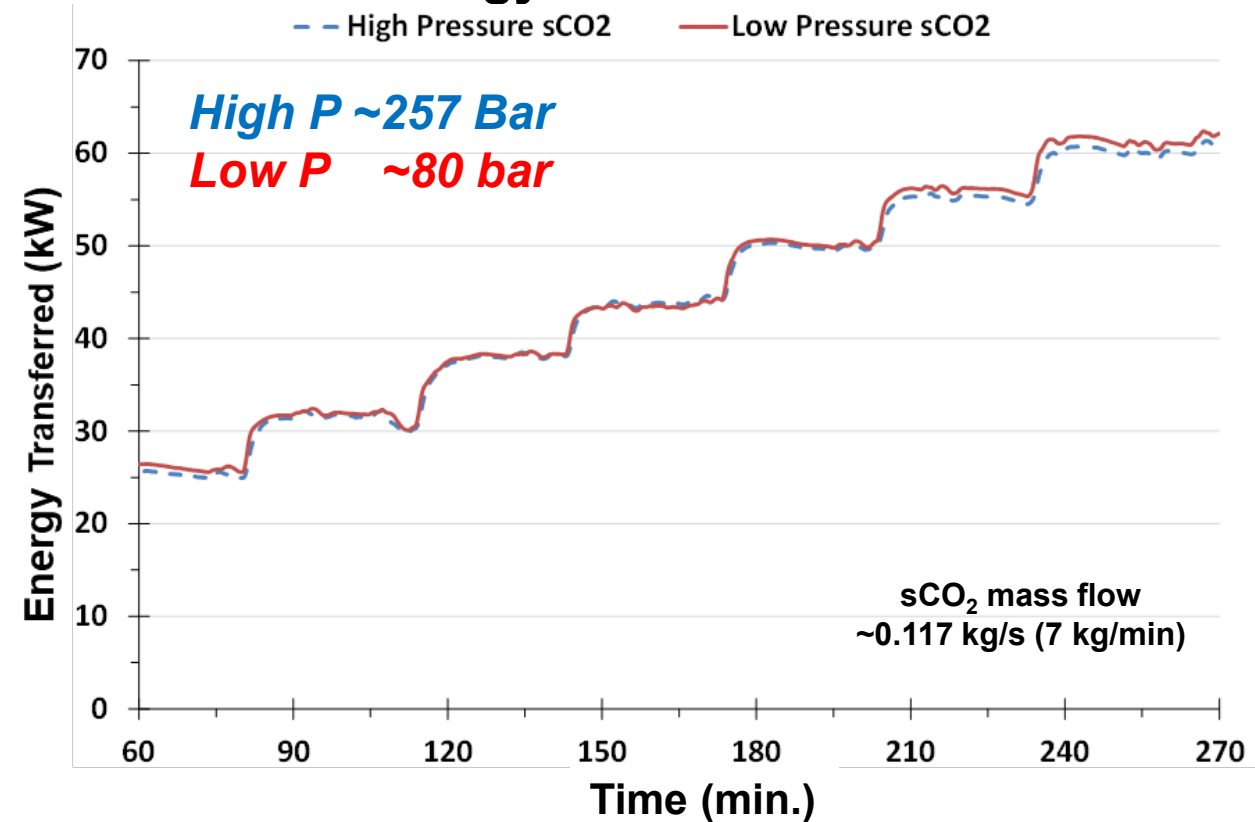
## Test & Energy Balance Plots Prototype 3D-SSHX Recuperator

### Time vs. Temperature Plot



**Approach T, < 10°C**

### Energy Balance Plot

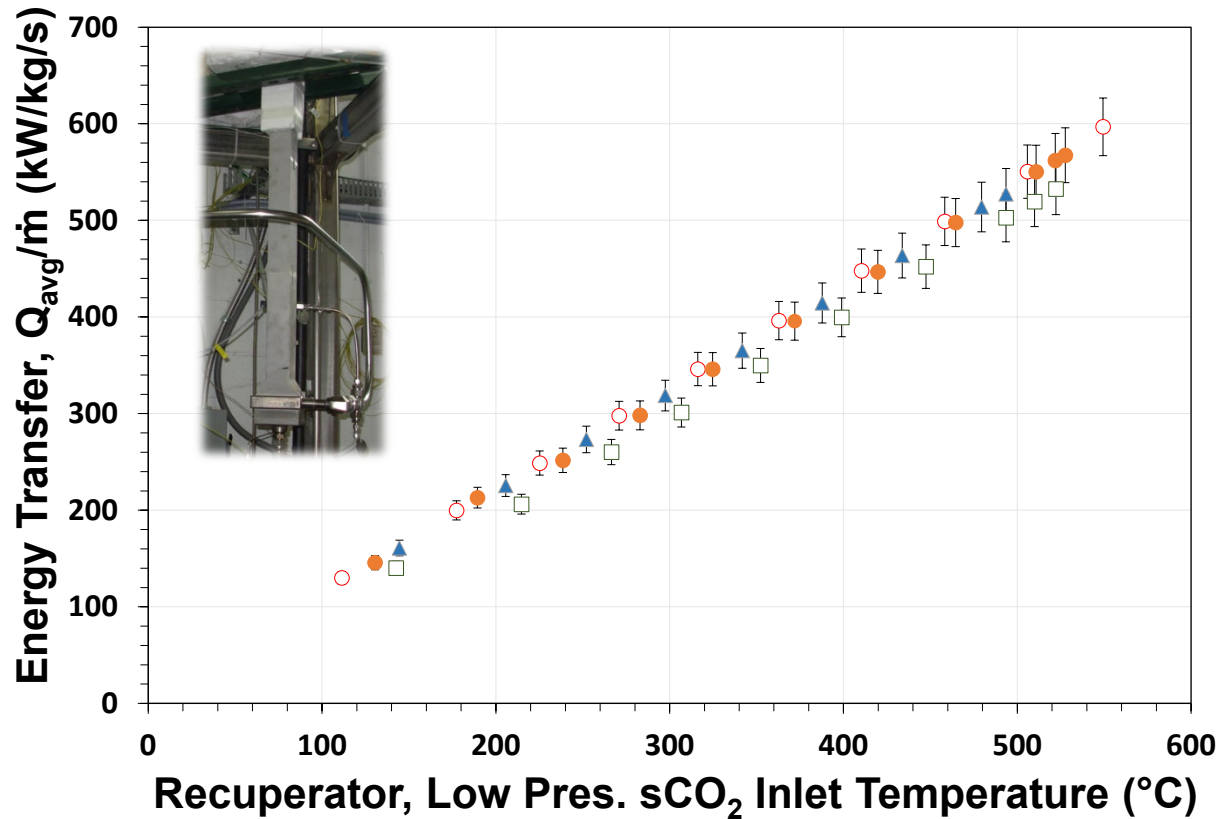


**Good Energy Balance, < 2% error**

## Energy Transfer Plots SSHX Recuperator Prototypes

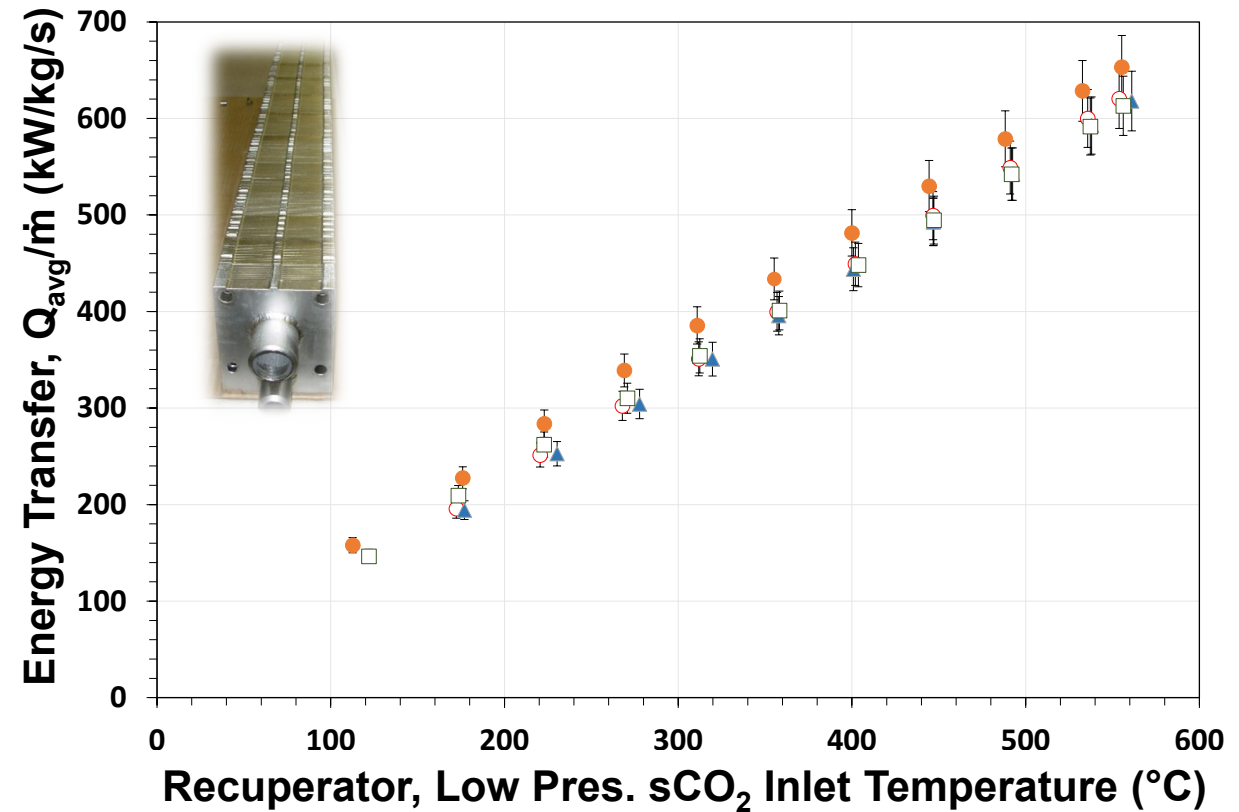
### 3D-SSHX Inconel 625

○ 152 bar #1   ● 152 bar #2   ▲ 202 bar   □ 256 bar



### Laser-SSHX 347H Stainless Steel

○ 152 bar #1   ● 151 bar #2   ▲ 202 bar   □ 252 bar

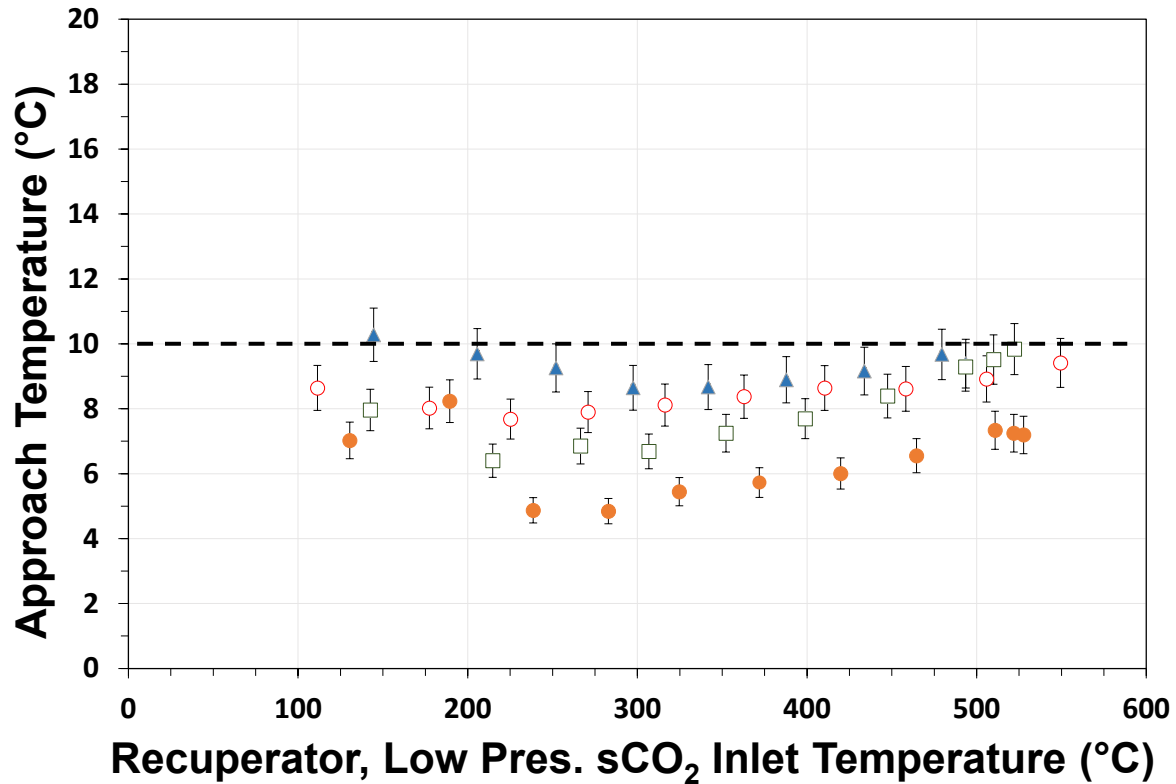


**Linear Response**

## Approach Temperature Plots SSHX Recuperator Prototypes

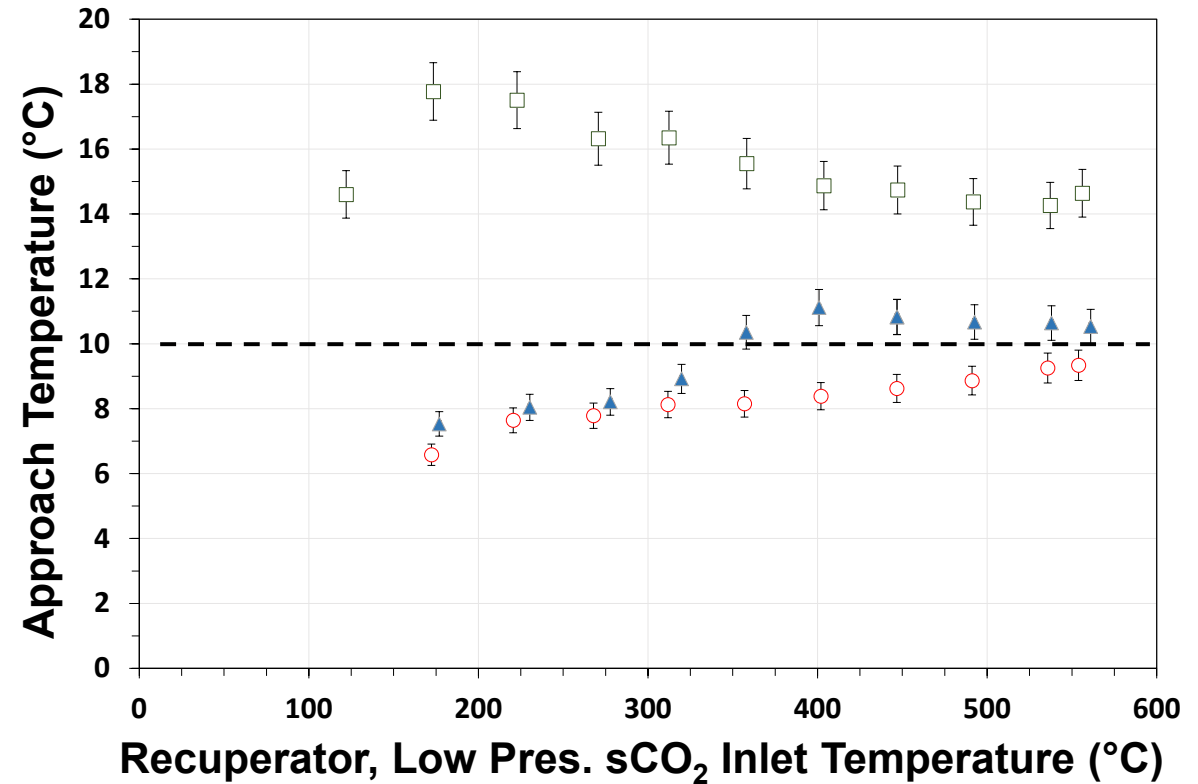
### 3D-SSHX

○ 152 bar #1   ● 152 bar #2   ▲ 202 bar   □ 256 bar



### Laser-SSHX

○ 152 bar #1   ▲ 202 bar   □ 252 bar

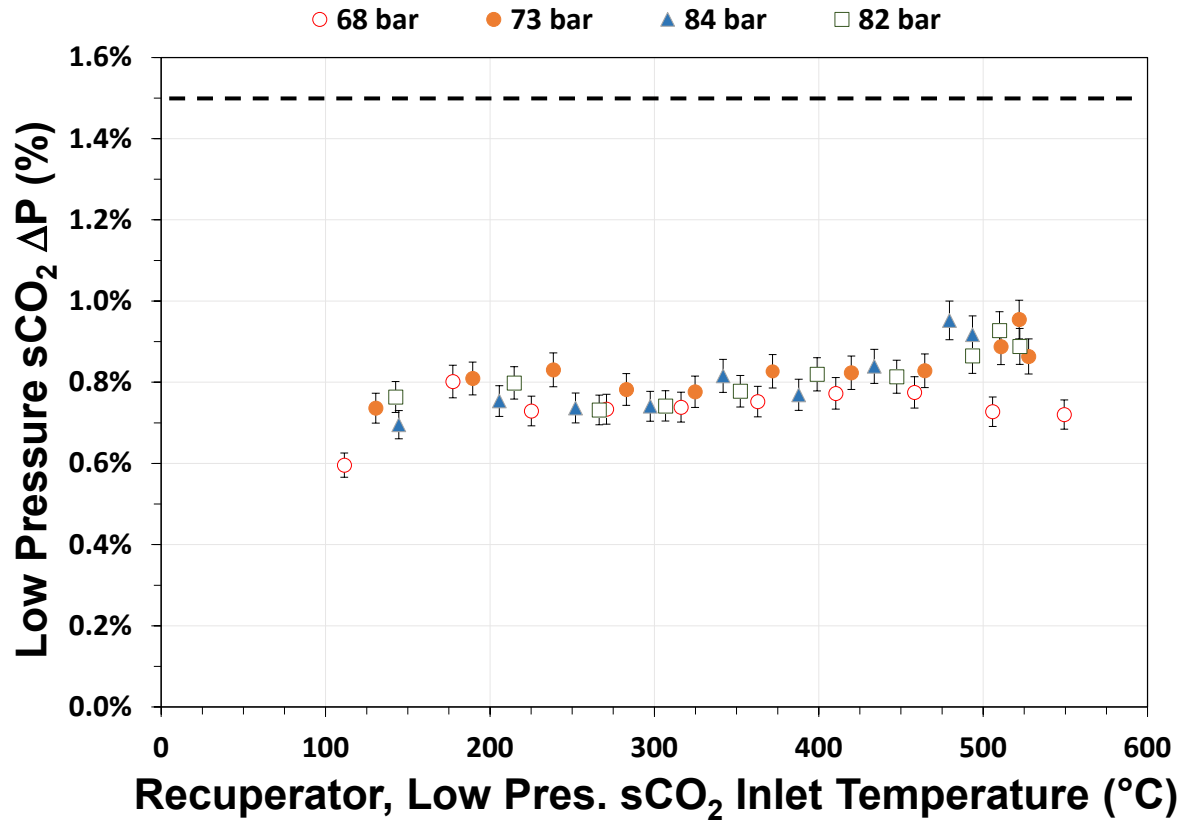


***Meets design specifications***

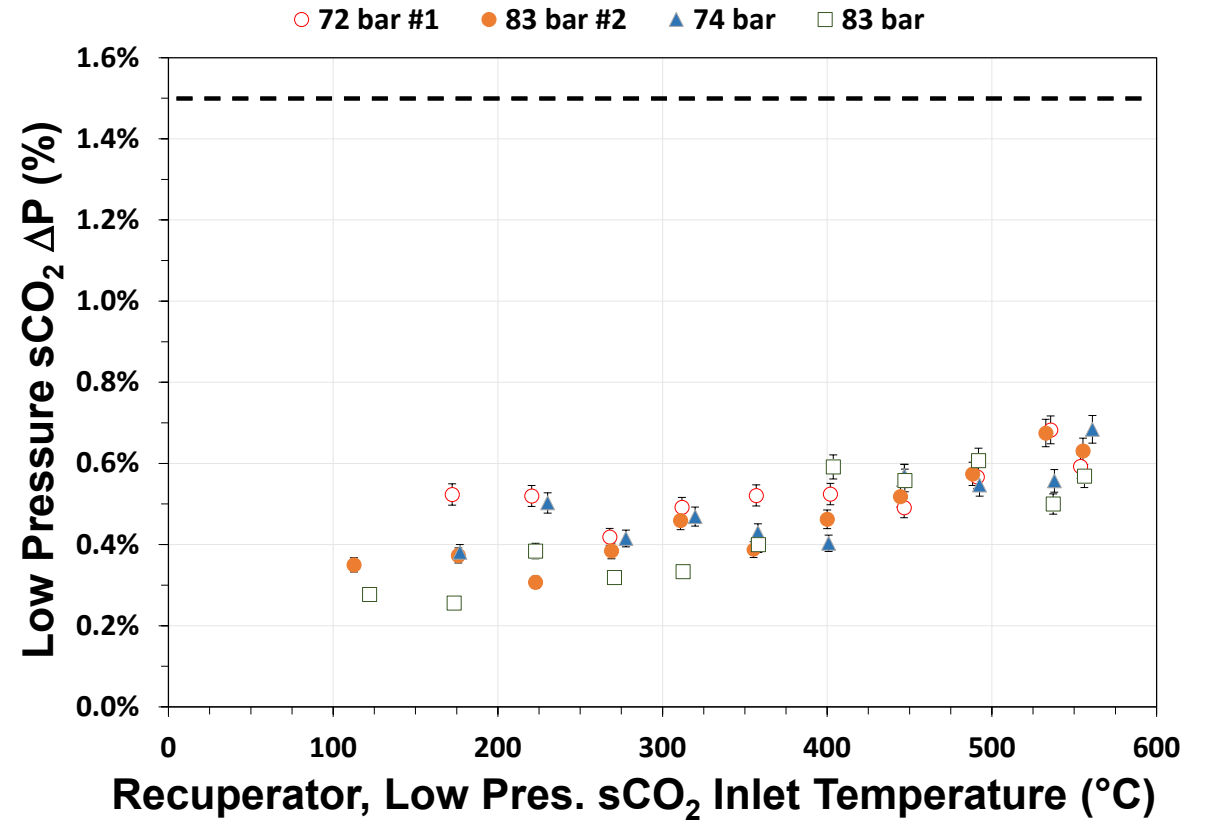
# Lower Pressure sCO<sub>2</sub> ΔP Plots

## SSHX Recuperator Prototypes

### 3D-SSHX



### Laser-SSHX

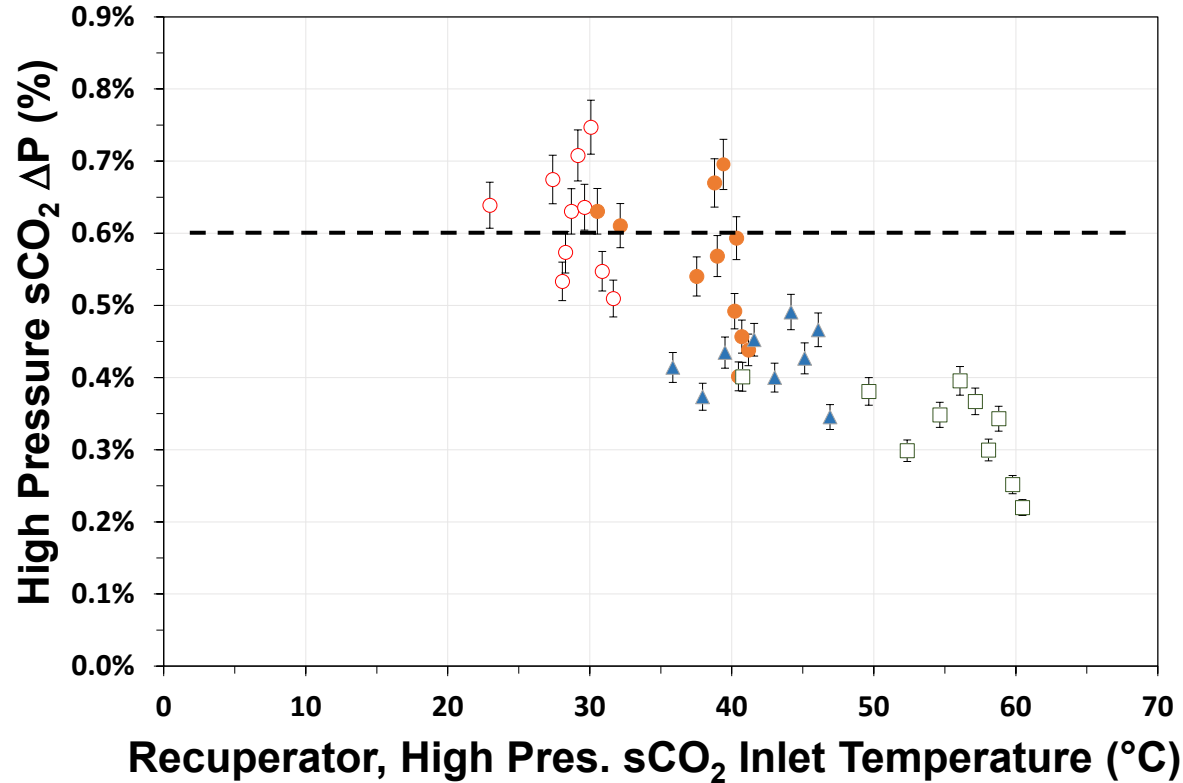


**Meets design specifications**

## Higher Pressure sCO<sub>2</sub> ΔP Plots SSHX Recuperator Prototypes

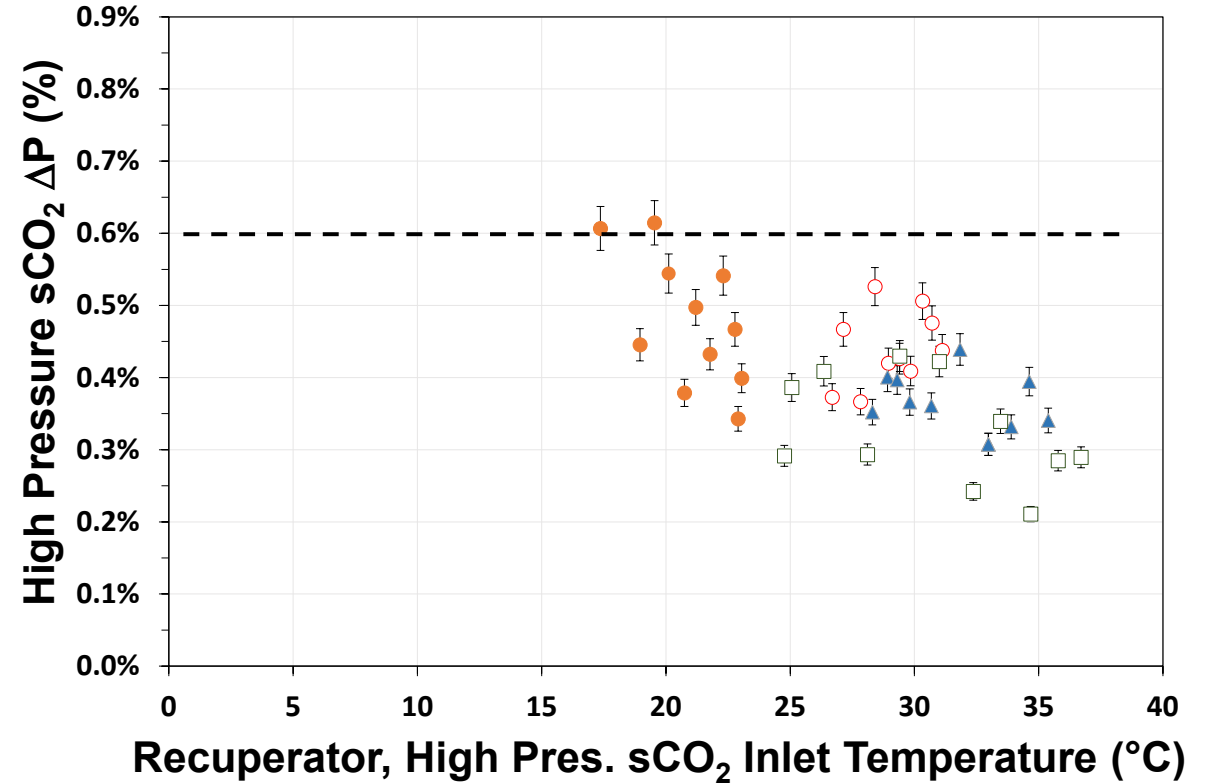
### 3D-SSHX

○ 152 bar #1   ● 152 bar #2   ▲ 202 bar   □ 256 bar



### Laser-SSHX

○ 152 bar #1   ● 151 bar #2   ▲ 202 bar   □ 252 bar

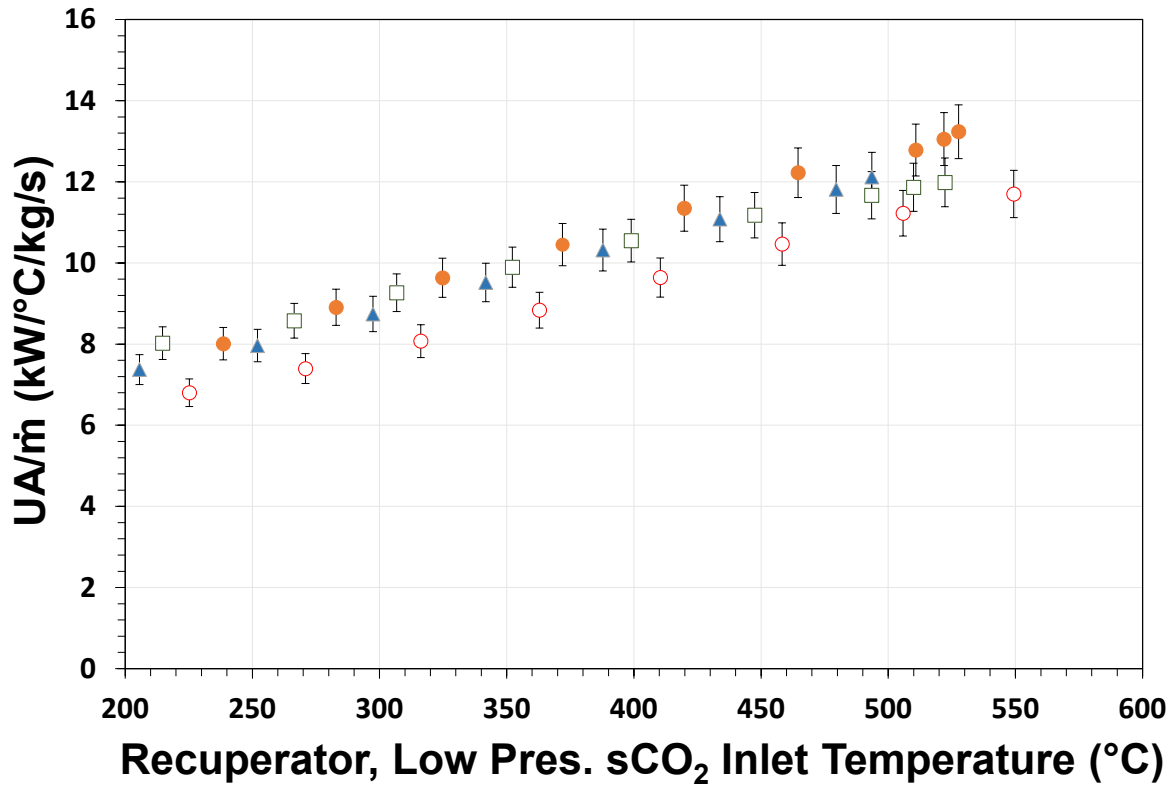


***Meets design specifications***

## Heat Transfer (UA) Plots SSHX Recuperator Prototypes

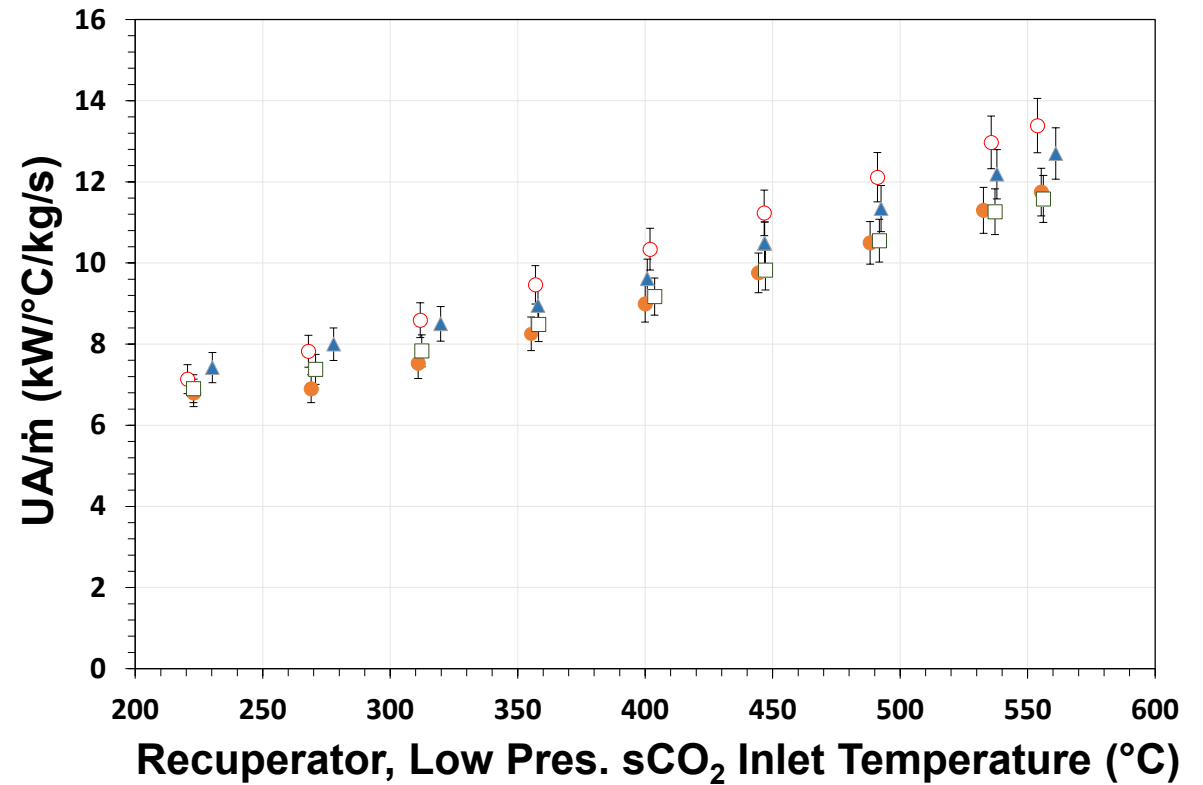
### 3D-SSHX

○ 152 bar #1   ● 152 bar #2   ▲ 202 bar   □ 256 bar



### Laser-SSHX

○ 152 bar #1   ● 151 bar #2   ▲ 202 bar   □ 252 bar



**Linear Response**

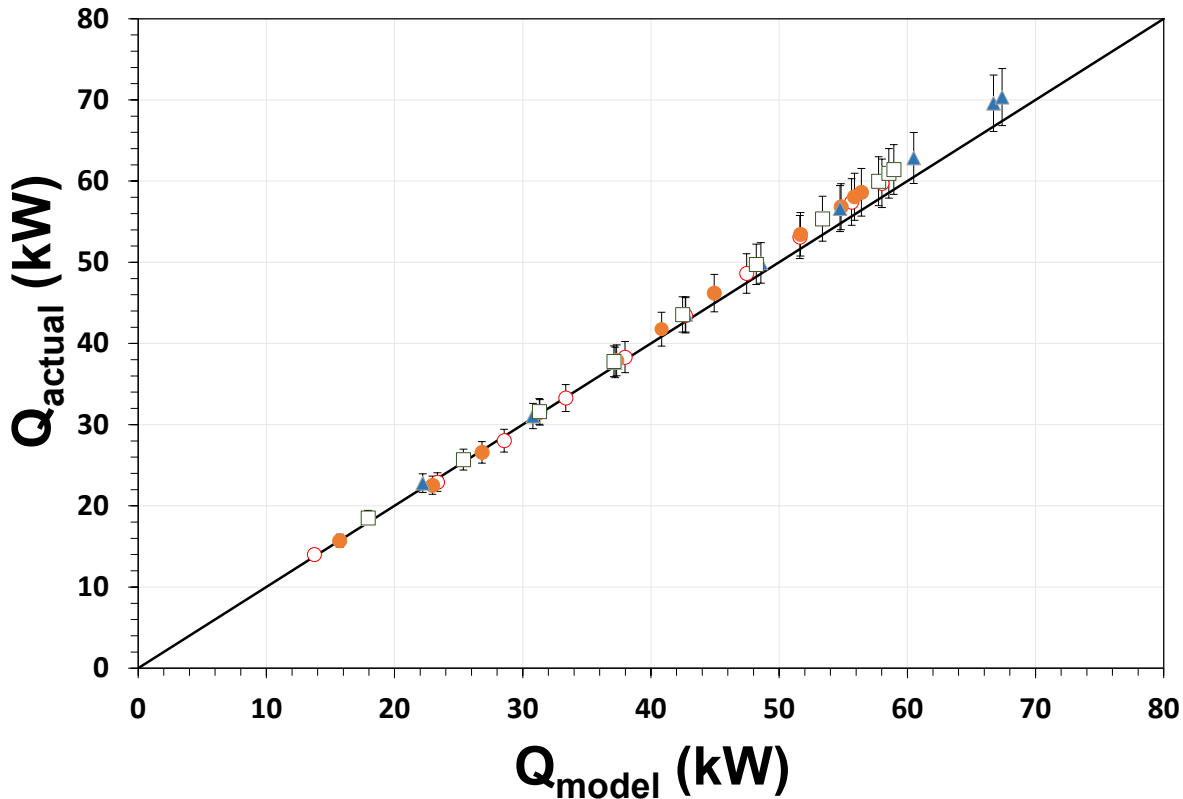


## Good correlation between Design & Actual HX performance data

### 3D-SSHX

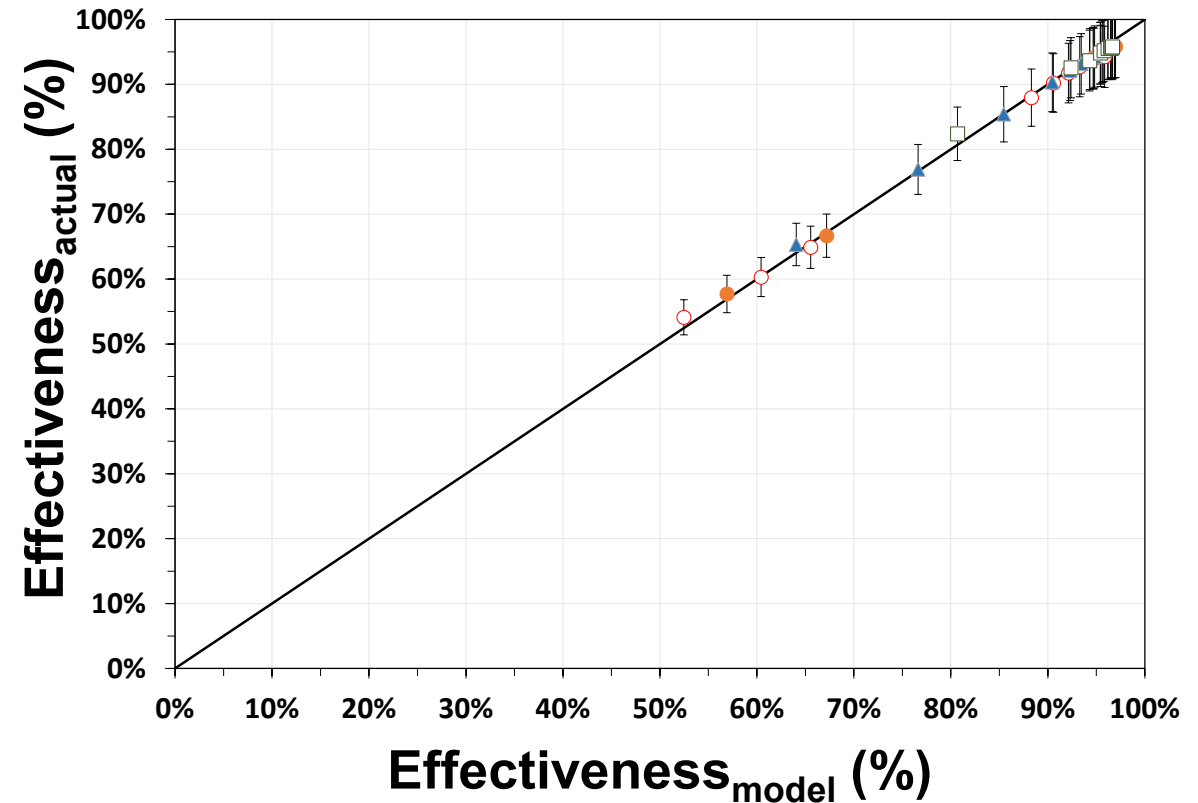
#### Transferred Energy, Q

○ 152 bar #1   ● 152 bar #2   ▲ 202 bar   □ 256 bar



#### Effectiveness, $\epsilon$

○ 152 bar #1   ● 152 bar #2   ▲ 202 bar   □ 256 bar

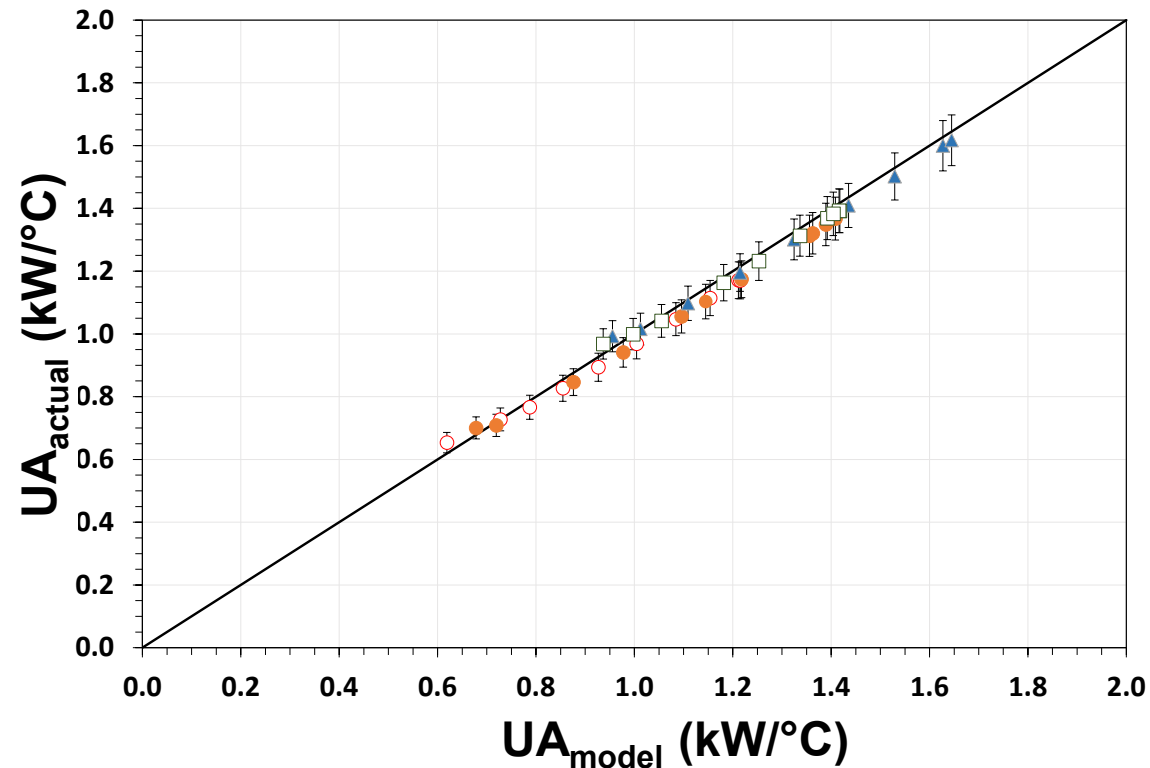


## Data confirms SSHX Recuperator Performance

### 3D-SSHX

#### Heat Transfer Coefficient, UA

○ 152 bar #1   ● 152 bar #2   ▲ 202 bar   □ 256 bar

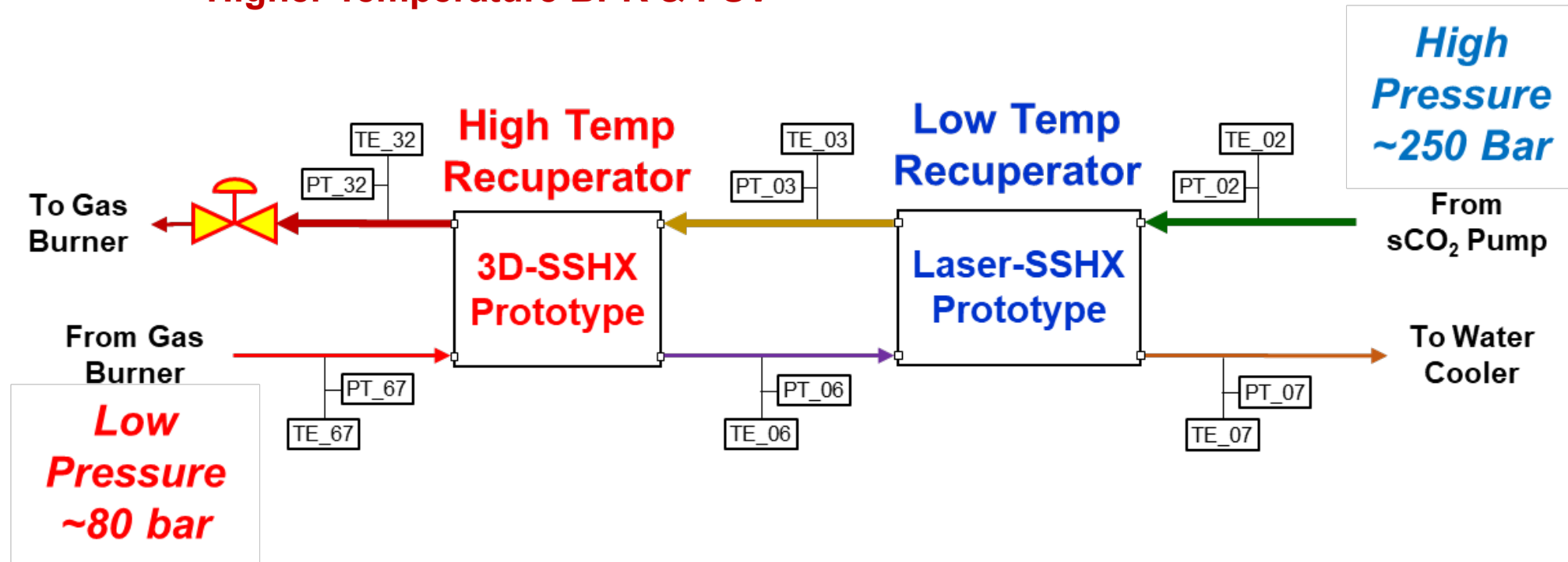


### SSHX Recuperator meets or exceeds program requirements

Criteria	Updated - 8/16/16	SSHX Prototype
Thermal Capacity	45.9 MWt	✓
Thermal Effectiveness	97%	✓
Pressure Loss	$\Delta P_h < 1.5\%$ (1.3 bar)	✓
	$\Delta P_c < 0.6\%$ (1.3 bar)	✓
Temperature Limit	577°C	✓
Differential Pressure	152 bar	✓
Life	30,000 hr	TBD
Cost	< \$100 / kWt	✓
Package Dimensions	8.8 x 3.6 x 2.6 m	✓

## Reconfigured sCO<sub>2</sub> Brayton Power Cycle Heat Exchanger Test Facility

- **COMBO-SSHX: Laser-SSHX & 3D-SSHX** piped in series
- Additional Temp. & Pres. sensors
- Higher Temperature BPR & PSV

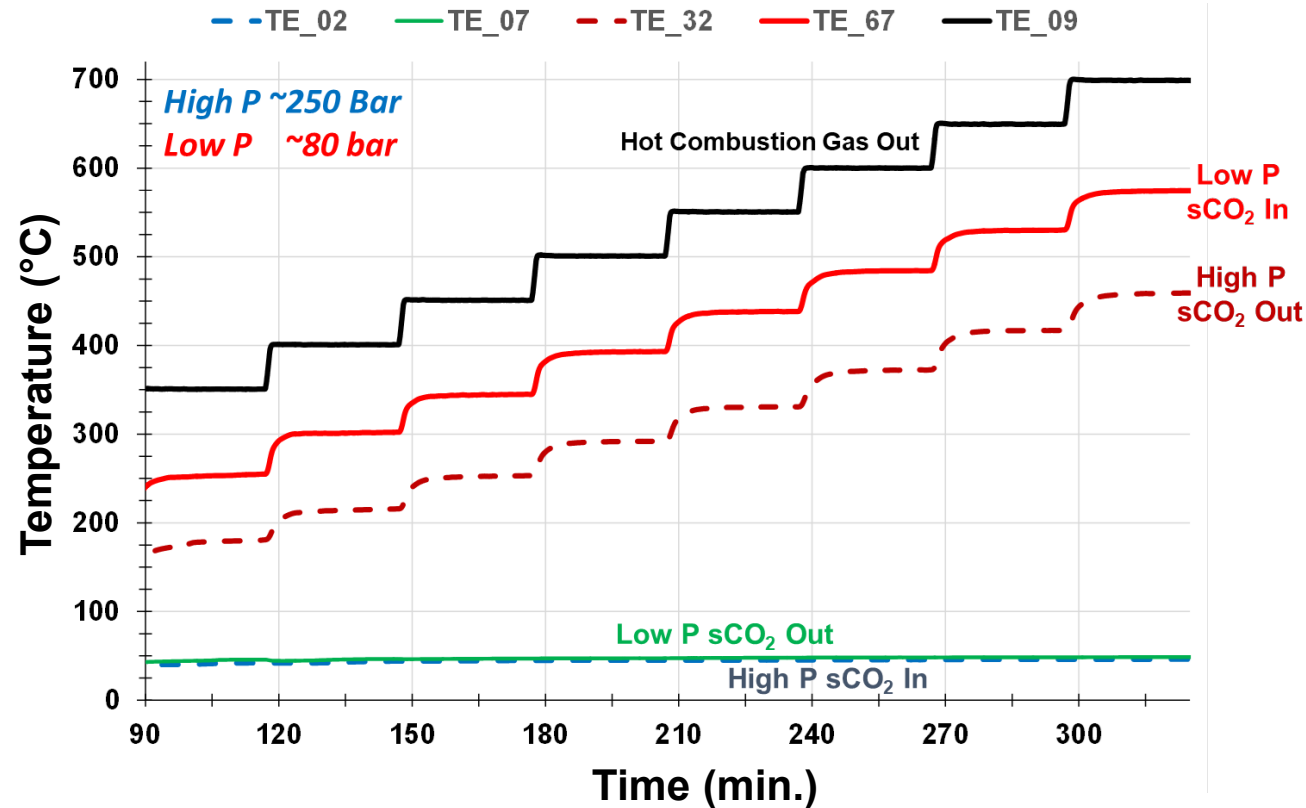


## Test & Energy Balance Plots

### COMBO-SSHX Recuperator

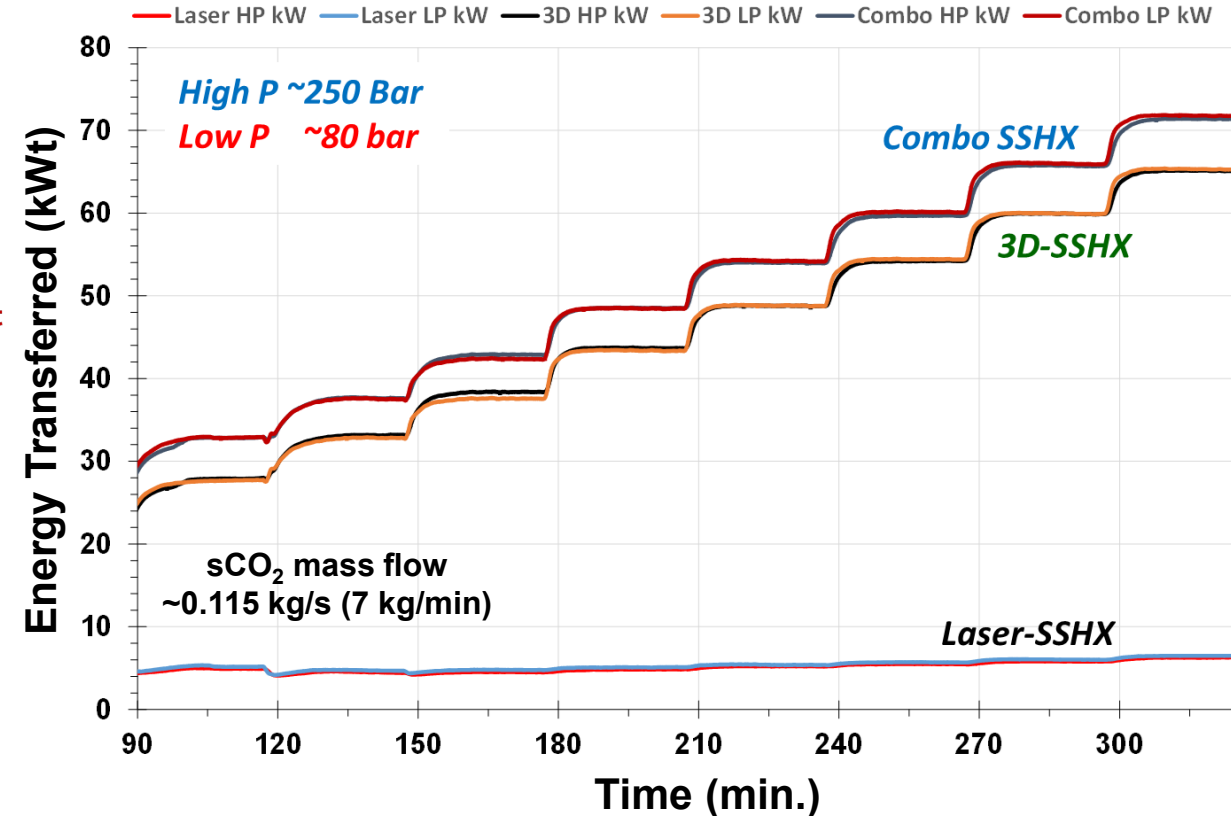
(Laser-SSHX & 3D-SSHX connected in series)

### Combo-SSHX Time vs. Temperature Plot



**Approach T: < 5°C**  
**Effectiveness: > 98%**

### Energy Balance Plot



**Good Energy Balance, < 2% error**

## Summary

- Prototype recuperators have been designed, fabricated, and tested
  - ❖ **3D-SSHX**
  - ❖ **Laser-SSHX**
  - ❖ **Combo-SSHX: Laser-SSHX piped in series with the 3D-SSHX**
- sCO<sub>2</sub> Heat Exchanger Test Loop has been *successfully operated* over range of operating conditions
- The **SSHX recuperator concept *meets or exceeds* STEP cost and thermal/hydraulic performance criteria**
  - ❖ Concept been scaled to 46 MWt thermal capacity, industrial scale
  - ❖ **Modular/Factory Fabricated design incorporates compact size/cost**
  - ❖ ***Potential for future enhancements***

*Thank you for your kind attention*

**Questions?**

**Work supported by US DOE under DE-FE0026273**  
Richard Dennis, Advanced Turbines Technology Manager  
Seth Lawson, Program Officer, Advanced Energy Systems Division