

# Large Scale Tri-Generation Energy Storage for Heat, Cold and Electricity based on Transcritical CO<sub>2</sub> Cycles

Paper #162

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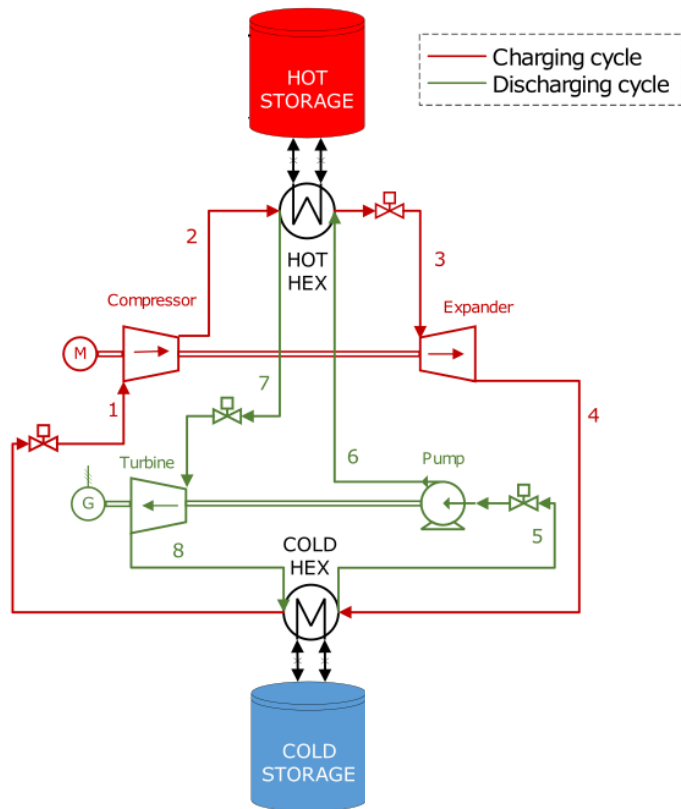
San Antonio, Texas, USA



# Agenda

- 1 Introduction**
- 2 Working principle of the system**
- 3 Model description**
- 4 Impact of thermal boundary conditions on system's performance**
- 5 Impact of economic boundary conditions on system's performance**
- 6 System operational flexibility**
- 7 Conclusions and interpretations**

# From an electricity storage system to a tri-generation energy system

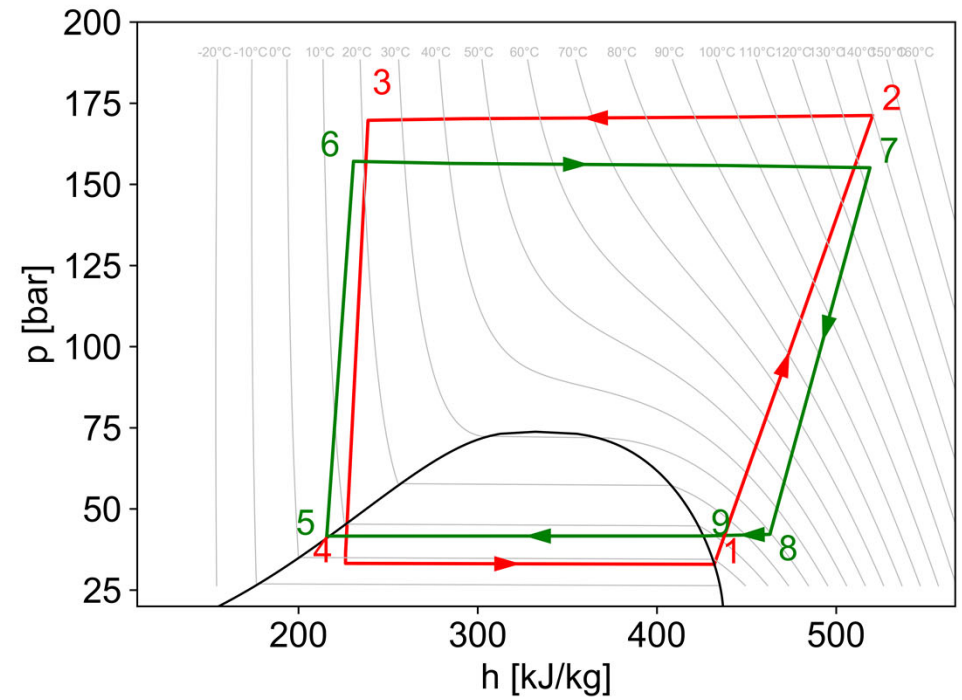
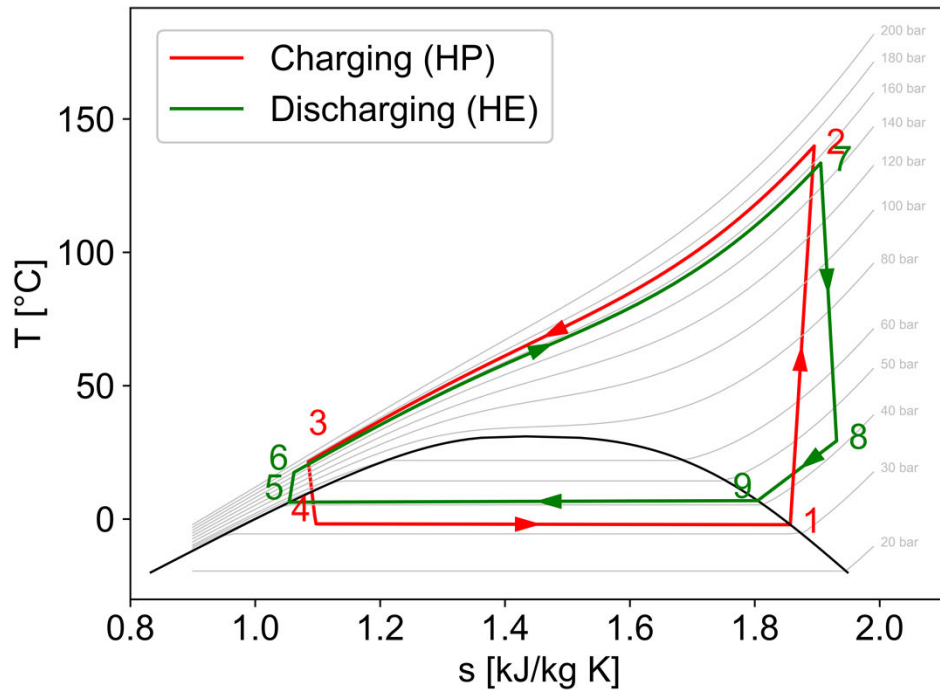


- CO<sub>2</sub> as working fluid
- **Charging cycle: transcritical heat pump**
- **Discharging cycle: organic Rankine cycle**
- Power range: 1-50 MW<sub>el</sub>
- Typical cycle time: 12-24 h

Thermal storage	Medium	Temp. range	Type	Setup
Hot	Water	15-150°C	Sensible	Multi-tank reservoirs
Cold	Water / Ice	0°C	Latent	Ice on coils

Moderate temperature levels allows to combine the system with **heating** and **cooling** applications!

# Thermodynamic diagrams



# Working principle of the system



$$COP_{hot}^{ex} = \frac{Q_{hot}}{E_{ch}^{tot} \cdot \gamma^{th}}$$

$$\eta_{RT} = \frac{E_{dch}}{E_{ch}^{tot} \cdot \gamma^{el}}$$

$$COP_{cold}^{ex} = \frac{Q_{cold}}{E_{ch}^{tot} \cdot \gamma^{th}}$$

Thermal share  $\gamma^{th}$  → amount of stored energy destined for **thermal** export

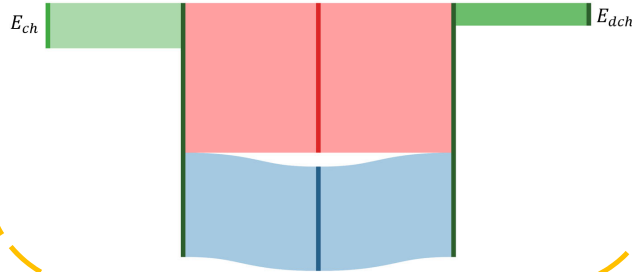
Electric share  $\gamma^{el}$  → amount of stored energy destined for **electricity** export

$$\left. \begin{array}{l} \text{Thermal share } \gamma^{th} \rightarrow \text{amount of stored energy destined for thermal export} \\ \text{Electric share } \gamma^{el} \rightarrow \text{amount of stored energy destined for electricity export} \end{array} \right\} \gamma^{th} + \gamma^{el} = 1$$

# Possible configurations

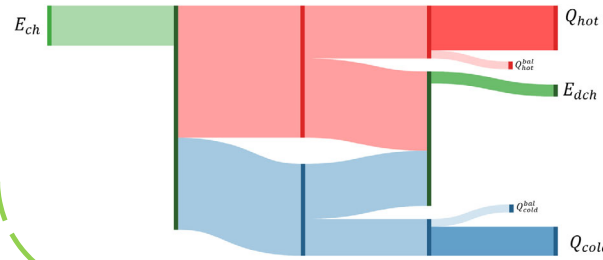
## Pure electricity storage (ETES)

- Charging cycle
- Discharging cycle
- Thermal storage
- $\gamma^{th} = 0$



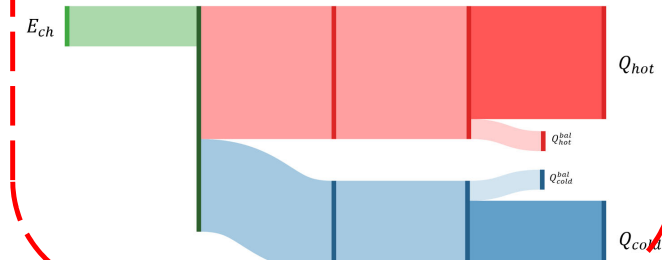
## Tri-generation energy system (3-TES)

- Charging cycle
- Discharging cycle
- Thermal storage
- Thermal export
- $0 < \gamma^{th} < 1$



## Heat pump unit (HPU)

- Charging cycle
- Thermal storage optional
- Thermal export
- $\gamma^{th} = 1$



Highly flexible and adaptable to specific electric and thermal demands!

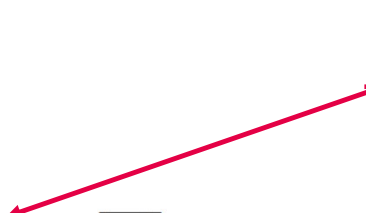
# Sophisticated Model is needed to calculate and optimize System performance

Considered model:

- Thermodynamic library: Refprop v10.0
- Steady state
- Sequential calculation solver developed in python

Constrained optimization problem:

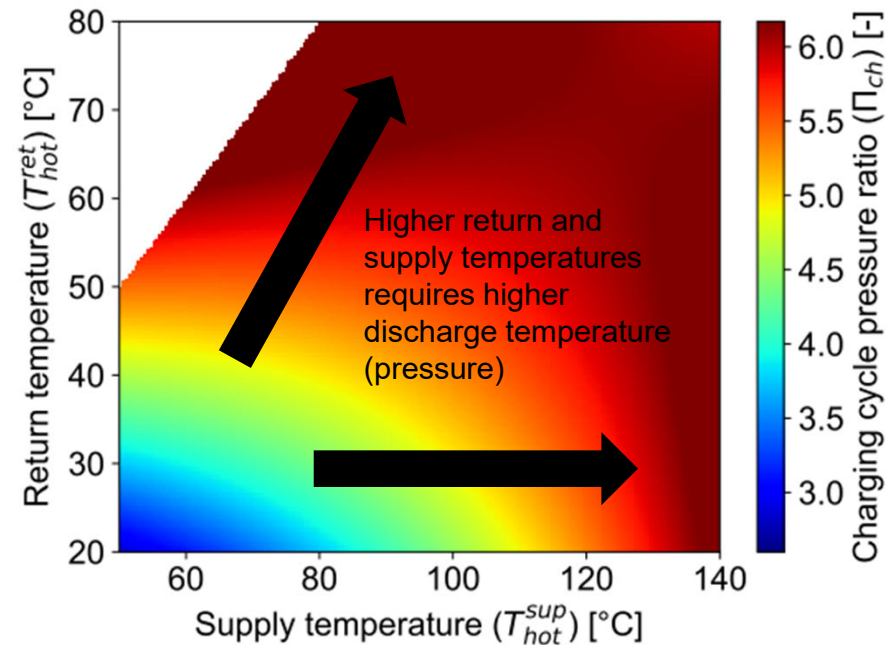
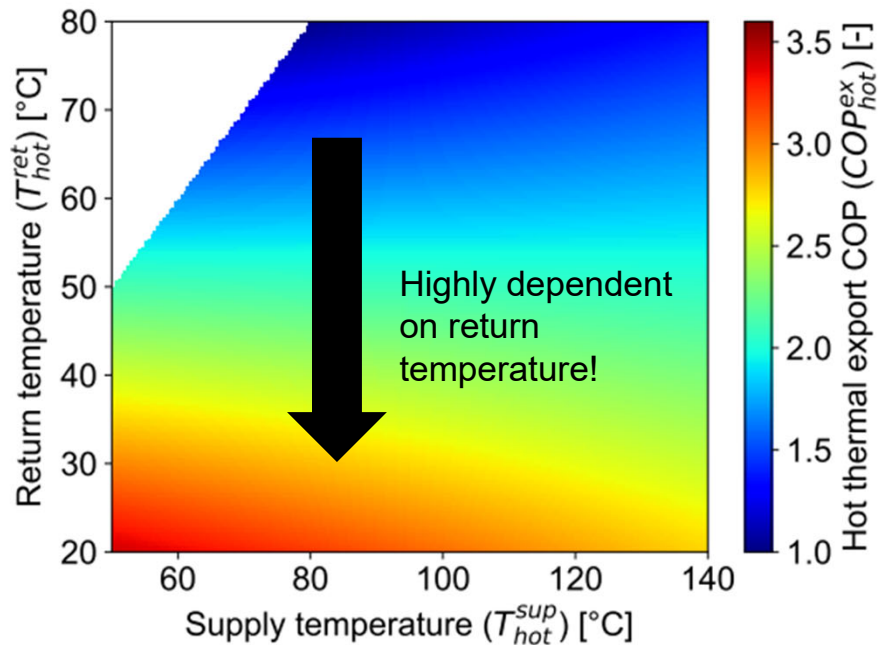
$$\begin{aligned} & \underset{x}{\text{minimize}} && f(x) + \sum_{i=1} Pen_i(x) \\ & \text{subject to} && l_b \leq x \leq u_b, \\ & && x \in \mathbb{R} \end{aligned}$$

- 
- Profit of the installation
  - Performance
  - other

# System performance is heavily dependent on thermal boundary conditions

$$COP_{hot}^{ex} = \frac{Q_{hot}}{E_{ch}^{tot} \cdot \gamma^{th}}$$

$$\Pi_{ch} = \frac{P_{cond}}{P_{evap}}$$





# System profitability and operation is heavily dependent on economic boundary conditions

The operation of the cycle is determined by the profit one can obtain from running the system

$$P_{cy}[\text{€}] = \left( \overbrace{E_{dch}^{el} \cdot C_{dch}^{el} + Q_{hot} \cdot C_{hot} + Q_{cold} \cdot C_{cold}}^{\text{Revenue}} \right) - \overbrace{E_{ch}^{tot} \cdot C_{ch}^{el}}^{\text{Costs}}$$

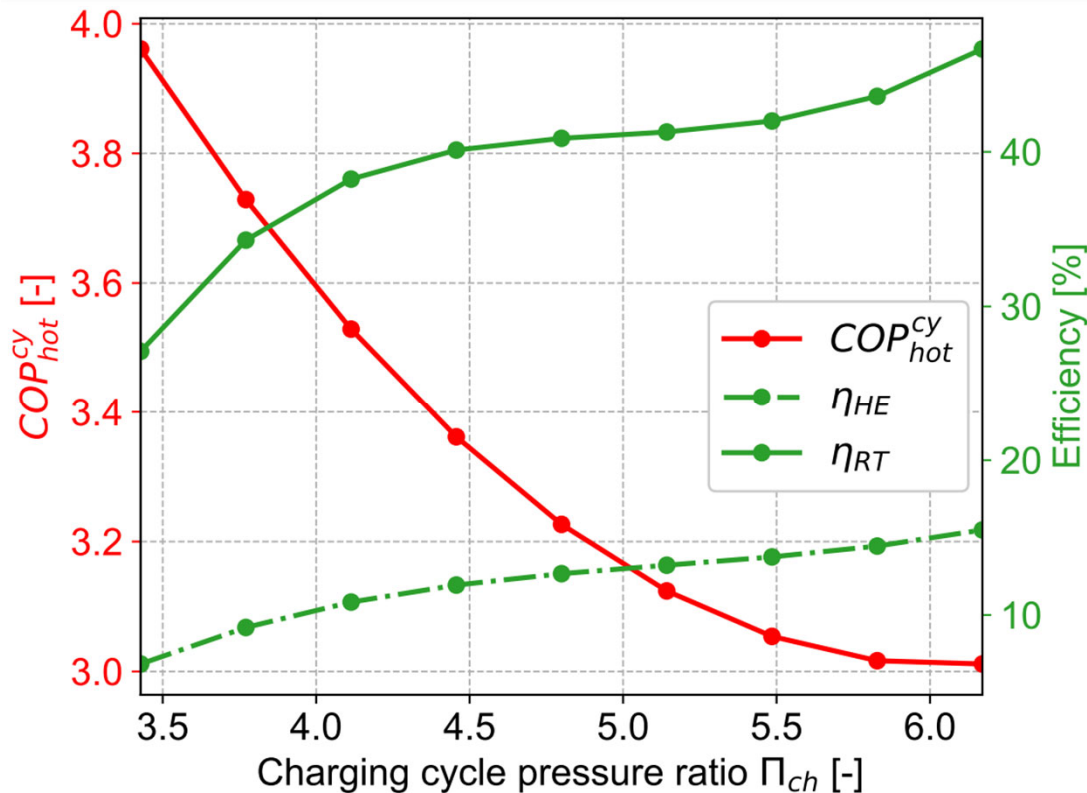


Dividing by purchased amount of electricity we obtain the normalized profit as a function of KPIs

$$\begin{aligned} \frac{P_{cy}}{E_{ch}^{tot} \cdot C_{ch}^{el}} \left[ \frac{\text{€}}{\text{€}_{ch}} \right] &= \frac{1}{E_{ch}^{tot} \cdot C_{ch}^{el}} \cdot (E_{dch}^{el} \cdot C_{dch}^{el} + Q_{hot} \cdot C_{hot} + Q_{cold} \cdot C_{cold}) - 1 \\ &= \left( (1 - \gamma^{th}) \cdot \eta_{RT} \cdot \phi_{el} + \gamma^{th} \cdot (COP_{hot}^{ex} \cdot \phi_{hot} + COP_{cold}^{ex} \cdot \phi_{cold}) \right) - 1 \end{aligned}$$

$$\begin{aligned} \phi_{el} &= \frac{C_{el}^{dch}}{C_{el}^{ch}} \\ \phi_{hot} &= \frac{C_{hot}}{C_{el}^{ch}} \\ \phi_{cold} &= \frac{C_{cold}}{C_{el}^{ch}} \end{aligned}$$

# A compromise between electrical and thermal export is necessary



$$\eta_{RT} = COP_{hot}^{cy} \cdot \eta_{HE}$$

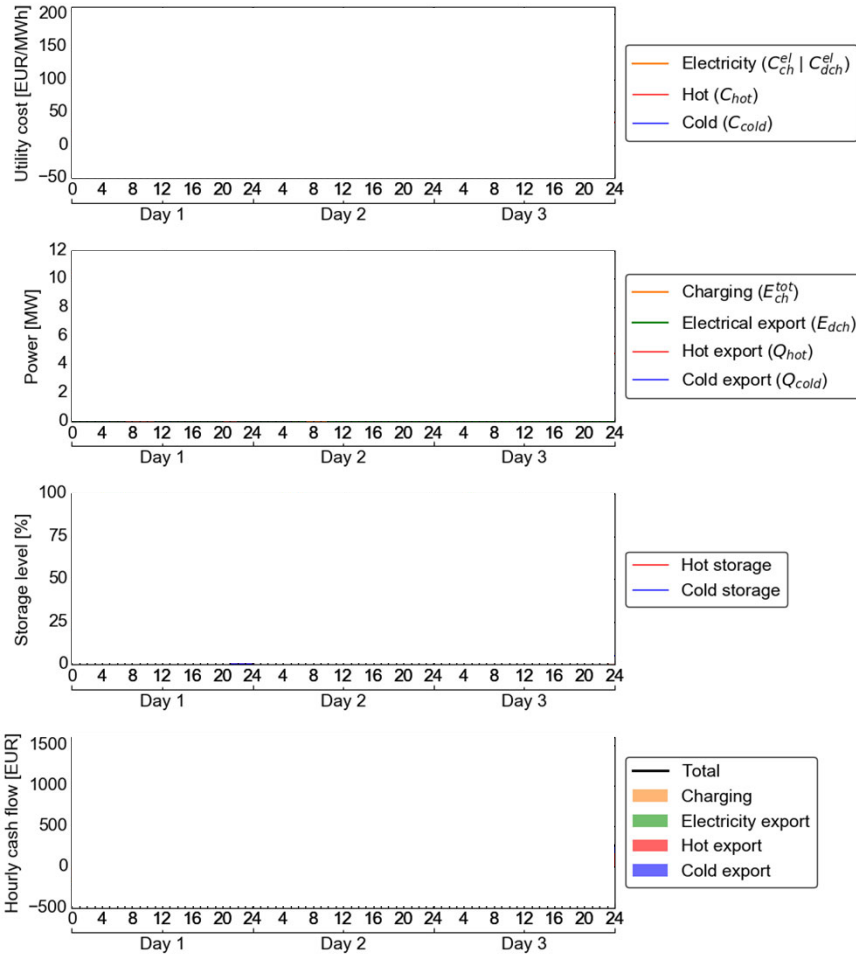
Charging cycle (pointing to  $COP_{hot}^{cy}$ )      Discharging cycle (pointing to  $\eta_{HE}$ )

- $\Pi_{ch} \uparrow$  Favors electricity export
- $\Pi_{ch} \downarrow$  Favors thermal export



$\Pi_{ch}$  can be optimized for the given set of thermal and economic boundary conditions of each cycle

# Highly adaptable and flexible system



Day	Economic boundary conditions	Stored energy use	Storage levels

Day	Charging	Export			TOTAL
		Electricity	Hot	Cold	
Day 1	-1'726	2'768	-	-	1'042
Day 2	-1'88	2'370	4'071	3'885	10'138
Day 3	-1'303	-	5'824	5'200	9'720

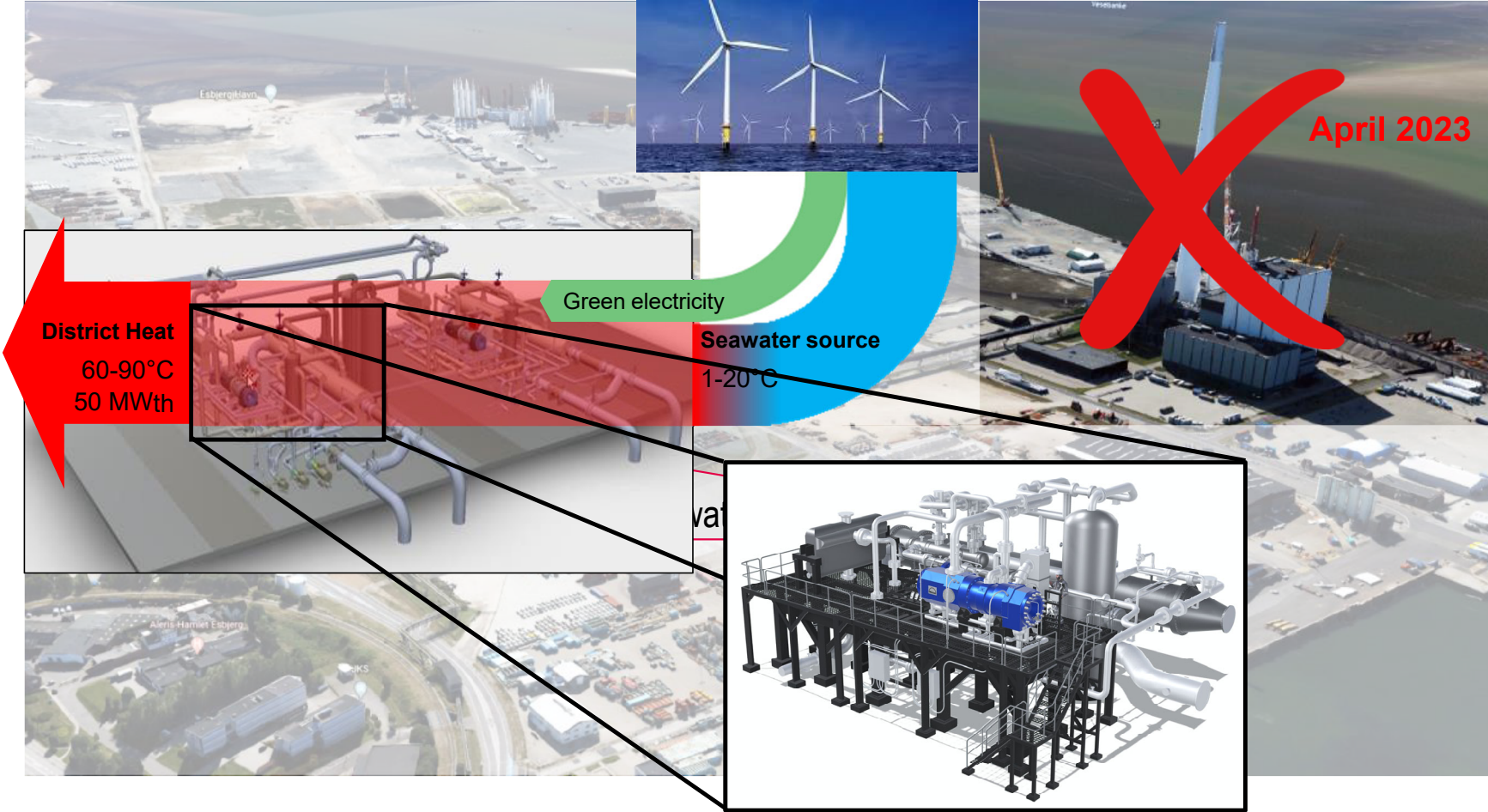
High profit obtained from thermal export!



# Conclusions and interpretations

- The **moderate temperature conditions** of the system allows to not only store and export **electricity**, but also **heat** and **cold**.
- 3-TES system offers a **good compromise** between roundtrip efficiency and thermal export performance.
- The **large design and flexibility** of the system allows to adapt the system to the changing boundary conditions expected throughout the 30+ years the installation is expected to operate with the **same equipment**.
- The complexity to find a single customer requiring the three forms of energy in the produced quantities makes the 3-TES system particularly suitable for **sector coupling** applications.

# First MAN HPU cycle under construction in Denmark!



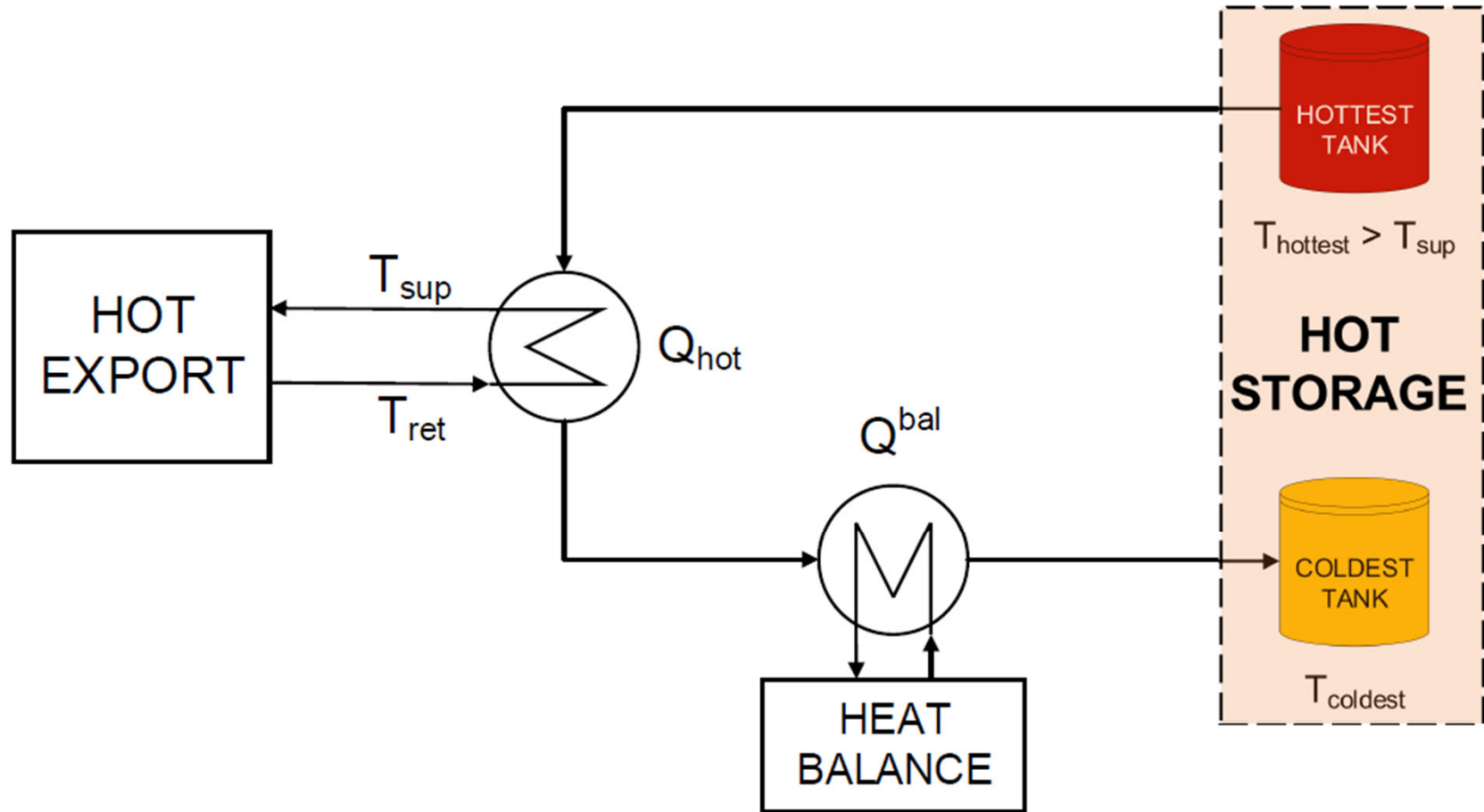
**MAN Energy Solutions**  
Future in the making



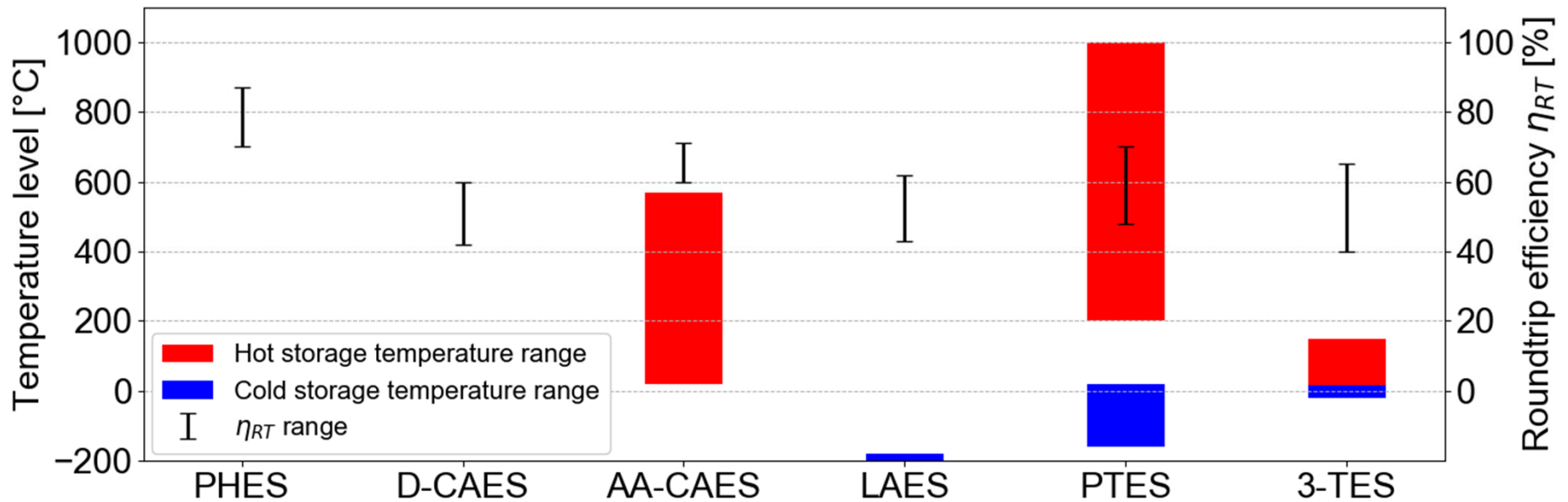
**Thank you for  
your attention!**



# Impact of return temperature



# Excellent compromise between round-trip efficiency and thermal export





# First MAN HPU cycle under construction!

- Biggest ever CO<sub>2</sub> heat pump (50+ MW<sub>th</sub>) installed in Esbjerg, Denmark.
- Replacement of CHP Coal fired plant.
- COP: 2.8 - 4.3
- Bid award January 2021
- Commissioning September 2022
- Heat production April 2023

