

02/22/2022



# Radial Compressor Design and Off-Design for Trans-critical CO<sub>2</sub> Operating Conditions

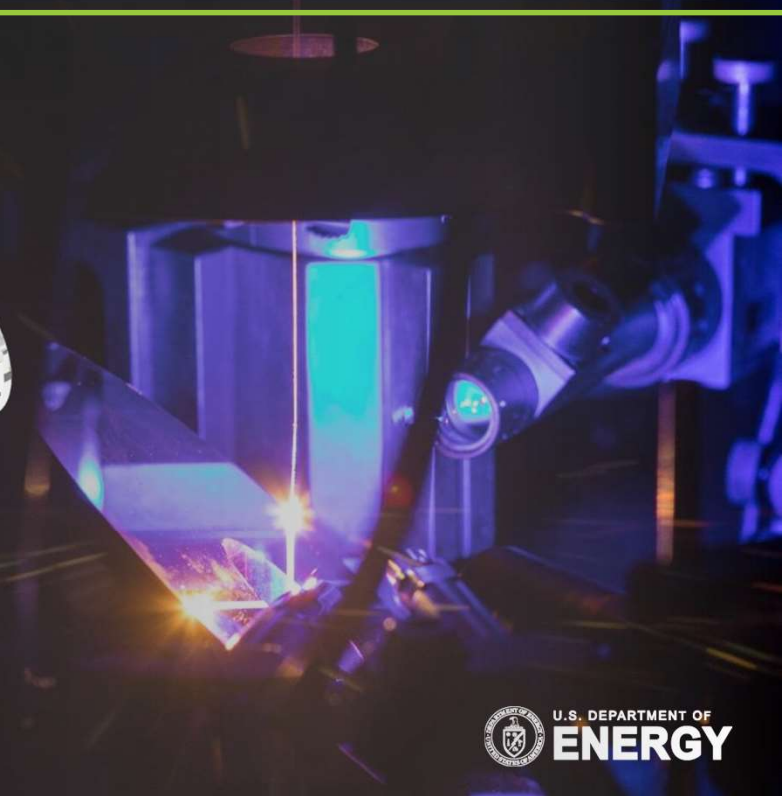
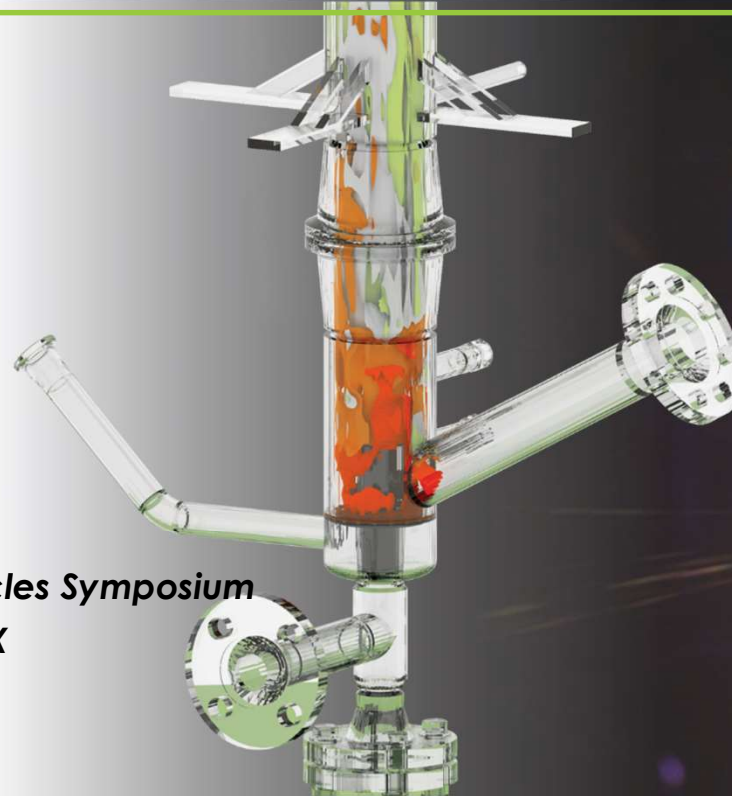


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7<sup>th</sup> International sCO<sub>2</sub> Power Cycles Symposium

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# Agenda

- Background
- Fluid Similarity Method
- Map Scaling
- Validation
- Compressor Design
- Off-Design Maps
- Compressor Design Updates
- Summary and Conclusions

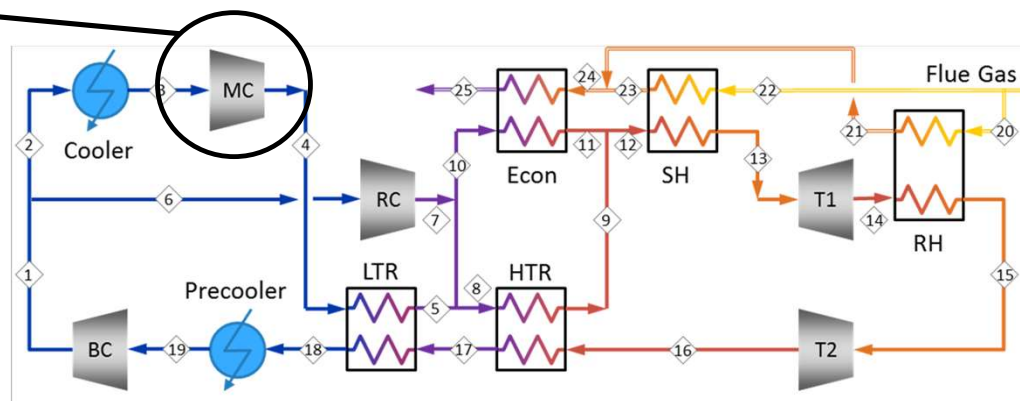


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# Background

- The main compressor/pump design condition ranges are as follows:

Main-Compressor	Inlet	Exit
Pressure (psia)	887-1200	4096-5980
Temperature (F)	71-94	98-131
Mass Flowrate (lbm/s)	5326-6991	
Volumetric Flowrate (ft <sup>3</sup> /s)	134-206	
Density (lbm/ft <sup>3</sup> )	37-46	55-58



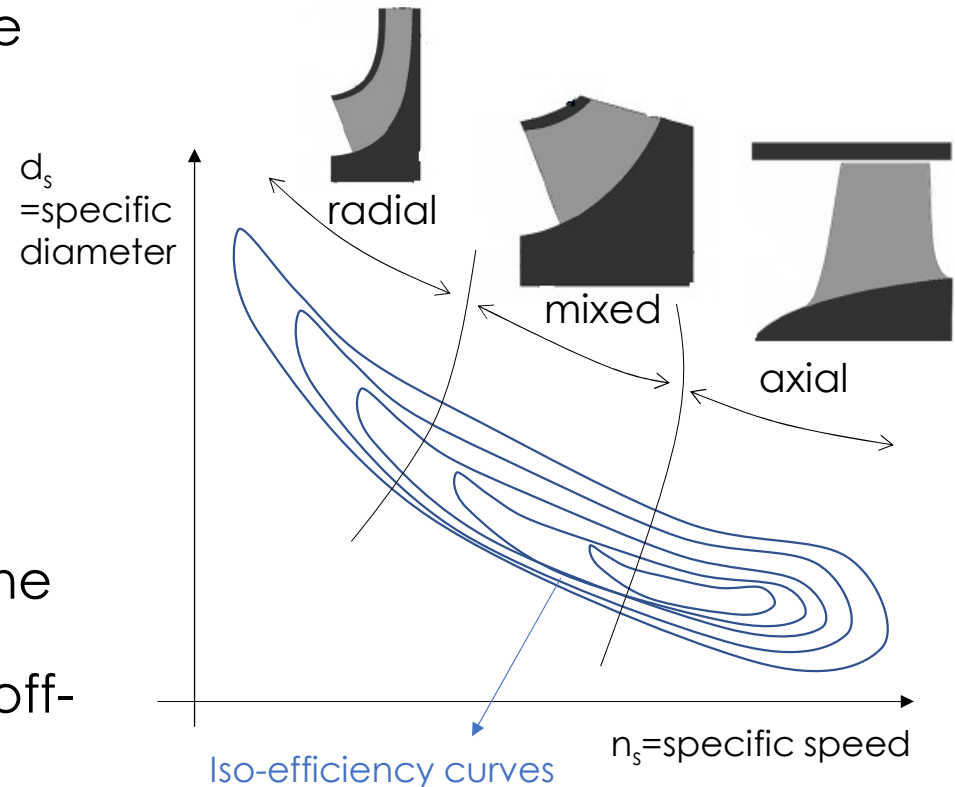
- The indirect cycle model uses two-stage compressor with intercooling.

Source: NETL

# Background

## Deciding on the Compression Method

- A Baije chart is used to determine the compression type.
- The compressor type is dependent on
  - Mass (or volumetric) flowrate to the compressor.
  - Inlet pressure and temperature.
  - Desired compression ratio.
  - Shaft speed.
- The type of the compressor affects the design methodology to be used, performance map generation, and off-design analysis.\*



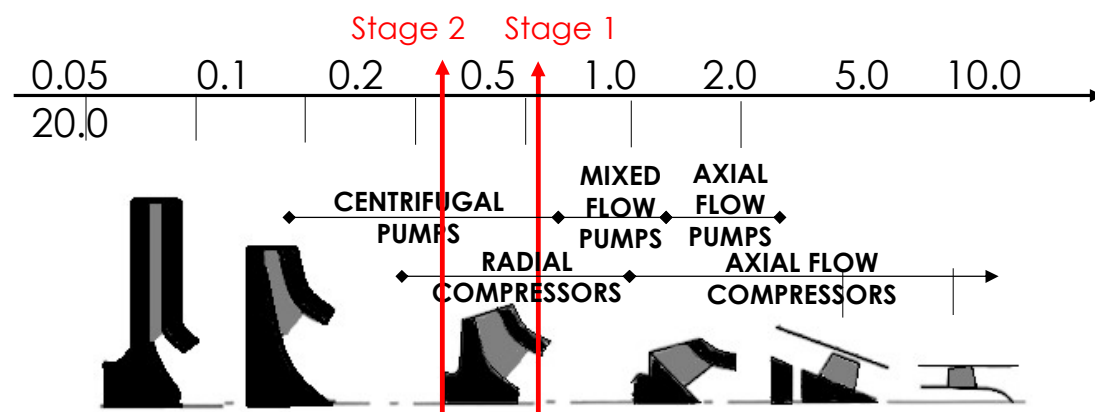
\*G. Musgrove, "Preliminary Aerodynamic Design of Centrifugal Compressors for Beginners," in SwRI Webinar Presentations, 2020

# Background

## Deciding on the Compression Method (continued)

- The calculations are updated with Stage 1 and Stage 2 data from the recent cycle optimization studies.

	$\dot{V}$ (ft <sup>3</sup> /s)	$\bar{z}$	$T_{t,in}$ (F)	$\pi_c$	$\gamma$	Ientropic Head Coefficient $H$ (ft.lbf/lbm)	Specific Speed $n_s$
Stage 1	135	0.233	71.44	2.484	4.479	5744	1.057
Stage 2	114	0.488	71.44	2.506	2.464	11114	0.6



$$H = \frac{\bar{z}RT_{t,in}}{\gamma - 1/\gamma} \left[ \pi_c^{\gamma-1/\gamma} - 1 \right]$$

$$n_s = \frac{\omega\sqrt{\dot{V}}}{(H)^{3/4}}$$

# Fluid Similarity Method



## Introduction

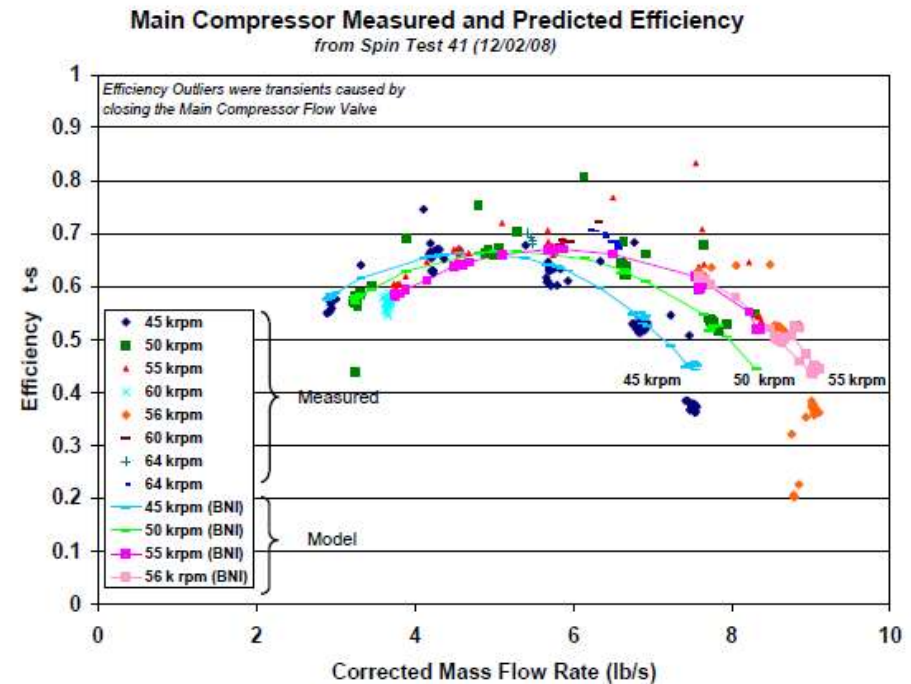
- Fluid similarity is frequently used in experiments to replace the actual fluid with an alternate fluid due to availability, safety or cost.
- Fluid similarity can be used in simulations and models for easier modelling (e.g., to use ideal gas models for real gas flows).
- Transcritical operation of the main compressor requires real gas and “calorically imperfect” gas modelling.
- Sandia National Lab’s (SNL) compressor is designed using this methodology.



# Fluid Similarity Method

## Level of Uncertainty of the Method

- SNL compared the measured compressor performance maps to the maps generated by using the fluid similarity method.\*
- The design was made with a refrigerant fluid, and performance maps are generated with NASA CCODEP code.\*
- For the efficiency, the difference between the actual data and model prediction with fluid similarity is within 5%.
- SNL concluded that the fluid similarity approach is applicable and gives results close to actual compressor performance.\*



Source: Sandia National Laboratories\*

\*Wright S.A., Radel R.F., Vernon M.E., Rochau G.E. and Pickard P.S., (2010), "Operation and Analysis of a Supercritical CO<sub>2</sub> Brayton Cycle", Sandia Report, SAND2010-0171, Albuquerque, NM

# Fluid Similarity Method

## Definition

- The method is analogous to Laplace or Fourier transforms for differential equations.

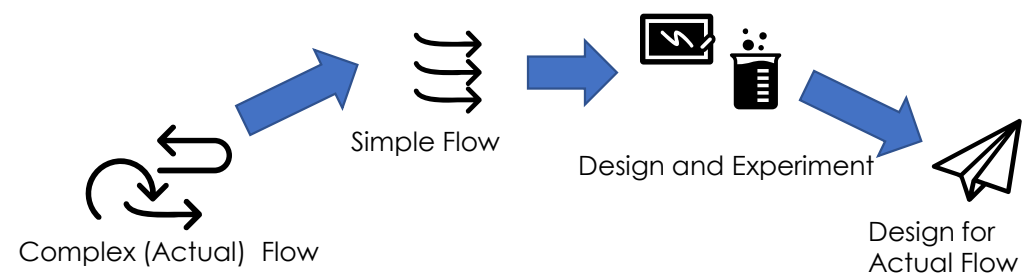
## Mathematics

- If the differential equation meets several requirements, it can be represented in either Laplace or Fourier domains.
- In the Laplace or Fourier domains, the equation is linear, and the solutions are simple.
- The solution of the transformed equation is then converted back to the real domain to obtain the actual solution.

$$\begin{array}{l}
 \mathcal{L} \left[ \frac{d^2y}{dt^2} - 5\frac{dy}{dt} + 6y = 0 \right. \\
 \left. y'(0) = 2 \quad y(0) = 2 \right] \rightarrow s^2Y(s) - 5sY(s) + 6Y(s) - 2s - 2 = 0 \\
 \rightarrow Y(s) = \frac{4}{s-2} + \frac{-2}{s-3} \xrightarrow{\mathcal{L}^{-1}} y(t) = 4e^{2t} - 2e^{3t}
 \end{array}$$

## Fluid Dynamics

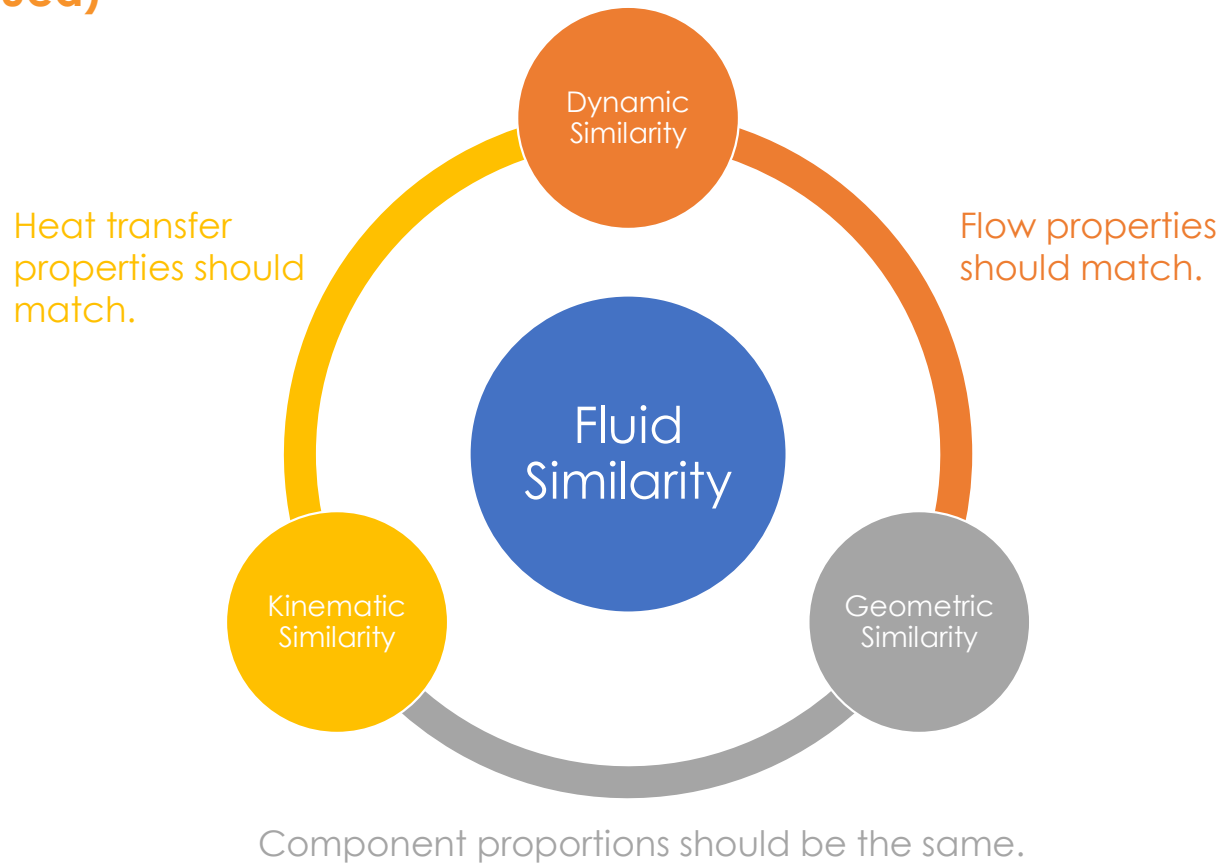
- If the actual fluid meets several conditions, the flow can be represented with another fluid.
- The “similar fluid” is both an ideal and calorically perfect gas, for which modelling is easier and well known.
- The solution obtained with the “similar fluid” is transformed back by scaling laws to obtain the solution for the actual fluid.





# Fluid Similarity Method

## Definition (continued)



# Fluid Similarity Method

## Finding Similar Fluids for sCO<sub>2</sub>

- The similar fluid should have the same following properties as the actual fluid. \*,\*\*

- Reynolds Number

In order to have equivalent flowrate that would yield identical inlet and exit flow angles with actual flow. This will partially satisfy geometrical similarity.

$$Re_D = \frac{\rho V D}{\mu}$$

Density → ρ  
Flow Speed → V  
Dynamic Viscosity → μ

- Prandtl Number Behavior

In order to have similar heat transfer scheme with the actual flow. Ensures same heat transfer boundary layer behavior.

$$Pr = \nu / \alpha$$

Kinematic Viscosity → ν  
Thermal Diffusivity → α

\*Nichols K.E., "How to Select Turbomachinery for your Application", Barbera-Nichols Inc.

\*\*Munson B.R., Young D.F. and Okiishi T.H., (2006), "Fundamentals of Fluid Mechanics", 5th Edition (International), John Wiley and Sons Inc., pp. 371-389

# Fluid Similarity Method



## Finding Similar Fluids for sCO<sub>2</sub> (continued)

- A study by University of Pisa\* researched several fluids for replacing supercritical CO<sub>2</sub> with an alternate fluid for experimental setups.
- The research was made amongst various fluids that have properties tabulated in well known databases such as REFPROP.
- Prandtl number behavior of various fluids is analyzed in the study.
- The following fluids were identified as the best candidates to be similar to sCO<sub>2</sub>.
  - Ammonia (NH<sub>3</sub>).
  - Air.
  - Freon/Refrigerant 23 (CHF<sub>3</sub>).
  - Water (H<sub>2</sub>O).

\*Pucciarelli A. and Ambrosini W., (2020), "A Successful General Fluid-to-Fluid Similarity Theory for Heat Transfer at Supercritical Pressure", *International Journal of Mass and Heat Transfer*, Vol.159, 120152, Elsevier Inc.

# Fluid Similarity Method

## Finding Similar Fluids for sCO<sub>2</sub> (continued)

- Main Compressor inlet flow Reynolds number is calculated for Stage 1 and Stage 2.
- The volumetric flowrate should be equal for both fluids to ensure the flow velocities are equivalent.
- REFPROP\* is used for the candidate fluids to find the matching flow conditions with sCO<sub>2</sub>.
- At the matched Reynolds number, the similar fluid should be:
  - Ideal gas.
  - Calorically perfect gas.
  - In gas or supercritical phase.
- Water and ammonia are eliminated due to their being liquid and non-ideal at the matched conditions.

\*NIST REFPROP v10

# Fluid Similarity Method

## Finding Similar Fluids for sCO<sub>2</sub> (continued)



	sCO <sub>2</sub>	Air	CHF <sub>3</sub> (Freon)
Pressure [psia]	887	3550	5510
Temperature [F]	71.44	22	260
Compressibility Factor	0.144	1.03	0.95
Sp. Heat Ratio	4.479	1.197	1.56
Density [lbm/ft <sup>3</sup> ]	47.285	19.249	54.291
Mass Flowrate [lbm/s]	6383	2599	7329
Volumetric Flowrate [ft <sup>3</sup> /s]	135	135	135
Reynolds Number	65.7E6	65.7E6	65.7E6

- Air mass flowrate at matched conditions is significantly different due to the difference in density.
- Using air as the similar fluid would cause significant geometrical differences (scaling would be problematic).
- Freon mass flowrate at matched conditions is close to sCO<sub>2</sub>; designed geometry will be “similar.”
- The density of Freon is very close to that of sCO<sub>2</sub>, making scaling of the maps easier and less error prone.

# Fluid Similarity Method



## Turbomachinery Design Similarity

- Reynolds number matching satisfies dynamic similarity only.
- To have kinematic similarity, the following design specs of the compressor should be matched with the similar fluid:\*

  - Head Coefficient
    - Ensures that the forces and pressures acting on the turbo component will be similar to the actual flow.
  - Specific Speed
    - Ensures that the flow coefficient and velocity triangles of the compressor design made for similar fluid will be similar to the actual flow.

- If the above two criteria are satisfied, then the geometric similarity is also assured.\*

\*Nichols K.E., "How to Select Turbomachinery for your Application", Barbera-Nichols Inc.

# Fluid Similarity Method

## Turbomachinery Design Similarity (continued)

- For the “Freon compressor,” the following should be the same as the “sCO<sub>2</sub> compressor” to satisfy kinematic similarity:
  - Shaft Speed.
  - Volumetric Flowrate.
- Equivalent compressor pressure ratio can be found by equating the head coefficients for two flow cases:

$$\frac{\bar{z}RT_{t,in}}{\gamma - 1/\gamma} \left[ \pi_c^{\gamma-1/\gamma} - 1 \right] = H = \frac{\bar{z}^*R^*T_{t,in}^*}{\gamma^* - 1/\gamma^*} \left[ \pi_{c^*}^{\gamma^*-1/\gamma^*} - 1 \right]$$
$$\frac{\omega\sqrt{\dot{V}}}{(H)^{3/4}} = n_s = \frac{\omega^*\sqrt{\dot{V}^*}}{(H)^{3/4}}$$

sCO<sub>2</sub>  Freon



# Map Scaling

## Affinity Laws

- Turbomachinery scaling is used frequently for performance map scaling of similar compressors and pumps.
- If the two pumps or compressors are geometrically close in terms of design, then the performance map of one machine can be used to estimate the performance of the other one.
- Scaling laws can be used to scale different fluid operation cases.
- Affinity Laws are used to scale the pressure ratio, isentropic efficiency, or head coefficient.
- In this context, the scaling laws are used to scale the maps from the Freon compressor to  $s\text{CO}_2$  compressor.

# Map Scaling

## Pressure Ratio Scaling

- The head coefficient of the sCO<sub>2</sub> compressor will be equal to the Freon compressor (from fluid similarity principles).\*
- Pressure ratio scaling formula is then found by using the above principle as follows:

$$\pi_c = \left\{ 1 + \frac{z_{CHF_3} \gamma_{CHF_3} R_{CHF_3} T_{CHF_3}}{z_{CO_2} \gamma_{CO_2} R_{CO_2} T_{CO_2}} \frac{\gamma_{CO_2} - 1}{\gamma_{CHF_3} - 1} \left[ \pi_C^{*(\gamma_{CHF_3} - 1) / \gamma_{CHF_3}} - 1 \right] \right\}$$

- The formula is used for each point in the Freon compressor pressure ratio ( $\pi_C^*$ ) vs. mass flowrate map curve.
- The mass flowrate for sCO<sub>2</sub> is scaled using the density ratio of two fluids.

\*Nichols K.E., "How to Select Turbomachinery for your Application", Barbera-Nichols Inc.

# Map Scaling

## Isentropic Efficiency Scaling

- The isentropic efficiency is scaled by using the following formula\*:

$$\frac{1 - \eta_{CHF_3}}{1 - \eta_{CO_2}} = \left( \frac{d_{2,CO_2}}{d_{2,CHF_3}} \right)^n$$

- Although geometrically “similar”, the impeller diameter ( $d_2$ ) of the Freon compressor is not exactly equal to  $sCO_2$  compressor.
- The wheel speed of the two compressors are proportional to the diameter ratio.
- The wheel speed equation is used to calculate the diameter ratio in the scaling formula
$$\left\{ \frac{h_{t1} \left( \pi_c^{(\gamma-1)/\gamma e_c} - 1 \right)}{\varepsilon} \right\}_{CO_2} = \frac{d_{2,CHF_3}}{d_{2,CO_2}} \left\{ \frac{h_{t1} \left( \pi_c^{(\gamma-1)/\gamma e_c} - 1 \right)}{\varepsilon} \right\}_{CHF_3}$$
- The coefficient “n” is calculated for each stage separately. It is calculated by using the efficiency scaling formula at the design point.

\*Nichols K.E., “How to Select Turbomachinery for your Application”, Barbera-Nichols Inc.

# Validation



## Validation of the Proposed Methodology

- Although the fluid similarity method has been used and validated by SNL, there are some variations in the application of the method in this study—mainly in the map scaling.
- The compressor design by SNL was used in the method validation procedure.
- The inlet flow analysis showed that the similar fluid for this compressor should be “air.”
- The in-house compressor design code was used to design the compressor for similar fluid conditions.

# Validation

## Compressor Design Procedure

- The scaling formulas are then used for scaling the air compressor dimensions to the sCO<sub>2</sub> compressor.
- The scaled compressor dimensions are then compared to the SNL compressor design.
- Per the fluid similarity laws, the flow angles should be the same for both the air and sCO<sub>2</sub> cases.

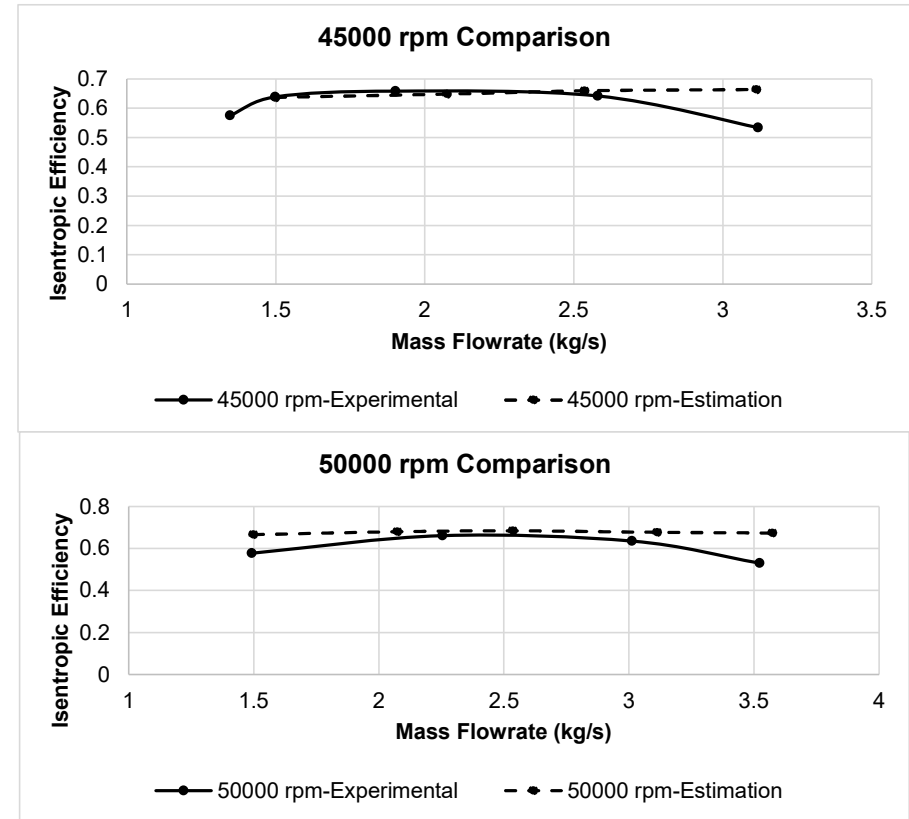
Parameter	Current Study		SNL*
Flow	Air	sCO <sub>2</sub>	sCO <sub>2</sub>
Impeller Diameter, $d_2$	0.068 m	0.048 m	0.051 m
Impeller Length, $L$	0.03 m	0.02 m	0.02 m
Inlet Tip Diameter, $R_{1t}$	0.01 m	0.008 m	0.009 m
Impeller Inlet Angle, $\beta_1$	57°	57°	50°
Impeller Exit Angle, $\beta_2$	49°	49°	50°
Throat Diameter, $b_2$	0.001 m	0.0007 m	0.0008 m
Exit Flow Angle, $\alpha_3$	72.6°	72.6°	71.5°
Number of Blades	13	13	12

\*Wright S.A., Radel R.F., Vernon M.E., Rochau G.E. and Pickard P.S., (2010), "Operation and Analysis of a Supercritical CO<sub>2</sub> Brayton Cycle", Sandia Report, SAND2010-0171, Albuquerque, NM

# Validation

## Map Scaling Methods

- NASA CCODP Code was used with the air compressor design parameters.
- The performance maps for the pressure ratio and isentropic efficiency were generated for the air compressor.
- The performance maps are then scaled to sCO<sub>2</sub> per the previously described methodology.
- Experimental off-design data of the SNL compressor for isentropic efficiency at various shaft speeds are used in map scaling validation.



# Compressor Design



## Design Methodology

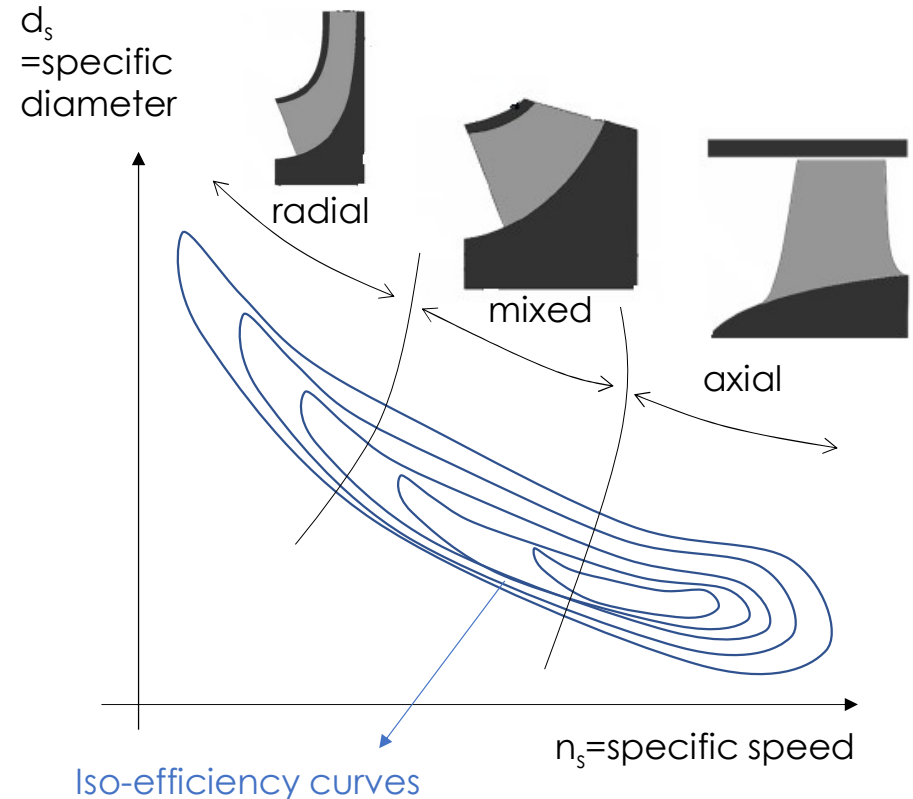
- Freon compressor is designed at the matched Reynolds number conditions with  $s\text{CO}_2$ .
- The in-house design code was used to design the compressor stages by using mean-line design principles.
- Freon thermodynamic properties are used in the design code.
- No changes to design equations made; Freon is an ideal and calorically perfect gas.
- A feasible design was made using centrifugal compressor industry design practices and a Baije chart.



# Compressor Design

## Design Methodology (continued)


- Baije chart is used initially to find initial design parameters such as slip factor, shaft speed, and specific diameter.
- Shaft speed is important; it affects all the design parameters.
- Two options are identified for compressor design shaft speed.
  - Fixed at 3600 rpm (advantageous for turbine coupling).
  - High rpm (higher efficiency).



# Compressor Design

## Radial Compressor Design Options

### For Highest Efficiency (average)

- Rotational speed: 16500 rpm
- Impeller Length: 15.5" 
- Slip Factor: 0.8
- Polytropic Efficiency: 0.84–0.87
- 2-stage compressor with intercooler (1 stage + Intercooling + 1 Stage)

### For Keeping Shaft Speed at 3600 rpm (average)

- Rotational speed: 3600 rpm
- Impeller Length: 31.5"
- Slip Factor: 0.85
- Polytropic Efficiency: 0.8–0.83
- 6-stage compressor with intercooler (3 stages + Intercooling + 3 stages)

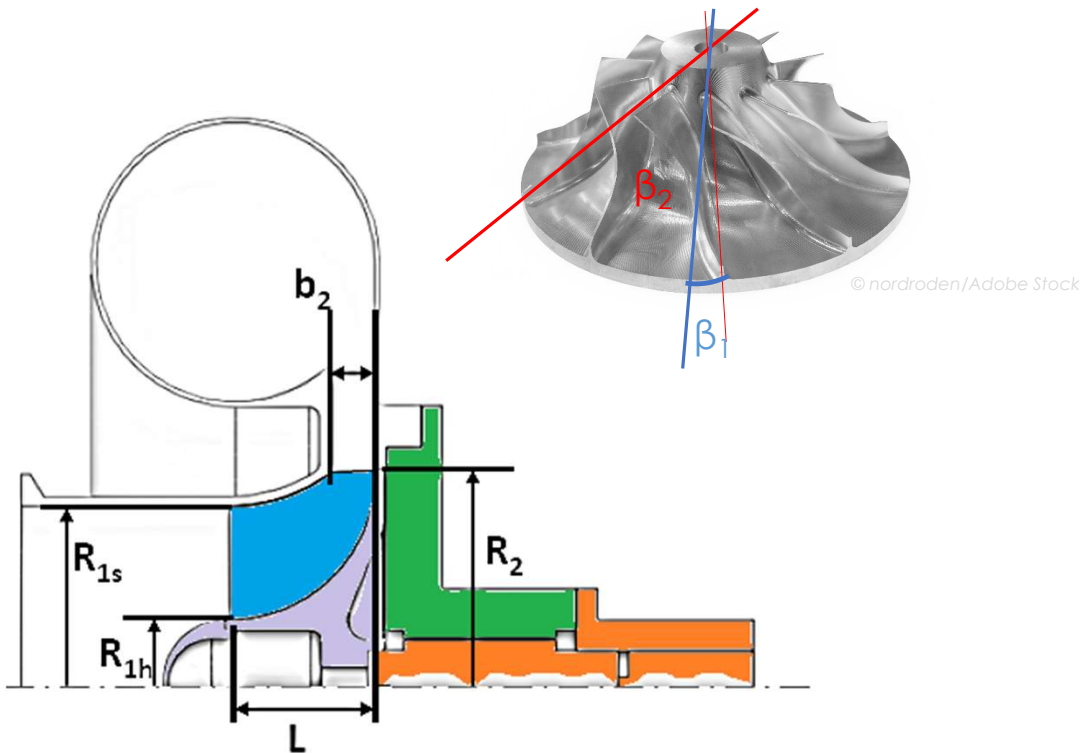
# Compressor Design

## Applied Design Standards

- Several design standards from SwRI tutorials, Aungiers, Wiesner et al., and Walsch et al. are adapted.
- Some design criteria used:
  - Mean Inlet Mach Number = 0.4-0.6
  - Impeller Backsweep Angle  $< 40^\circ$
  - Inducer hub-to-tip ratio = 0.35-0.5
  - Exit flow speed  $< 500$  m/s
  - Impeller Diameter  $< 0.8$ m [a manufacturability limit]
  - Exit Flow Mach Number  $< 0.2$
  - Slip Factor = 0.8-0.95

# Compressor Design

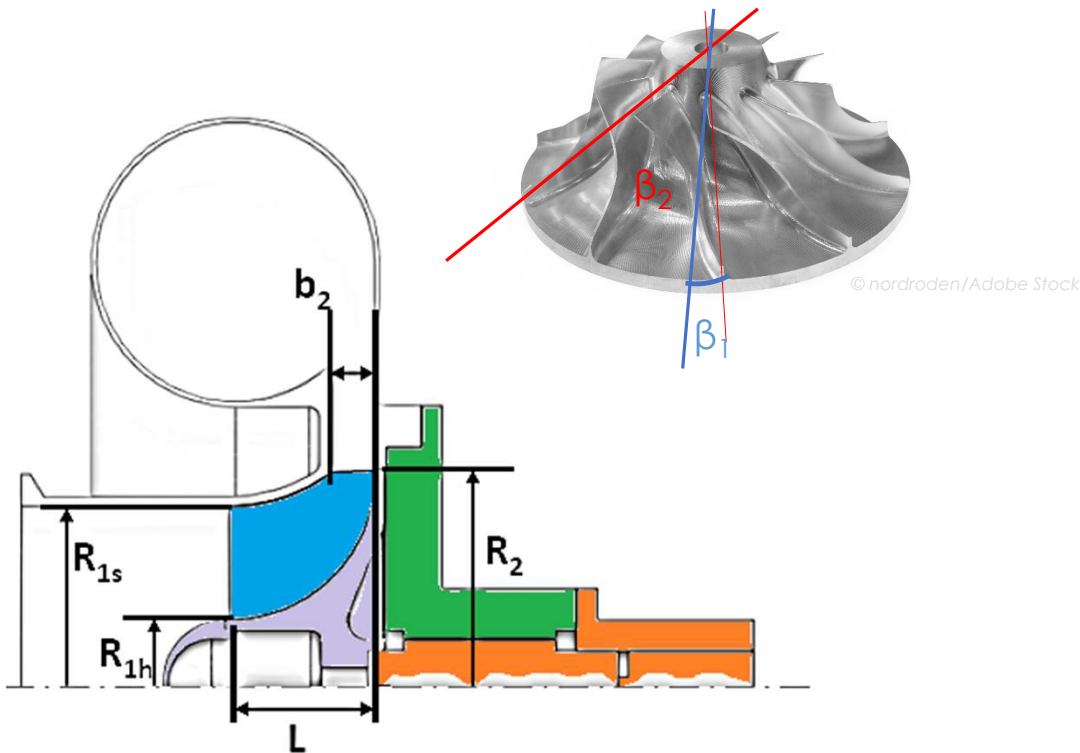
## Stage 1 Design



Parameter	Value
Inlet Hub Diameter, $R_{1h}$	2.64"
Inlet Tip Diameter, $R_{1s}$	5.28"
Impeller Radius, $R_2$	7.81"
Blade Length, $L$	4.8"
Impeller Inlet Angle, $\beta_1$	$38^\circ$
Impeller Exit Angle, $\beta_2$	$32^\circ$
Slip Factor	0.81
Number of Impeller Blades	9
Throat Diameter, $b_2$	0.46"
Pressure Ratio	1.445
Isentropic Efficiency	0.78
Flow Coefficient	0.09

# Compressor Design

## Stage 2 Design



Parameter	Value
Inlet Hub Diameter, $R_{1h}$	2.39"
Inlet Tip Diameter, $R_{1s}$	4.79"
Impeller Radius, $R_2$	9.72"
Blade Length, $L$	8"
Impeller Inlet Angle, $\beta_1$	37°
Impeller Exit Angle, $\beta_2$	28°
Slip Factor	0.86
Number of Impeller Blades	15
Throat Diameter, $b_2$	0.22"
Pressure Ratio	2.013
Isentropic Efficiency	0.85
Flow Coefficient	0.04

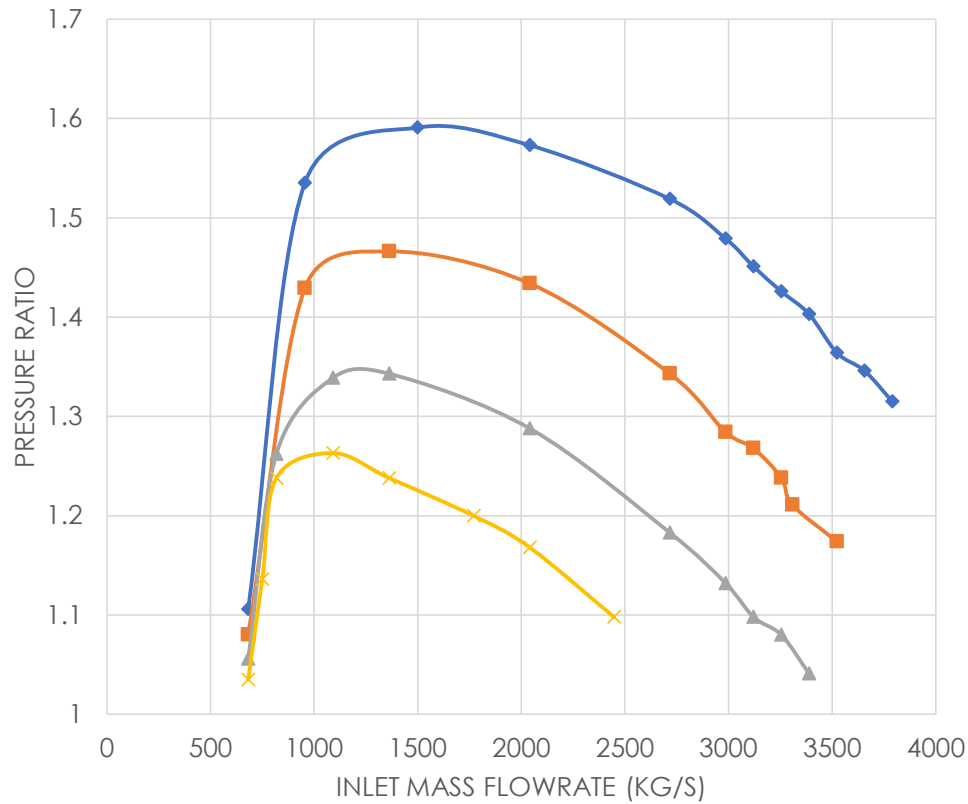
# Off-Design Maps

## Methodology

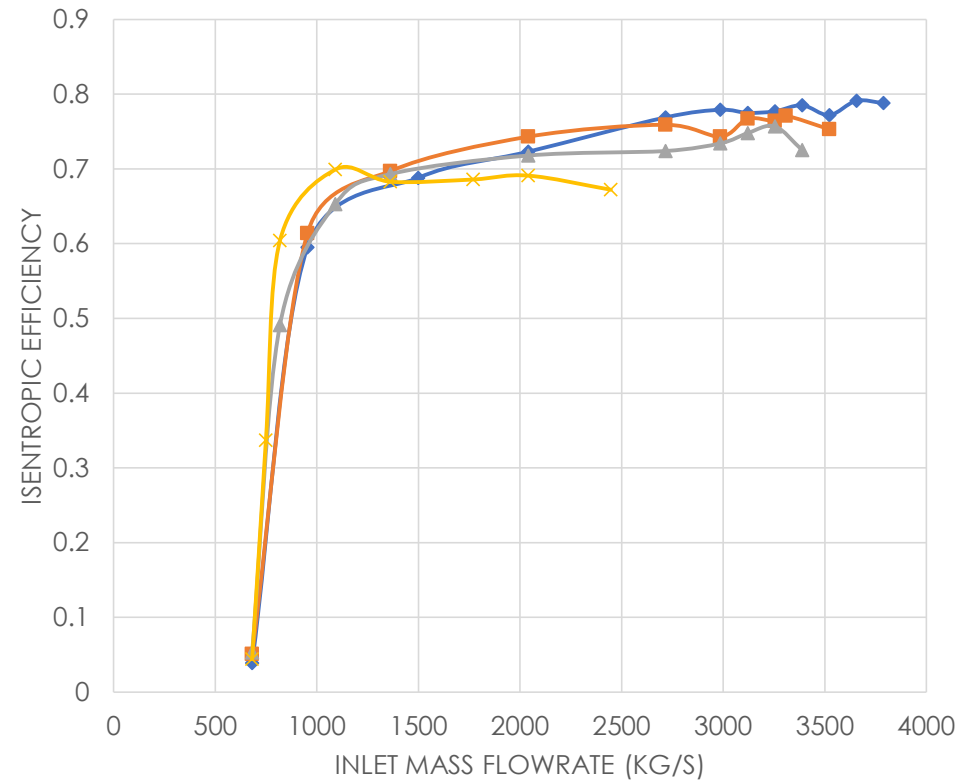
- NASA CCODP code is used to generate the off-design maps for the Freon compressor.
- No changes in the performance map calculation are made; Freon is an ideal and calorically perfect gas.
- Maps are generated for four different speeds:
  - 100% Speed (16500 rpm)-Design Speed.
  - 90% Speed (14850 rpm).
  - 80% Speed (13200 rpm).
  - 70% Speed (11550 rpm).
- Maps for pressure ratio and isentropic efficiency are generated.

# Off-Design Maps

## Stage 1



—●— 100% design rpm —■— 90% design rpm —▲— 80% design rpm —×— 70% design rpm

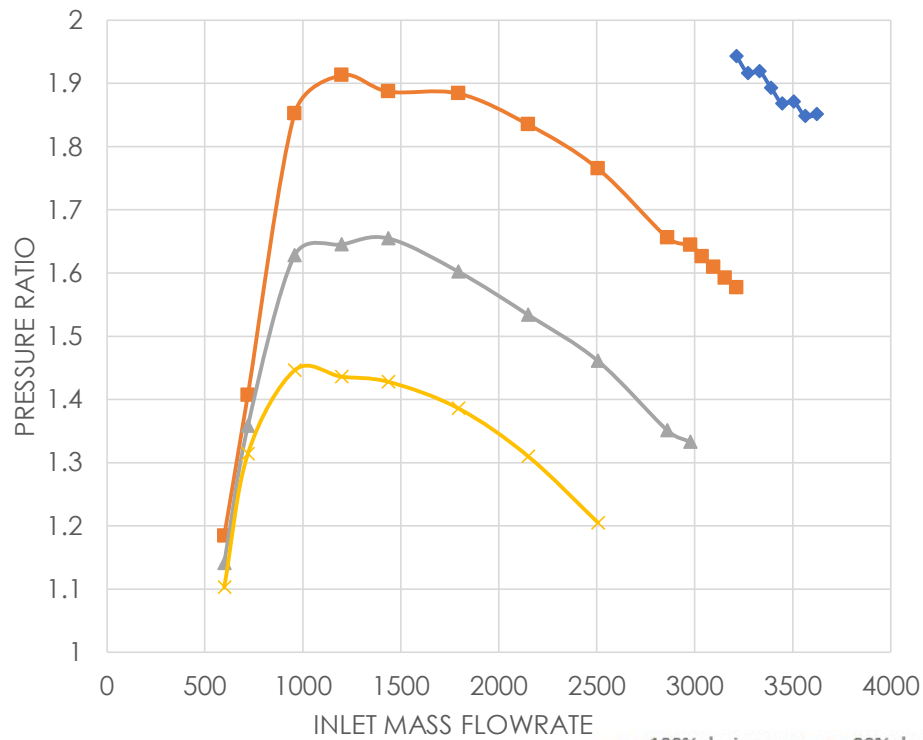




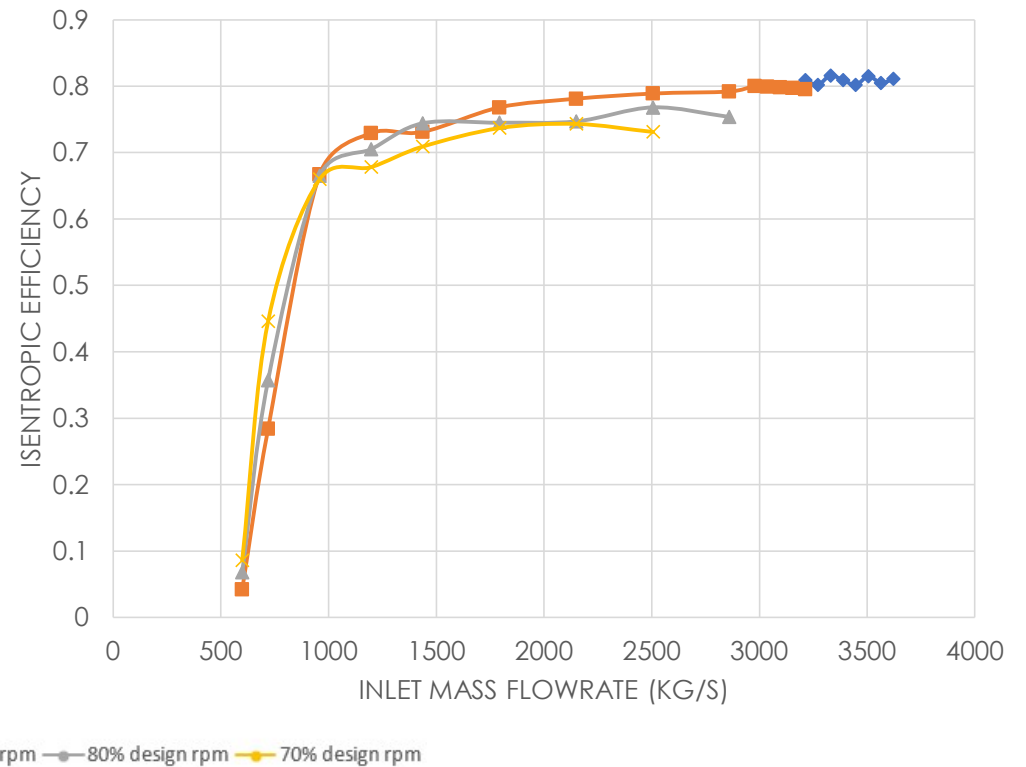
# Off-Design Maps

## Stage 2

Pressure Ratio vs. Mass Flowrate

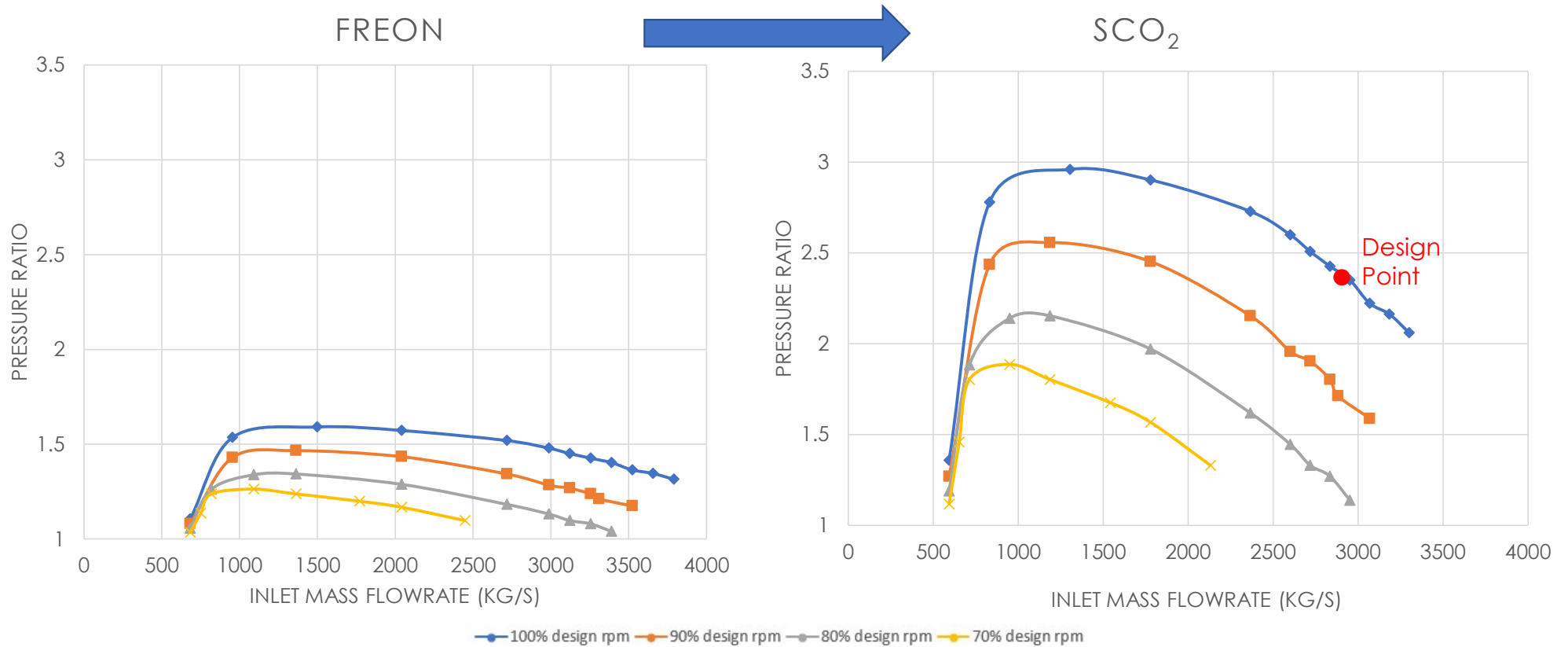


Isentropic Efficiency vs. Mass Flowrate



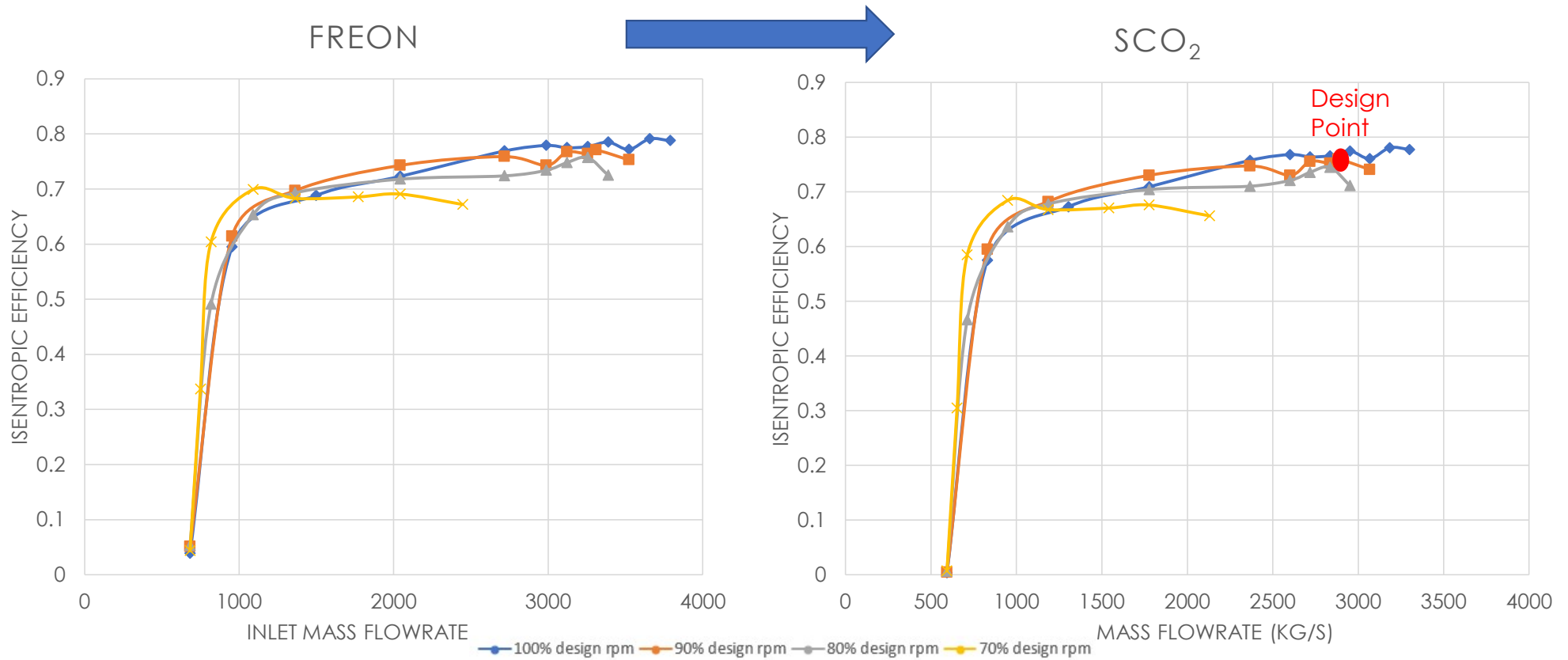
# Off-Design Maps

## Pressure Ratio Scaling



# Off-Design Maps

## Isentropic Efficiency Scaling



# Off-Design Maps

## General Comments

- Map shapes for the pressure ratio are similar to centrifugal pump maps; wide-parabolic curves.
- Similarity to pump maps is expected per Baije analysis.
- Stage 2 operational range is too narrow due to high impeller design exit Mach number (at 0.9).
- Higher impeller design Mach number increases design efficiency but reduces the operational range.
- Stage 2 will be re-designed. Two options exist for Stage 2:
  - Divide Stage 2 into two stages: reduces pressure ratio and the impeller Mach number.
  - Run Stage 2 at lower rpm: requires integrally geared compressor design (second stage will not be on the same shaft with first).

# Compressor Design Updates

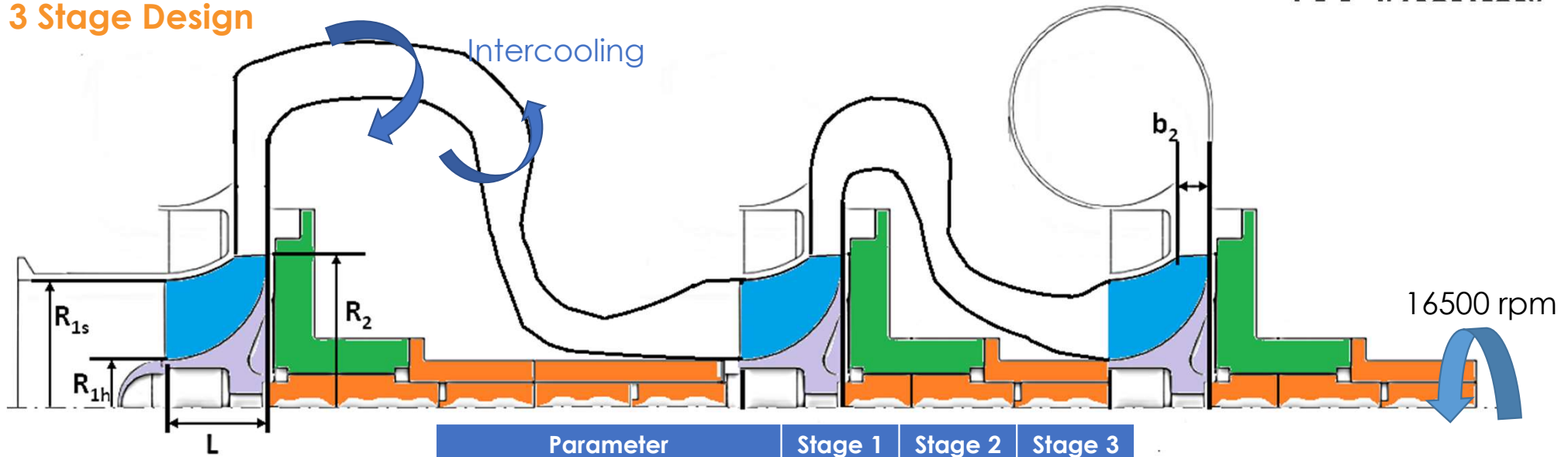


## Re-Design of Second Stage

- Second stage of two stage design had a narrow operational range due to high impeller exit Mach number.
- Second stage of the previous design is divided into two stages with each having the same pressure ratio.
- Shaft speed is the same for all stages (1 6500 rpm).
- Intercooling is applied between Stages 1 and 2 only.
- Fluid similarity method is used to design and run off-design analysis for each stage.
- Off-design maps are scaled to  $s\text{CO}_2$  with the same method used in Stage 1.

# Compressor Design Updates

## 3 Stage Design

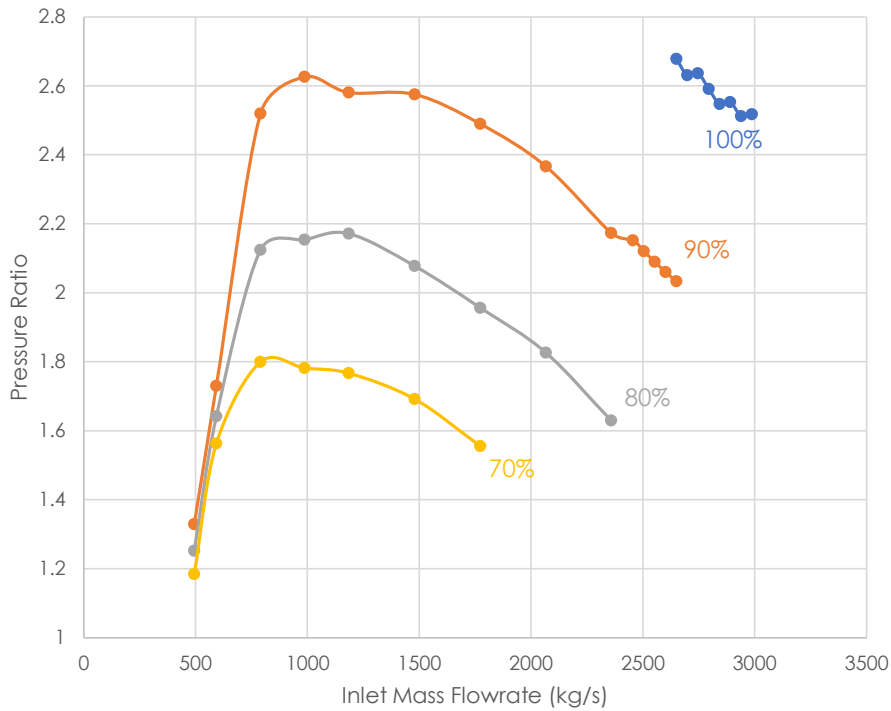


Parameter	Stage 1	Stage 2	Stage 3
Inlet Hub Diameter, $R_{1h}$	2.64"	2.39"	2.46"
Inlet Tip Diameter, $R_{1s}$	5.28"	4.79"	4.91"
Impeller Radius, $R_2$	7.81"	6.57"	7.32"
Blade Length, $L$	4.8"	3.9"	4.7"
Throat Diameter, $b_2$	0.46"	0.52"	0.39"
Number of Blades	9	9	13
Pressure Ratio (sCO <sub>2</sub> Equivalent)	2.5	1.583	1.583

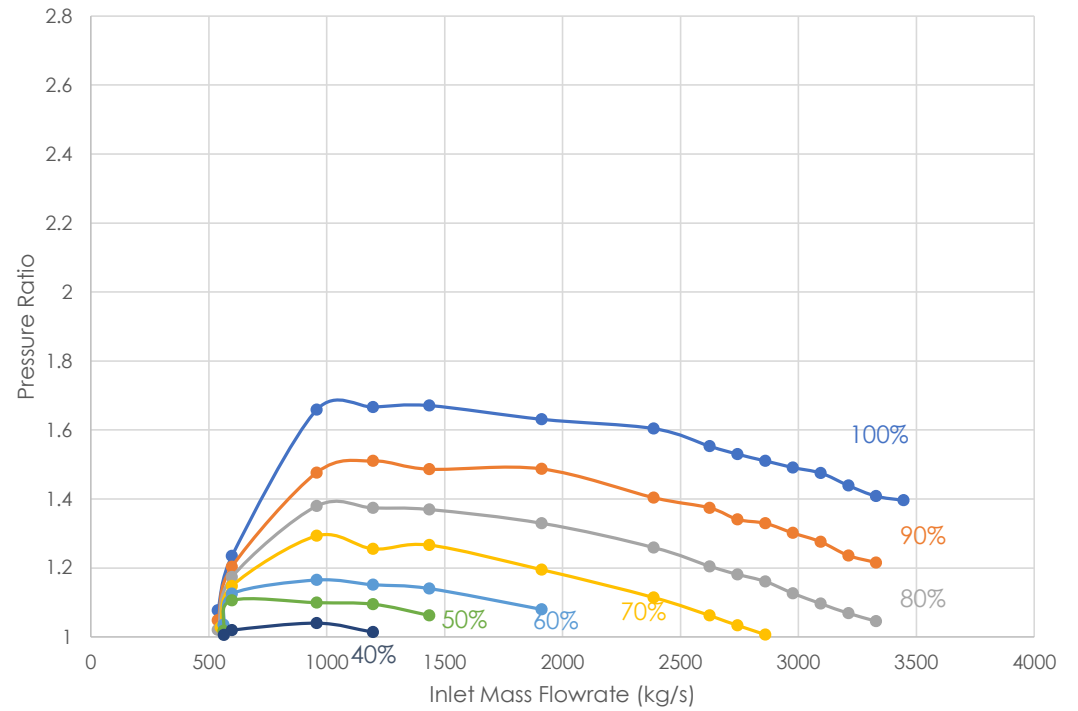
# Compressor Design Updates

## Off-Design Maps – Stage 2

sCO<sub>2</sub>-PR vs. Mass Flowrate

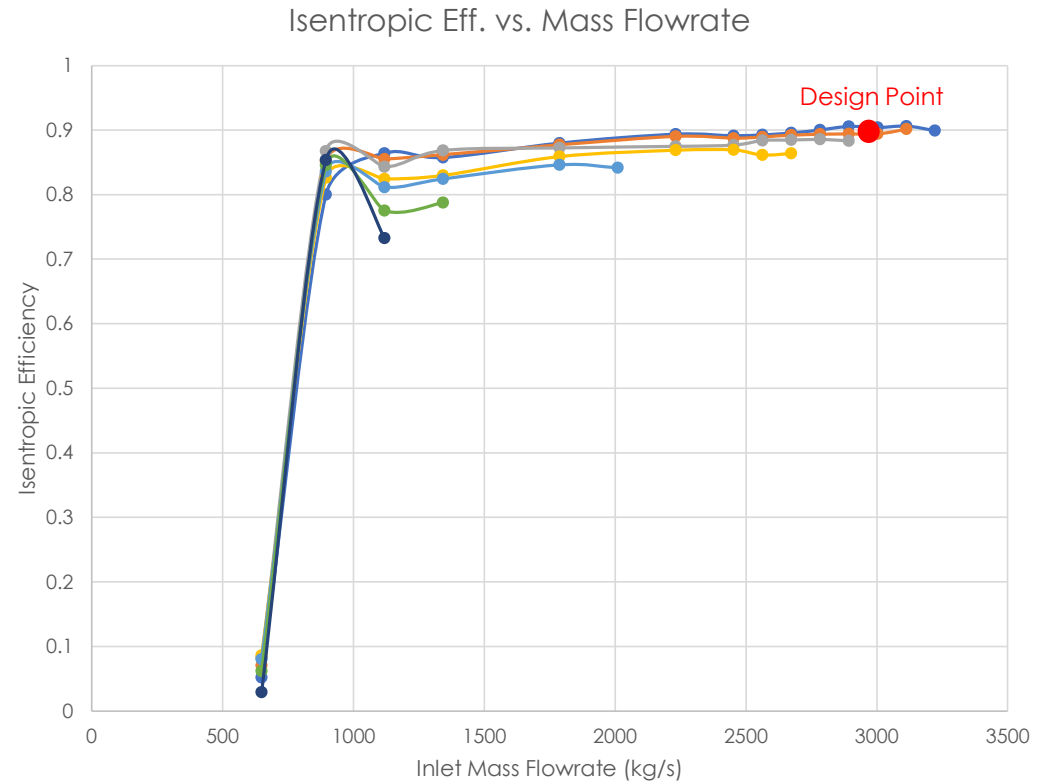
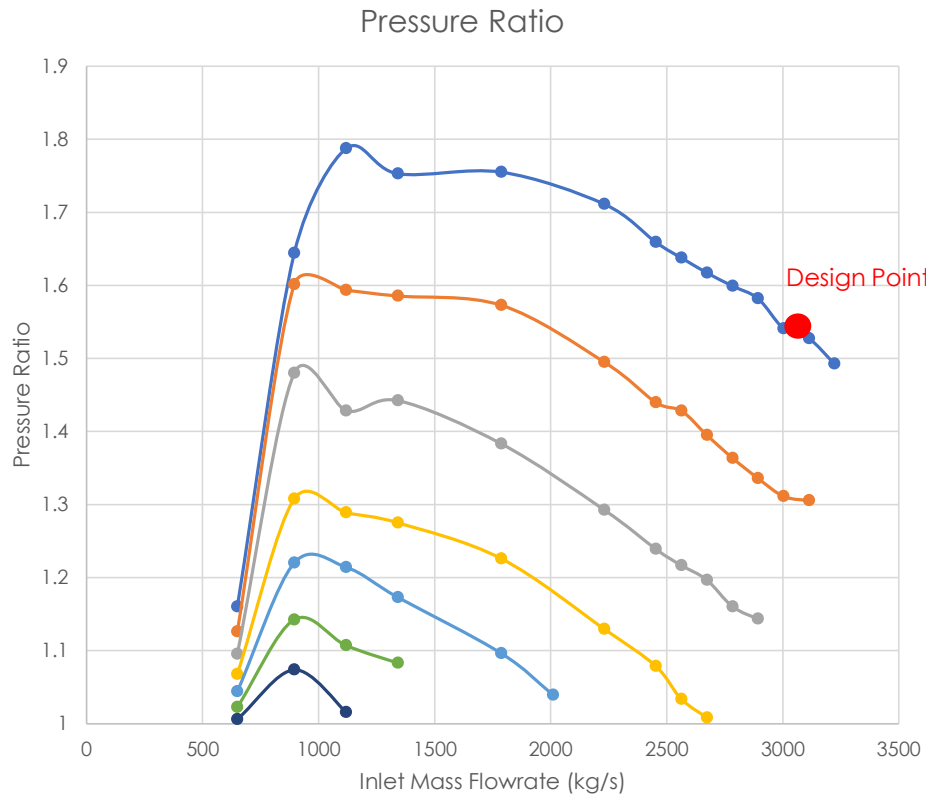


sCO<sub>2</sub>-PR vs. Mass Flowrate



# Compressor Design Updates

## Off-Design Maps – Stage 3





# Summary and Conclusions



- The fluid similarity method is used to design and generate performance maps for the indirect cycle main compressor.
- For the main compressor flow conditions, Freon is the “similar” fluid for the analysis, which is both an ideal and calorically perfect gas.
- NASA CCODP code is used to generate performance maps for the Freon compressor design.
- Maps showed centrifugal pump-like characteristics for the pressure ratio and efficiency.
- The maps are scaled for sCO<sub>2</sub> application.
- Scaled map data are used to develop Aspen Plus compressor models for each stage.

# Disclaimer



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# Questions/ Comments

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