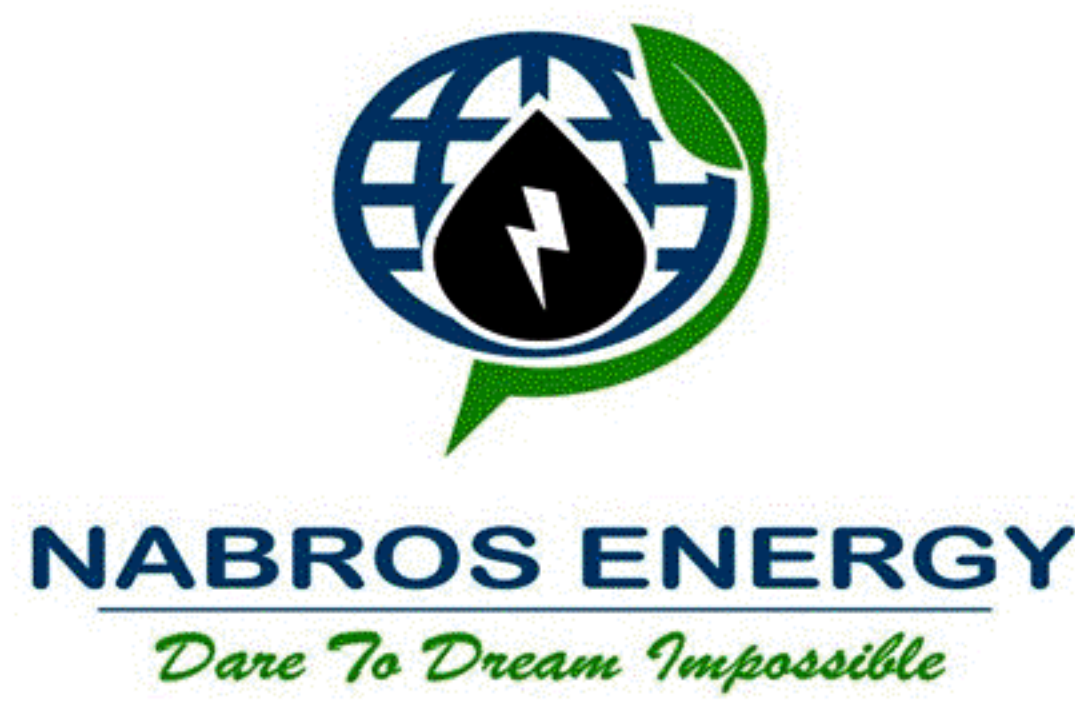


# DESIGN AND CFD ANALYSIS OF CENTRIFUGAL COMPRESSOR AND TURBINE FOR SUPERCRITICAL CO<sub>2</sub> POWER CYCLE



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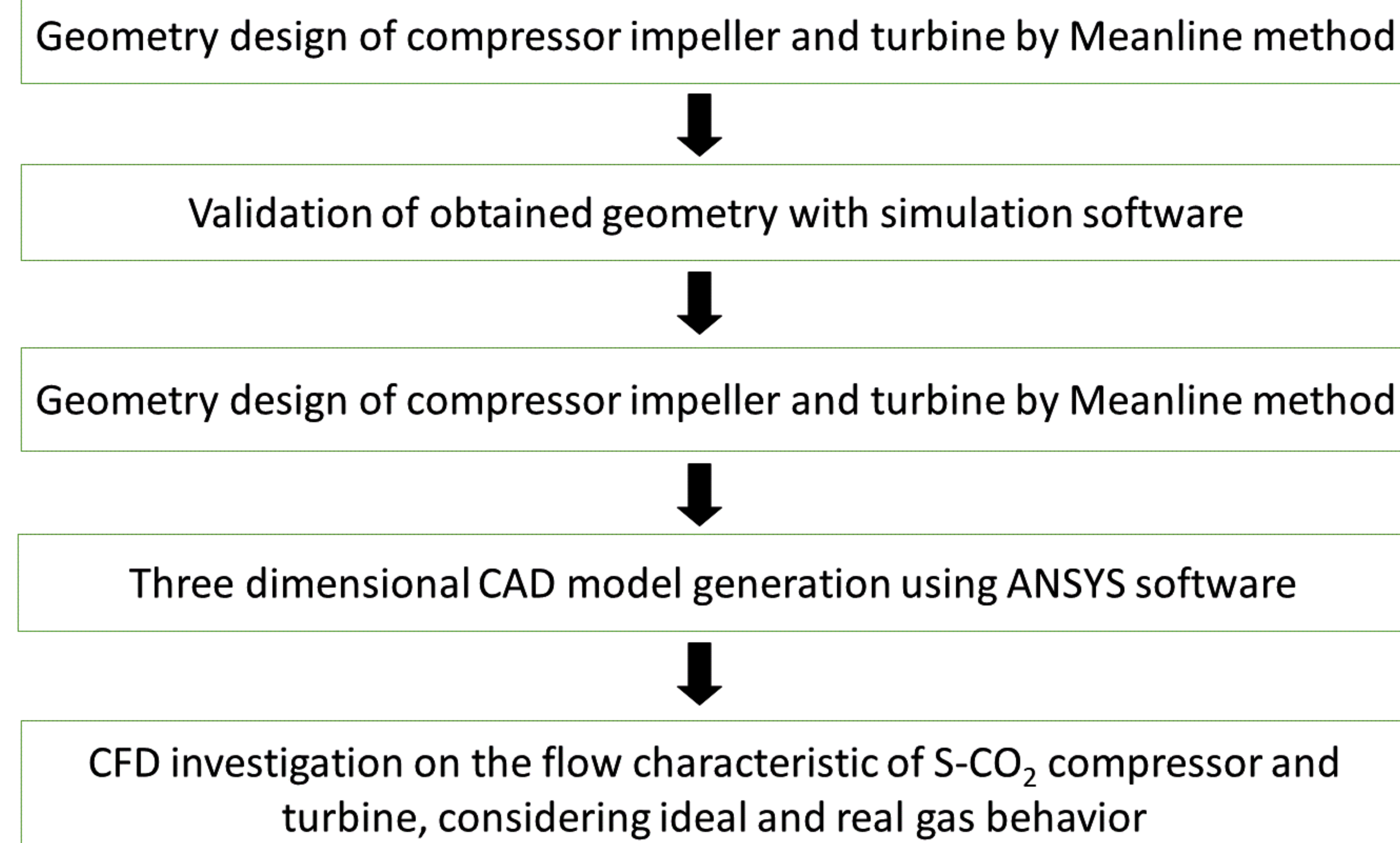
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## INTRODUCTION

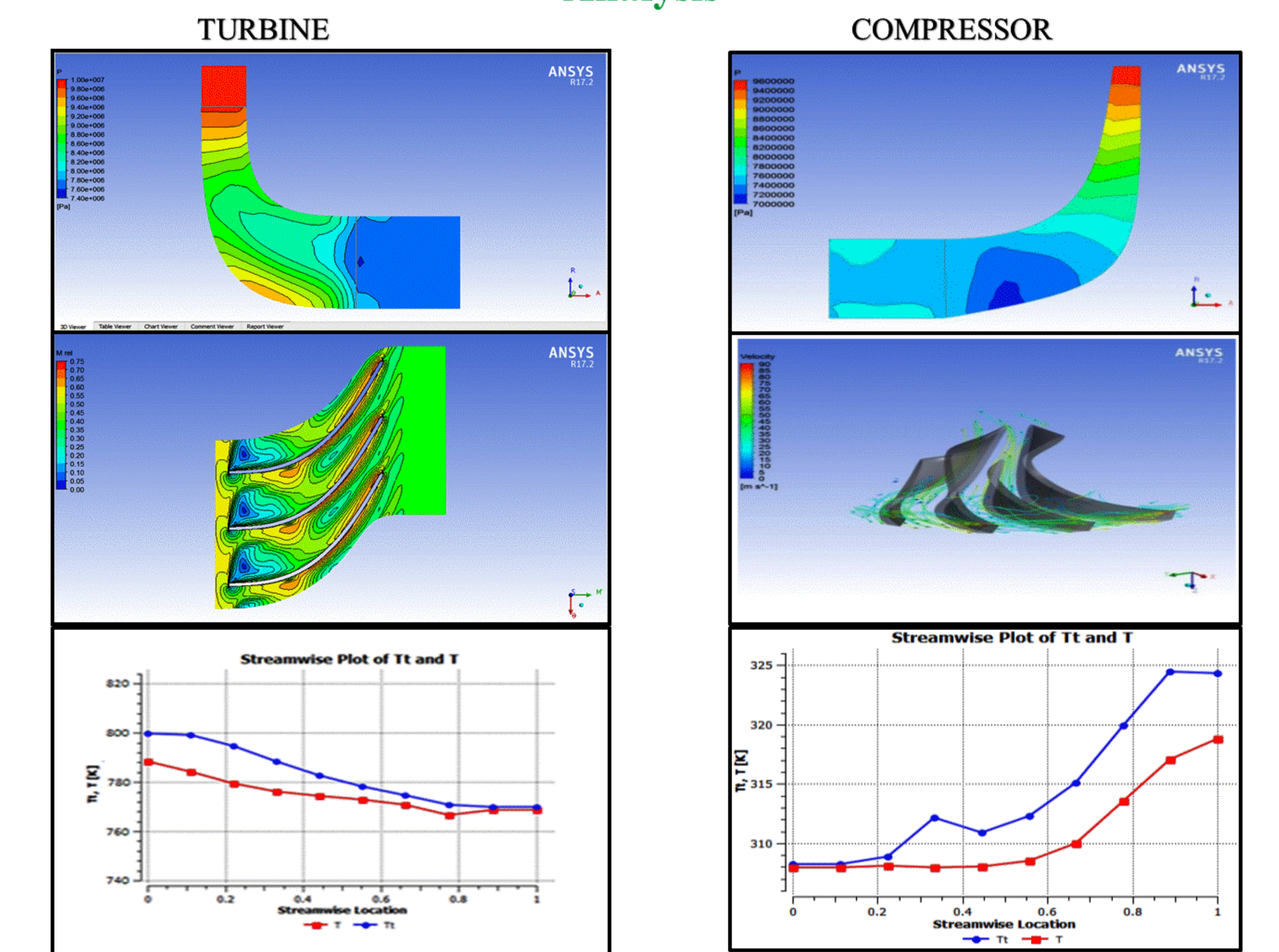
- Supercritical CO<sub>2</sub> (S-CO<sub>2</sub>) power cycles are the most promising technology for high temperature heat source namely concentrated solar thermal, nuclear, fossil fuel as well as low temperature heat source like waste heat recovery and geothermal applications.
- The main reason is lower compressibility factor of CO<sub>2</sub> near critical point (73.8 bar, 31.1 °C).
- A design and CFD analysis of the compressor and turbine for supercritical CO<sub>2</sub> has been done in the present work.
- We have developed a in-house code for meanline design of compressor and turbine, considering Aungier's loss correlation in Engineering Equation Solver (EES) for net 10 kWe power.
- The operating range of compressor, temperature is 305 to 320 K and pressure is 75 to 110 bar. Turbine inlet temperature is 800 K.
- The fluid properties were implemented via property table in the computational analysis code to simulate nonlinear behavior near the critical point of CO<sub>2</sub>.
- Overall results shows 80% isentropic efficiency of turbine and compressor, and compression work has also reduced by 50% as compared to ideal compression process.

## METHODOLOGY



General Parameter	
Reynolds Number	5*10 <sup>7</sup>
Shroud Tip mesh Method	Match Expansion at Blade Tip
Topology Mesh Technique	ATM optimized
Boundary Layer Refinement Control Factor	Proportional to Mesh Size
Near Wall Treatment	Y+ Method
Turbulence Model	K-w SST model
Number nodes and Element	
Turbine	Compressor
2,76,610 & 2,49,568	6,78,000 & 6,25,100

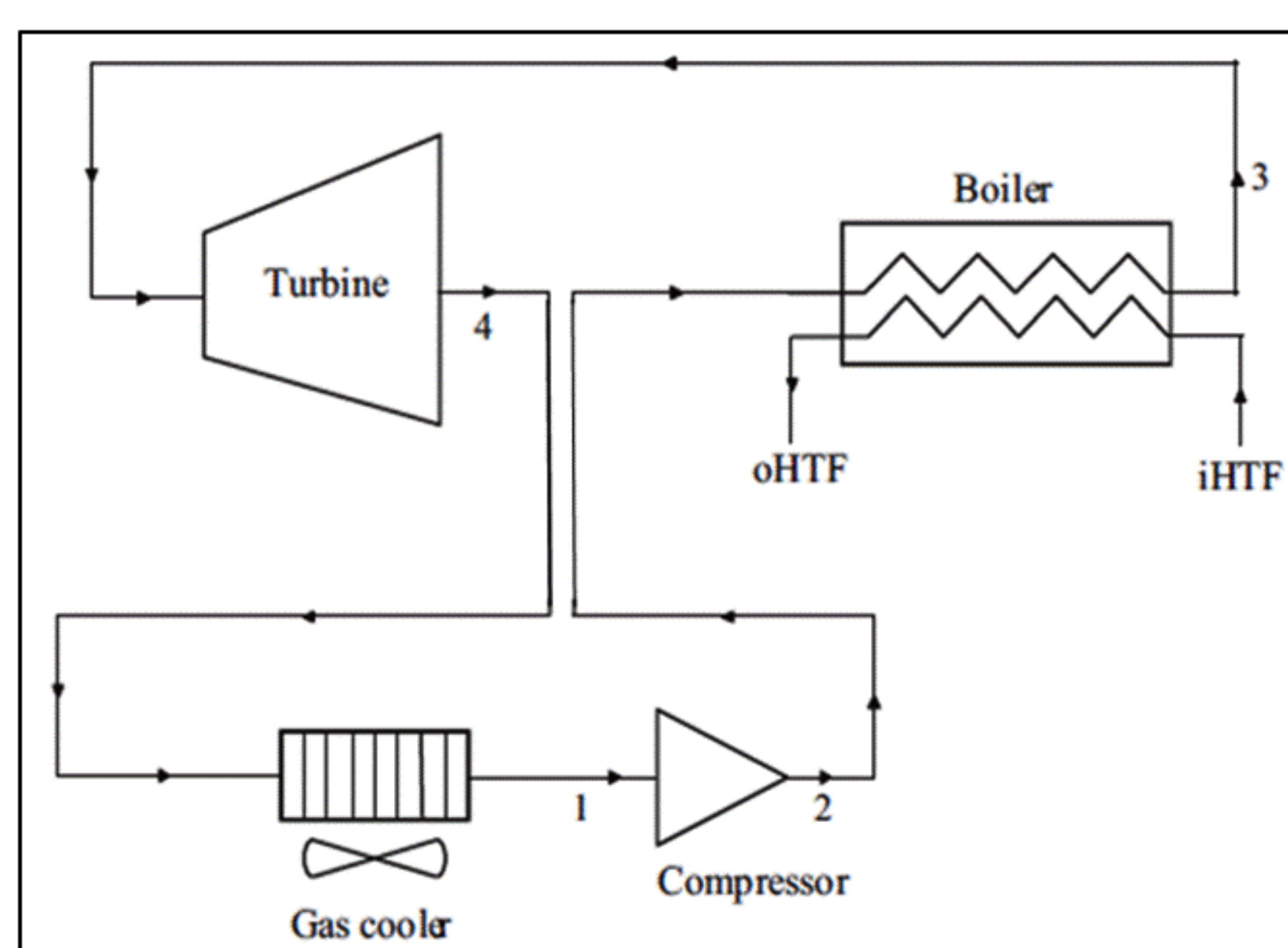
## Analysis



Comparison of thermodynamic property for Compressor for Ideal vs Real gas

Property	Location	Analysis Type	
		Meanline	Real Gas (CFD)
T <sub>static</sub> in K	In	307	307.2
	Out	326.7	318
T <sub>total</sub> in K	In	308	308
	Out	338	324
P <sub>static</sub> in bar	In	72	74
	Out	88	95
P <sub>total</sub> in bar	In	75	75
	Out	105	105
Density in Kg/m <sup>3</sup>	In	129	271.14
	Out	146	418.5

## THERMODYNAMIC ANALYSIS

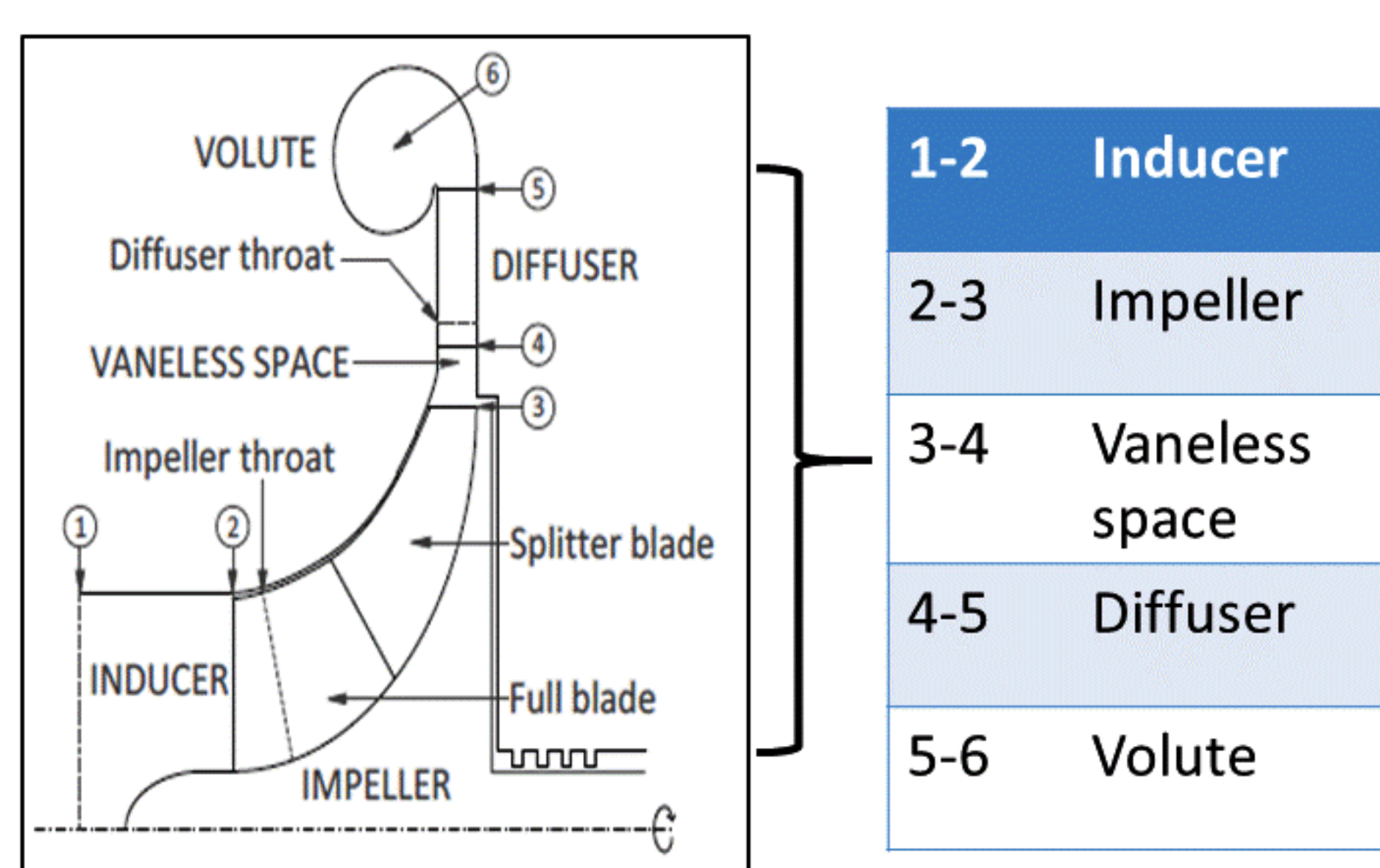


State Points	Pressure (bar)	Temperature (K)	Specific Enthalpy (kJ/kg)	Density (kg/m <sup>3</sup> )
1	75	308	396.74	274.97
2	105	331.9	409.27	335.06
3	101.3	800	1014.9	66.185
4	77.72	773.2	985.13	52.819

$$M_{wf} = \frac{30}{h_3 - h_4}$$

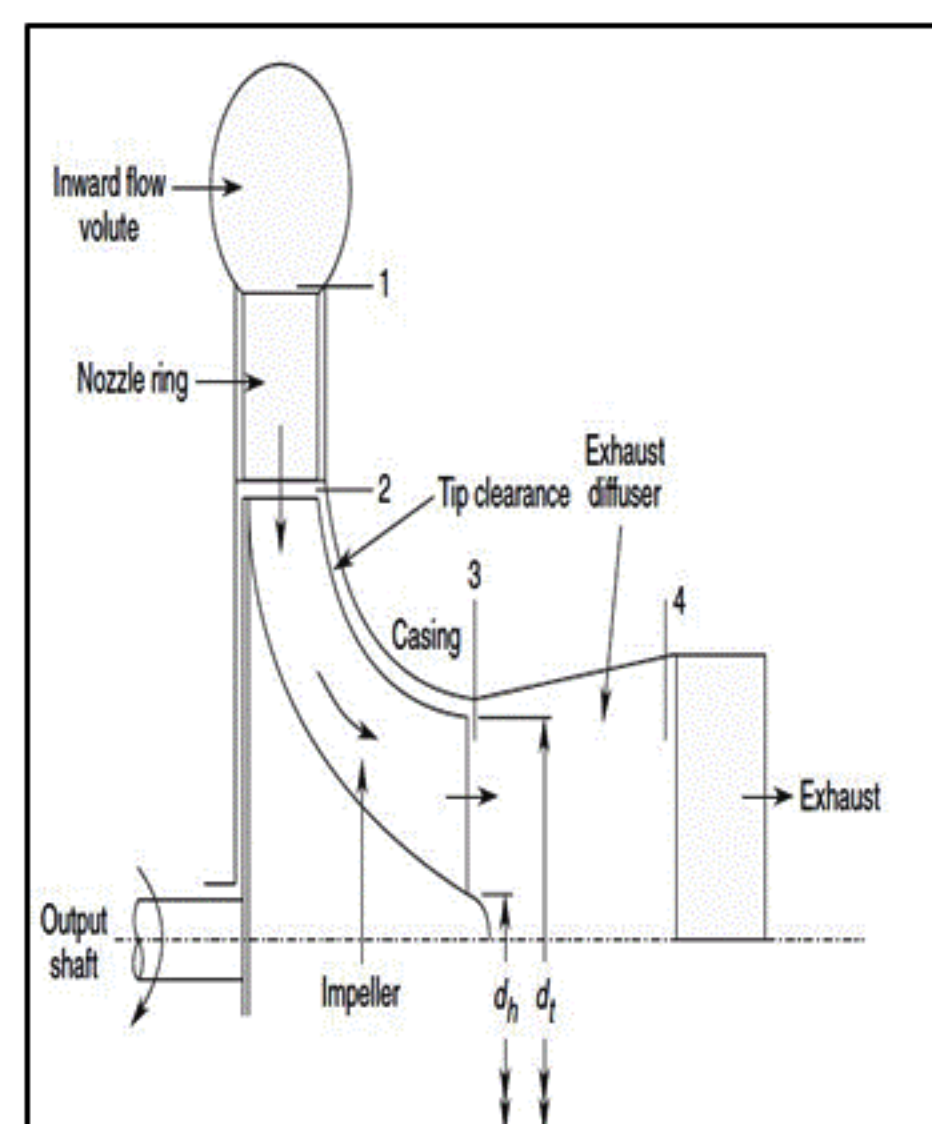
The calculated mass flow rate from above equation is 1.01 kg/s

### CENTRIFUGAL COMPRESSOR



1-2	Inducer
2-3	Impeller
3-4	Vaneless space
4-5	Diffuser
5-6	Volute

### RADIAL INFLOW TURBINE



0-1	Volute
1-2	Nozzle
2-3	Impeller
3-4	Diffuser

## DESIGN

### Turbine and Compressor Meanline Design and Meshing

#### Inlet and Exit velocities of Turbine

M <sub>abs</sub>	0.396	M <sub>abs</sub>	0.098
M <sub>rel</sub>	0.114	M <sub>rel</sub>	0.299
U <sub>2</sub> (m/s)	206.741	U <sub>3</sub> (m/s)	127.97
V <sub>2</sub> (m/s)	181.683	V <sub>3</sub> (m/s)	44.36
W <sub>2</sub> (m/s)	52.526	W <sub>3</sub> (m/s)	135.44
V <sub>w2</sub> (m/s)	176.529	V <sub>w3</sub> (m/s)	0
V <sub>a2</sub> (m/s)	42.968	V <sub>a3</sub> (m/s)	44.36
α <sub>2</sub>	76.32	α <sub>3</sub>	0
β <sub>2</sub>	-35.112	β <sub>3</sub>	-70.881

#### Geometry of Turbine

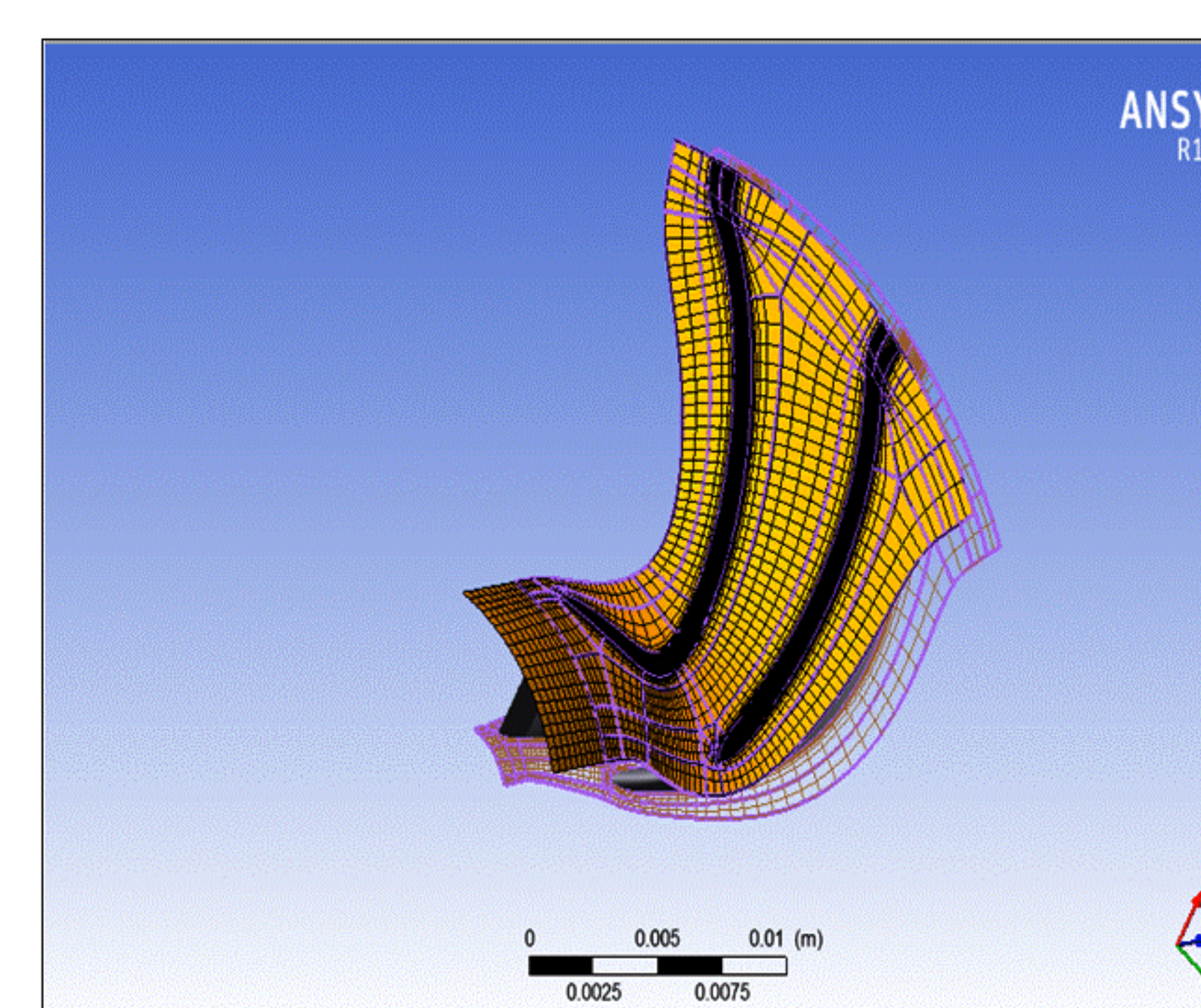
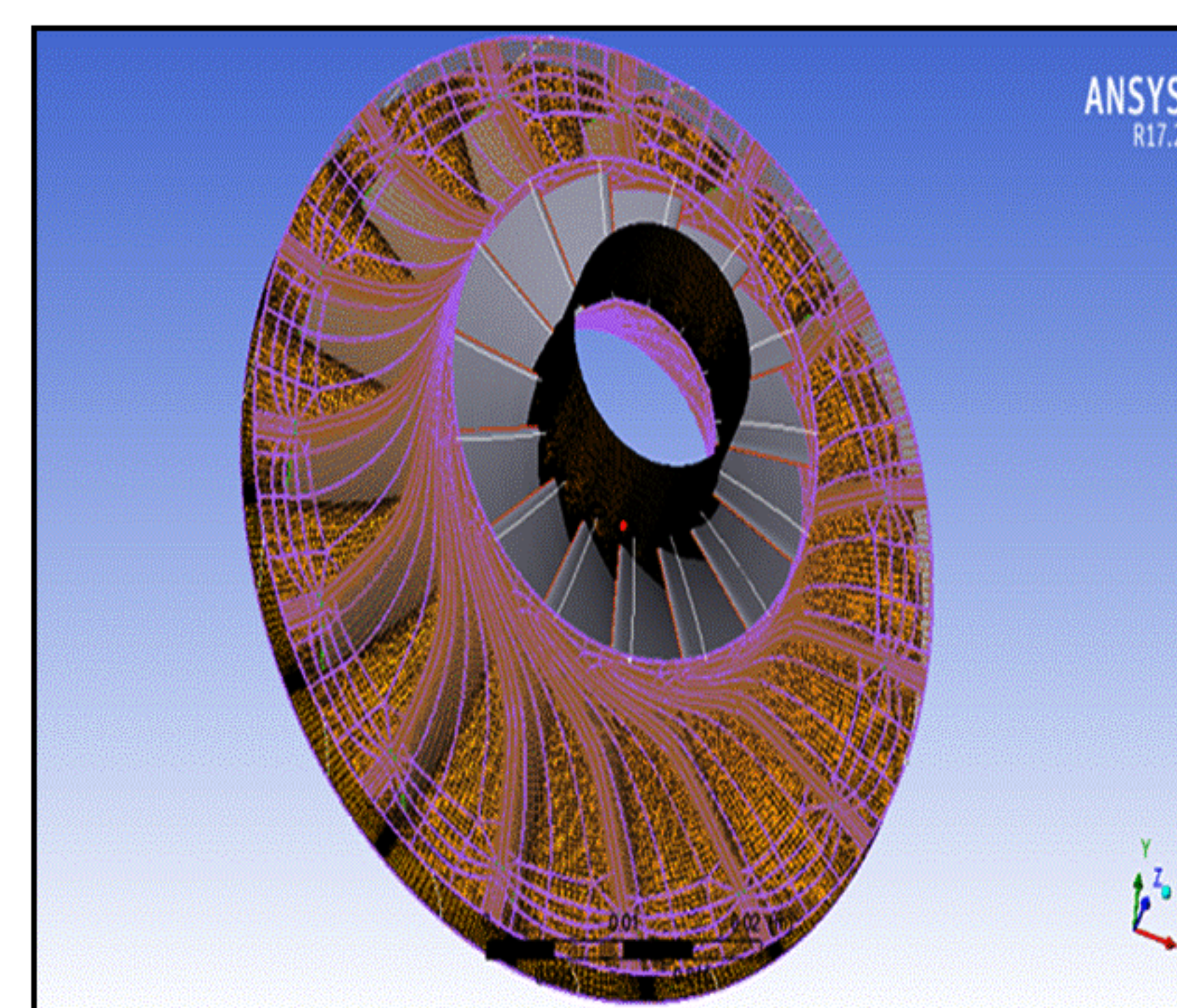
d <sub>2</sub> (mm)	Tip width (mm)	d <sub>3,hub</sub> (m)	d <sub>3,shr</sub> (m)	d <sub>2</sub> /d <sub>3</sub>	β <sub>3,rms</sub>	β <sub>3,hub</sub>
45.47	3.109	12.732	28.146	2.082	-65.93	-52.536

#### Impeller Inlet

M <sub>rel,hub</sub>	0.193	M <sub>rms</sub>	0.595
M <sub>rel,shr</sub>	0.316	M <sub>U</sub>	0.639
V <sub>m,hub</sub> (m/s)	47.11	V <sub>rms</sub> (m/s)	167.54
V <sub>w,hub</sub> (m/s)	0	W <sub>rms</sub> (m/s)	34.39
β <sub>hub</sub>	26.1	α <sub>rms</sub>	16.7
β <sub>shr</sub>	56.8	α <sub>rms</sub>	78.7

#### Geometry of Compressor

D <sub>hub,in</sub> (mm)	D <sub>shr,in</sub> (mm)	A <sub>throat</sub> (mm <sup>2</sup> )	D <sub>imp,out</sub> (mm)	Tip Width (mm)
5	15.61	95.2	37.79	1.823



## CONCLUSION

- 1) Analysis for centrifugal compressor was carried out for real and ideal gas, The findings are, power for compression reduced by 50% for real gas compare to ideal gas compression under the effect of compressibility factor 0.3 near the liquid nature. Isentropic efficiency is 80% for both cases.
- 2) The incidence angle for turbine was optimized to -26.3 degree, head coefficient is 0.8927 and stage flow coefficient is 0.2384. We have achieved 80% isentropic efficiency of turbine, after considering all the losses