

sCO₂ Research & Development at NETL



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and Walter Shelton – NETL, Research and Innovation Center

6th International Supercritical CO₂ Power Cycles Symposium, March 27-29, 2018, Pittsburgh, PA



Solutions for Today | Options for Tomorrow

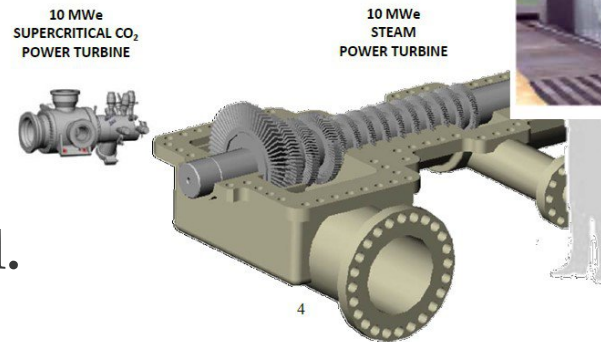


NETL's Vision for sCO₂ Power Generation

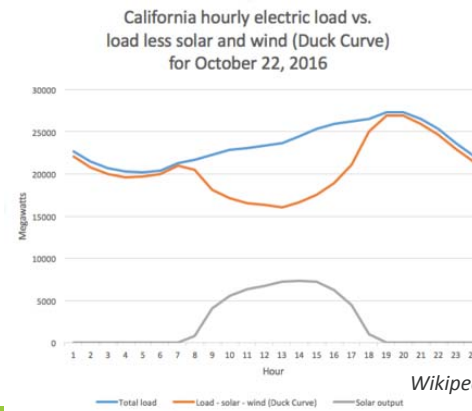


- Higher efficiency (up to 4 pts above AUSC steam).
- Reduced footprint.
- Potential for dry cooling.
- Enabling technology for clean coal.
- CO₂ sequestration (especially for direct cycle).
- Scalability (5 to 500 MW).
- Flexibility (load following, quick start/shutdown)?

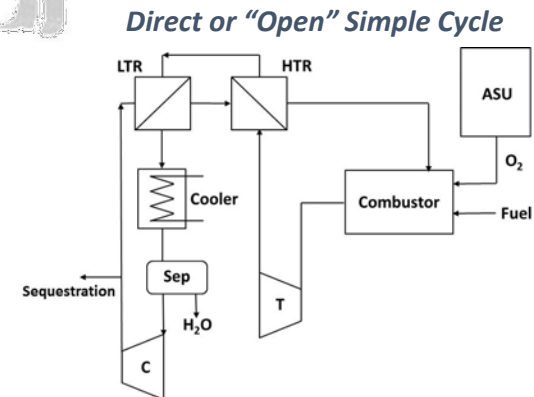
www.breakingenergy.com



Echogen's 10 MWe sCO₂ power turbine compared to a 10 MWe steam turbine.



Wikipedia



NETL Research & Innovation Center (RIC)



Role in Supercritical CO₂ Technology Program

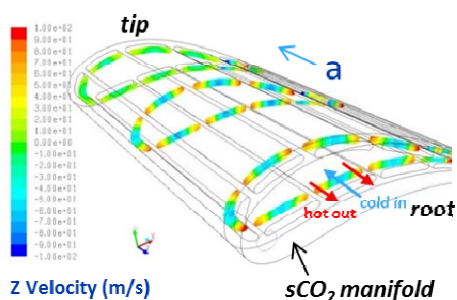
Goal – Develop technology toward achieving the program goal of increased efficiency using sCO₂-based power cycles.

Approach – Perform R&D on turbine blade cooling, oxy-combustion, and materials, along with systems studies.

Aerothermal/Heat Transfer

PI: Jim Black

Cool turbine blades to allow higher turbine inlet temperatures.

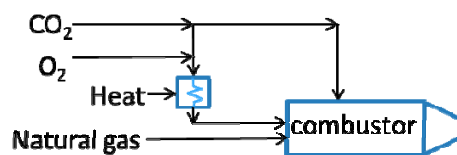


Source: NETL

Oxy-combustion

PI: Peter Strakey

Improve efficiency using higher temperature direct-fired cycle with oxy-combustion.



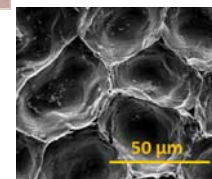
Proposed Oxy-Fuel Combustor

Source: NETL

Materials

PI: Omer Dogan

Evaluate material corrosion, erosion, mechanical property degradation in sCO₂. Identify materials compatible in sCO₂.

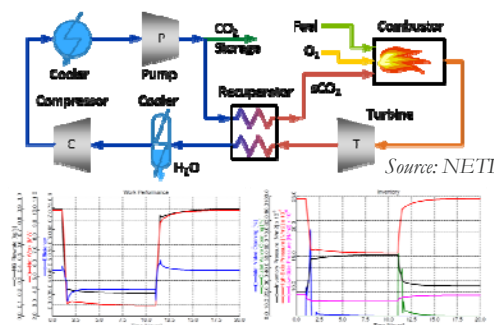


Source: NETL

Systems Analyses

PIs: Weiland, Shelton, Liese

Steady-state and dynamic modeling, techno-economic evaluations of various configurations of sCO₂ power cycle plants (direct- and indirect-fired cycles)

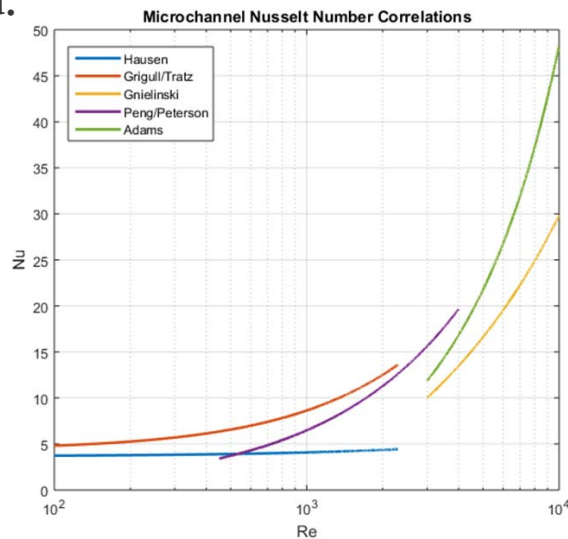


Aerothermal and Heat Transfer R&D



Convective Heat Transfer Coefficients

- Wide Re range of interest for sCO₂ power cycle components – 1,000 < Re < 500,000
- Thermophysical properties change rapidly near the critical point making accuracy of calculation in this region difficult.
- Many correlations proposed in the literature. Difficult to compare unless they are graphed.

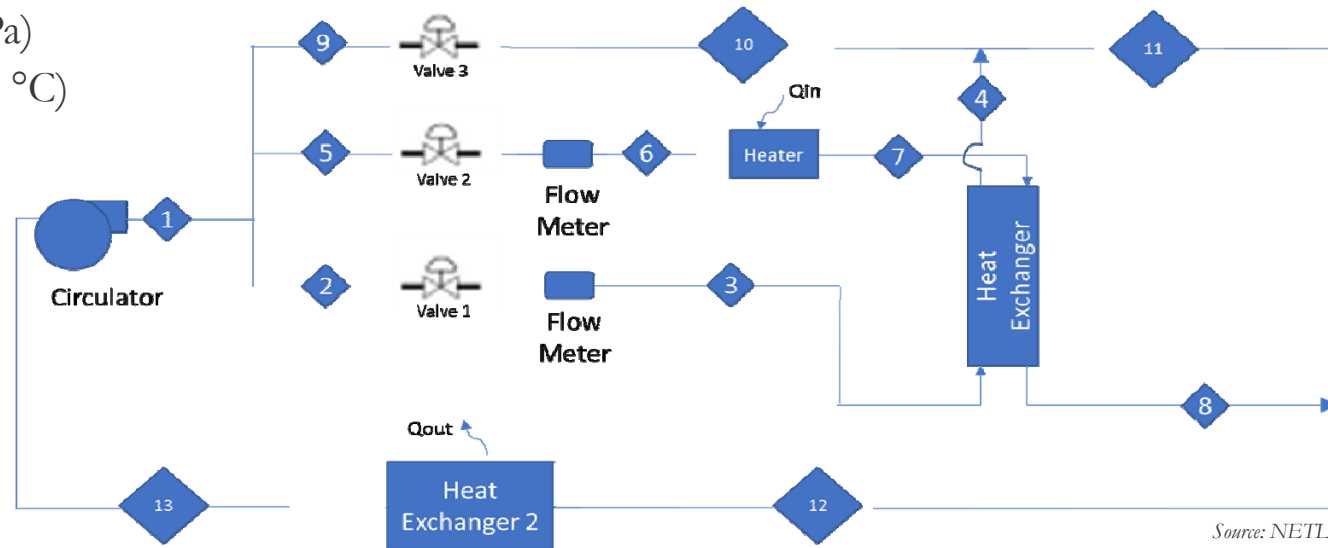


Author	Nu Correlation	Range Valid
Hausen (1959)	$Nu = 3.66 + \frac{0.19(RePr D/L_h)^{0.8}}{1 + 0.117(RePr D/L_h)^{0.467}}$	Re < 2300
Grigull and Tratz (1965)	$Nu = 4.36 + \frac{0.00668 \left(\frac{d_h}{x}\right) RePr}{1 + 0.04 \left[\left(\frac{d_h}{x}\right) RePr\right]^{2/3}}$	laminar
Gnielinski (1976)	$Nu = \frac{\left(\frac{f}{8}\right) (Re - 1000) Pr}{1.07 + 12.7 \left(\frac{f}{8}\right)^{1/2} (Pr^{2/3} - 1)}$ $f = (1.82 \cdot \log(Re) - 1.64)^{-2}$	3,000 < Re < 5 × 10 ⁶ 0.5 ≤ Pr ≤ 2000
Adams et al (1997)	$Nu = \frac{\left(\frac{f}{8}\right) (Re - 1000) Pr}{1.07 + 12.7 \left(\frac{f}{8}\right)^{1/2} (Pr^{2/3} - 1)} (1 + 7.6 \times 10^{-5} Re(1 - (d_h/d_o)^2))$ $d_o = 1.164 \text{ mm}$	turbulent
Peng and Peterson (1995)	where $Nu = 0.072 \left(\frac{D_h}{W_c}\right)^{1.15} [1 - 2.421(Z - 0.5)^2] Re^{0.8} Pr^{1/3}$ $Z = \frac{\min(H, W)}{\max(H, W)}$ H- height, W- width	450 < Re < 4000

Aerothermal and Heat Transfer R&D

Heat Exchange & Experimental Testing (HEET) Rig

- **Objective:** Validate or develop new correlations for calculating convective HT coefficients
- Utilize Wilson Plot measurement technique
- **Capabilities:**
 - Max Pressure – 3,500 psig (24 MPa)
 - Max Temperature – 1,000 °F (538 °C)
 - Max Flow Rate – 3 lb/s (1.5 kg/s)
 - Max Reynolds Number – 500,000
 - Pure CO₂ or mixture with up to 10% N₂



Source: NETL

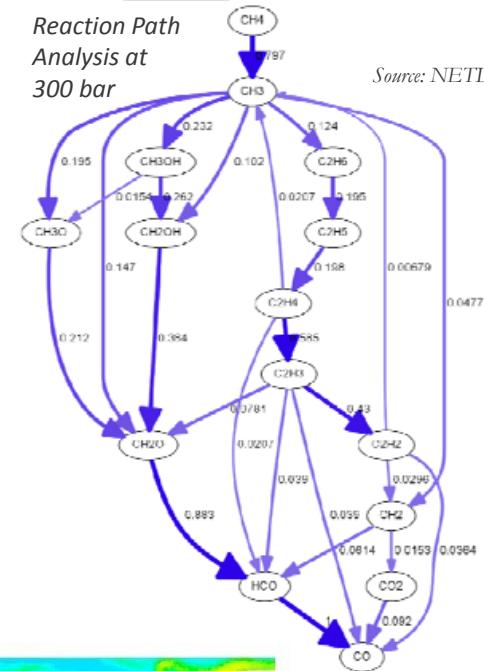
Oxy-Combustion R&D

Analysis of Combustion Fundamentals

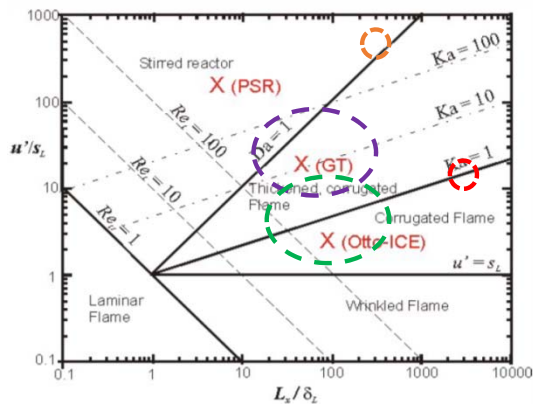
- Natural Gas or Syngas with Oxygen and CO₂ dilution (P ~300 bar, TIT ~1500 K).
- Issues
 - Operating Conditions - Virtually no validation data, no kinetic models, no experience at 300 bar!
 - Heat Release - More likely to resemble a rocket engine than a gas turbine combustor: Combustion dynamics may be an issue.
 - Kinetics - Most methane oxidation models based on GRI Mech, which is only validated below 10 atm.
- Approach: Utilize CFD as well as simple 0D and 1D models to assess the issues.



Reaction Path Analysis at 300 bar
Source: NETL

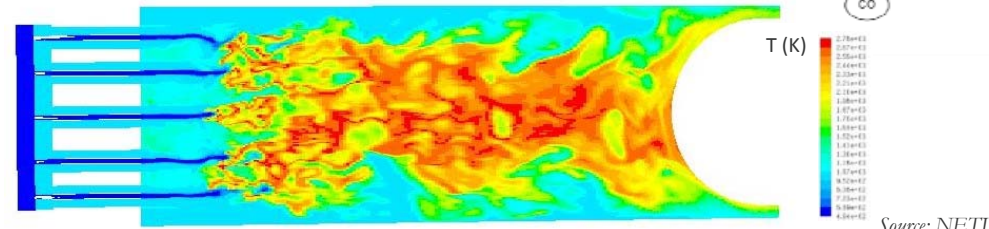


Gas Turbines
 IC Engines
 300 bar sCO₂ (.31O₂+ .69CO₂)
 $S_L = 0.58 \text{ m/s}$ ($T_F=2690\text{K}$)
 $\delta_L = 0.67 \mu\text{m}$
 $Ka=0.7$
 $T_{ign}=9.2e-4 \text{ s}$
 300 bar sCO₂ (.09O₂+ .91CO₂)
 $S_L = 0.05 \text{ m/s}$ ($T_F=1610\text{K}$)
 $\delta_L = 6.60 \mu\text{m}$
 $Ka=361$
 $T_{ign}=2.5e-3 \text{ s}$



Borghi Phase Diagram

CFD of Oxy-Combustor



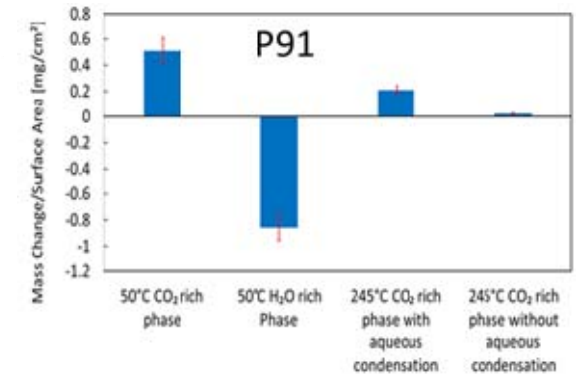
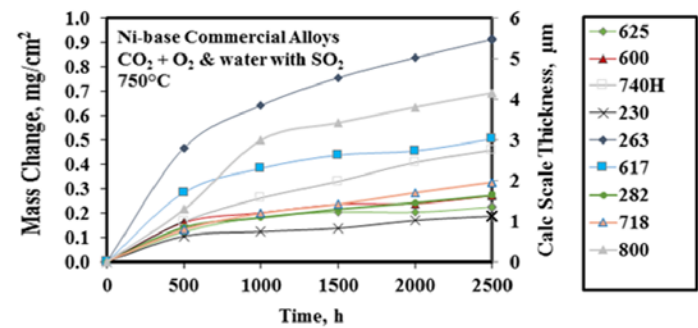
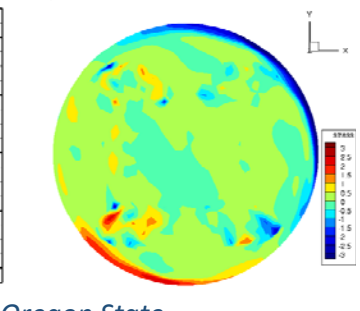
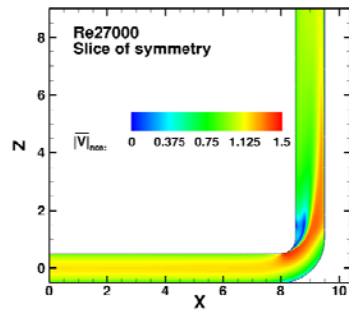
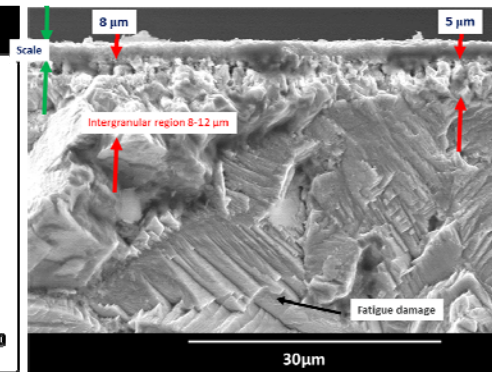
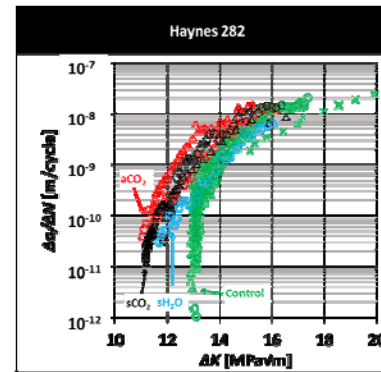
Source: NETL

sCO₂ Materials R&D

Materials Compatibility



- **Effect of sCO₂ cycle environments on mechanical properties**
 - Measurement of fatigue crack growth rates after sCO₂ exposures
- **Low-temperature corrosion in direct sCO₂ cycles**
 - Inexpensive alloys (e.g. P22, P91), corrode with carbonic acid
- **High-temperature oxidation in direct sCO₂ power cycles**
 - 750 °C exposure testing with H₂O, O₂, and SO₂ impurities
- **Erosion of components in sCO₂ cycles**
 - CFD of pipe bends shows high-shear oscillations that may cause erosion of oxide scale

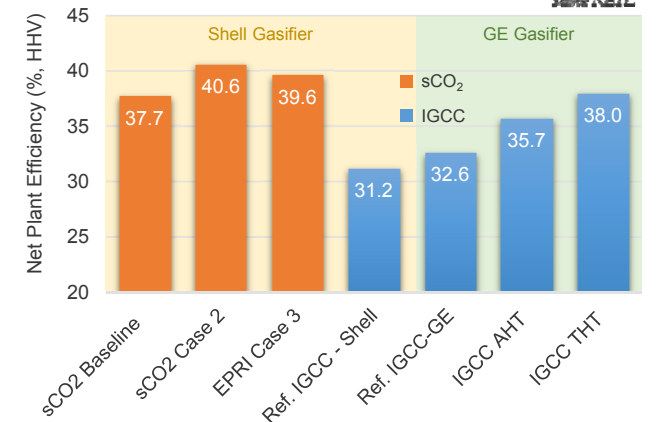
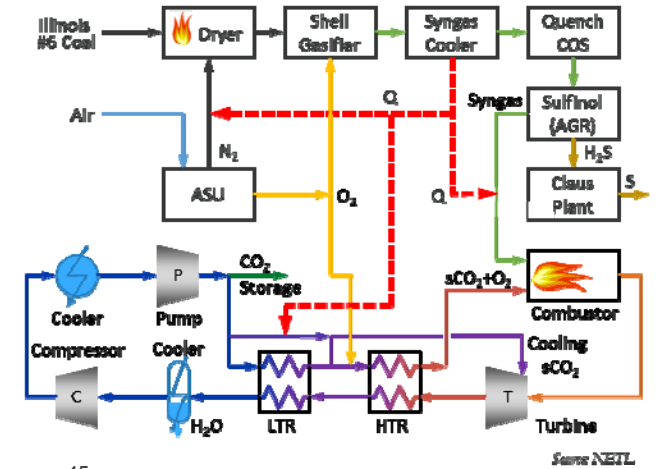


Techno-Economic Analysis R&D

Direct sCO₂ power plants



- Modeled two thermally-integrated Shell gasifier/
direct sCO₂ plants with carbon capture
 - Thermal efficiency of 40.6% (HHV) with 99% carbon capture
 - 20% Cost of Electricity improvement over IGCC systems with carbon capture
- Ongoing and future direct sCO₂ analyses:
 - Change gasifier types and/or syngas cleanup strategies to improve plant efficiency
 - Analysis of natural gas-fired direct sCO₂ system, with detailed turbine cooling model and effect of incomplete combustion
 - Development of component models and control strategies to facilitate off-design and part load studies
 - Improve sCO₂ component cost accuracy



NETL Research and Innovation Center

sCO₂ Research Team Contacts



Most of this work is being presented at the 6th International Supercritical CO₂ Power Cycles Symposium in Pittsburgh, March 2018.

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