



# Thermodynamic model investigation for S-CO<sub>2</sub> Brayton cycle for coal-fired power plant application

5th International Supercritical CO<sub>2</sub>  
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# Outline

- Introduction and context
- Objectives
- Methodology
- Thermodynamics investigation (Results)
- Conclusion and future works

# CONTEXT

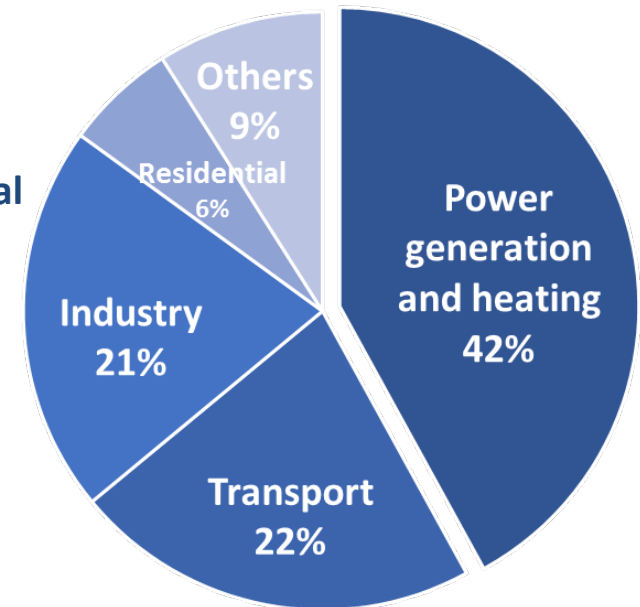
## ■ Challenge in energy demand and the important role of coal in energy mix

- Growing world energy demands :
  - 22126 TWh in 2011
  - Electricity ↑ 80% from 1990 to 2010
  - ↑ 70% is expected by 2035
- Coal-fired plants: 41% of world's power generation
- Power generation: 42% of world's CO<sub>2</sub> emission

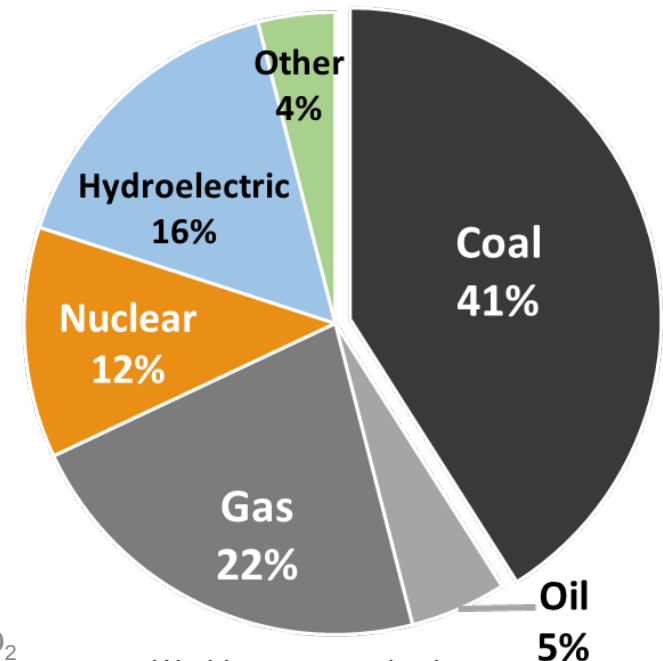
## ■ Challenge in environment

- CO<sub>2</sub> emission: 31.3 Gt in 2011
- Reduction target of 40%-70% by 2050 (post COP 21)

Power Plant Efficiency improvement



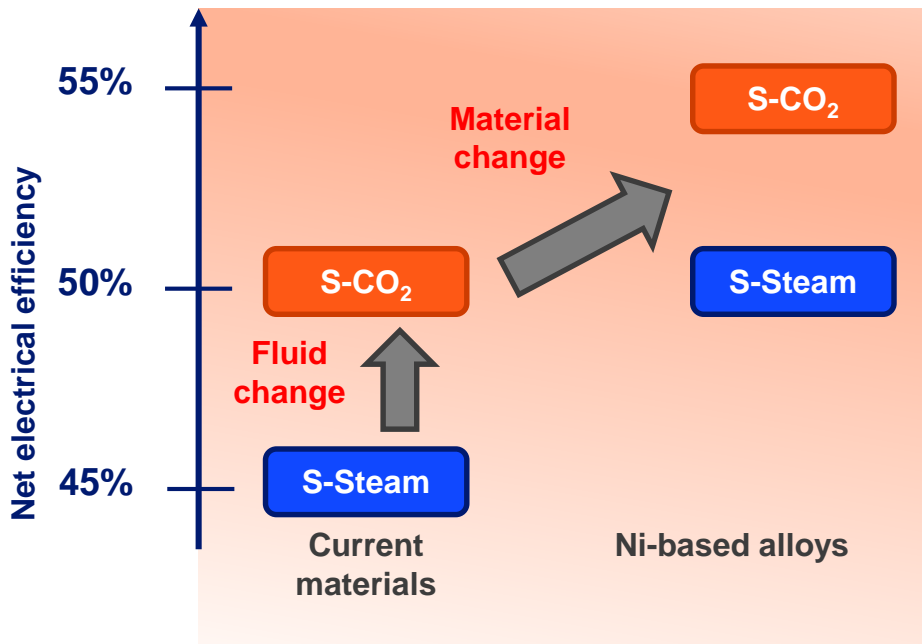
World CO<sub>2</sub> emission in different sector  
– IEA world energy outlook 2013



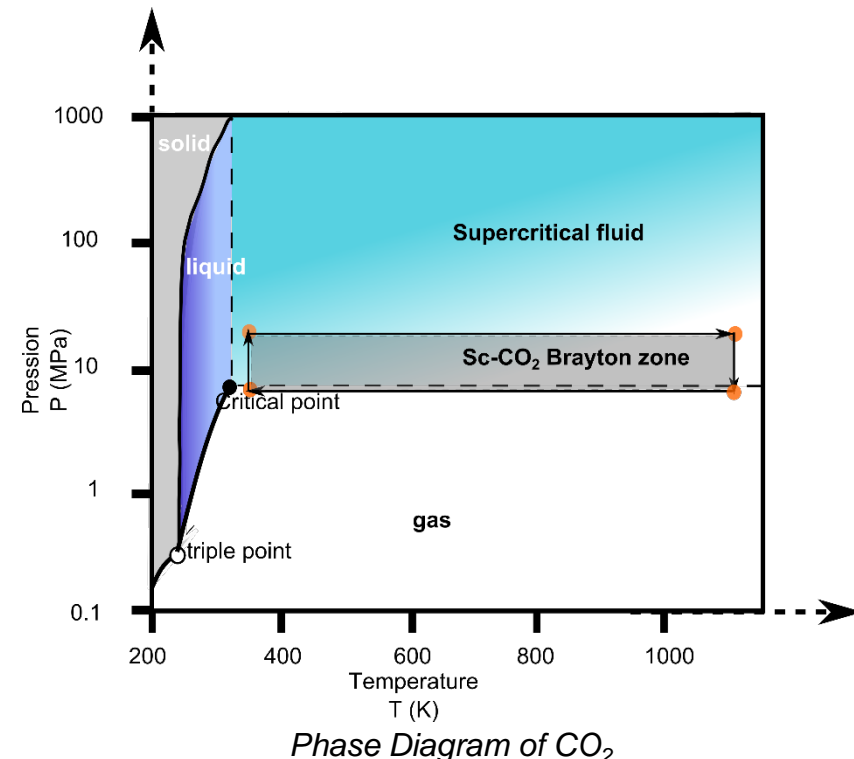
World energy production  
– IEA world energy outlook 2013

# INTRODUCTION

- **State of the art for coal-fired plant**
  - S-Steam: 46%  $L_{HV}$  30MPa/873/893 K
  - Potential of enhancement (material/architecture/working fluid?)
- **S-CO<sub>2</sub> cycle allows at least ↗ 5%pts LHV efficiency**



- **Operation condition**
  - In the vicinity of the critical point
  - High T (up to 1300K) and P (30 MPa)



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# OBJECTIVES OF THIS STUDY

## Modeling and simulation of cycle

Learn more about the cycle behaviors before demonstration at industrial scale

Cycle performance

Machinery sizing

Economics

## Thermodynamic model (EoS) for S-CO<sub>2</sub>

Calculations on density, speed of sound, heat capacity, transport properties

Difficulty on thermodynamic models:

### Operation condition

- High T and P
- Non-classical behaviors near critical point

## Objectives

- Comparison of existing thermodynamics models (EoS) for CO<sub>2</sub>
- Selection of the most accurate model for CO<sub>2</sub> (in the vicinity of the critical point and supercritical region)
- EoS sensitivity study in process simulation

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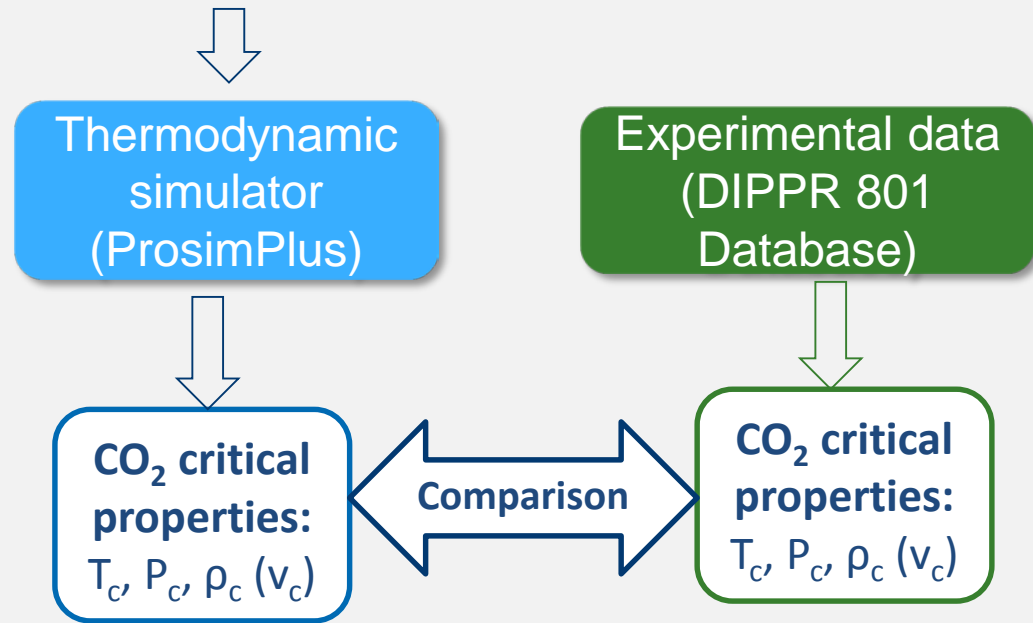
# METHODOLOGY

Step 1: CO<sub>2</sub> critical property comparison with collected DIPPR database

## Step 1: Simulated CO<sub>2</sub> critical properties compared with experimental data

Cubic EoS, virial type EoS, EoS expressed in terms of Helmholtz energy

Candidate EoS: PR, PR-BM, SRK, LKP, BWRS, SW





# METHODOLOGY

Step 1: CO<sub>2</sub> critical property comparison with collected DIPPR database



Step 2: CO<sub>2</sub> criteria property comparison in the vicinity of the critical point

**Step 2: CO<sub>2</sub> criteria property comparison in the vicinity of the critical point**

- 300 K < T < 310 K, P = 7.38 MPa

Candidate EoS: PR, PR-BM, SRK, LKP, BWRS, SW

Thermodynamic simulator  
(ProsimPlus)

Experimental data  
(DECHEMA Database)

criteria properties:  
Density( $\rho$ ), heat capacity ( $c_p$ ), speed of sound( $\omega$ )

Comparison

criteria properties:  
Density( $\rho$ ), heat capacity ( $c_p$ ), speed of sound( $\omega$ )

# METHODOLOGY

Step 1: CO<sub>2</sub> critical property comparison with collected DIPPR database



Step 2: CO<sub>2</sub> criteria property comparison in the vicinity of the critical point



Step 3: CO<sub>2</sub> criteria property comparison in the whole region of study

**Step 3: CO<sub>2</sub> criteria property comparison in the entire region of interest**

- 300 K < T < 900 K, 7 MPa < P < 30 MPa

Candidate EoS: PR, PR-BM, SRK, LKP, BWRS, SW

Thermodynamic simulator (ProsimPlus)

Experimental data (DECHEMA Database)

criteria properties:  
Density, heat capacity, speed of sound( $\omega$ )

Comparison

criteria properties:  
Density, heat capacity, speed of sound( $\omega$ )

**Favorable EoS**

EoS leads to the **smallest** relative "model/measurement" deviation

# METHODOLOGY

Step 1: CO<sub>2</sub> critical property comparison with collected DIPPR database



Step 2: CO<sub>2</sub> criteria property comparison in the vicinity of the critical point



Step 3: CO<sub>2</sub> criteria property comparison in the whole region of study



Step 4: EoS sensitivity study in process modeling

## Step 4: EoS sensitivity in process modeling of Brayton cycle

- Recuperated Brayton Cycle (RC)
- Recompression Recuperated Brayton Cycle (RRC)

Favorable EoS



Process simulator (ProsimPlus)



Process modeling with constraints: Design parameter, cycle efficiency,...

Other 5 EoS



Process simulator (ProsimPlus)



Process modeling with constraints: Design parameter, cycle efficiency,...

Comparison



Results Analysis and Discussion

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- Thermodynamics investigation
  - Step 1: CO<sub>2</sub> critical property comparison
  - Step 2: Criteria property comparison near the critical point
  - Step 3: Criteria property comparison in the region of interest
  - Step 4: Model Sensitivity (process simulation)
- Conclusion and future works

# STEP 1) CRITICAL PROPERTIES COMPARISON

- Experimental  $T_c$ ,  $P_c$  as input parameters

- $T_c=304.21$  K,  $P_c=7.3830$  MPa

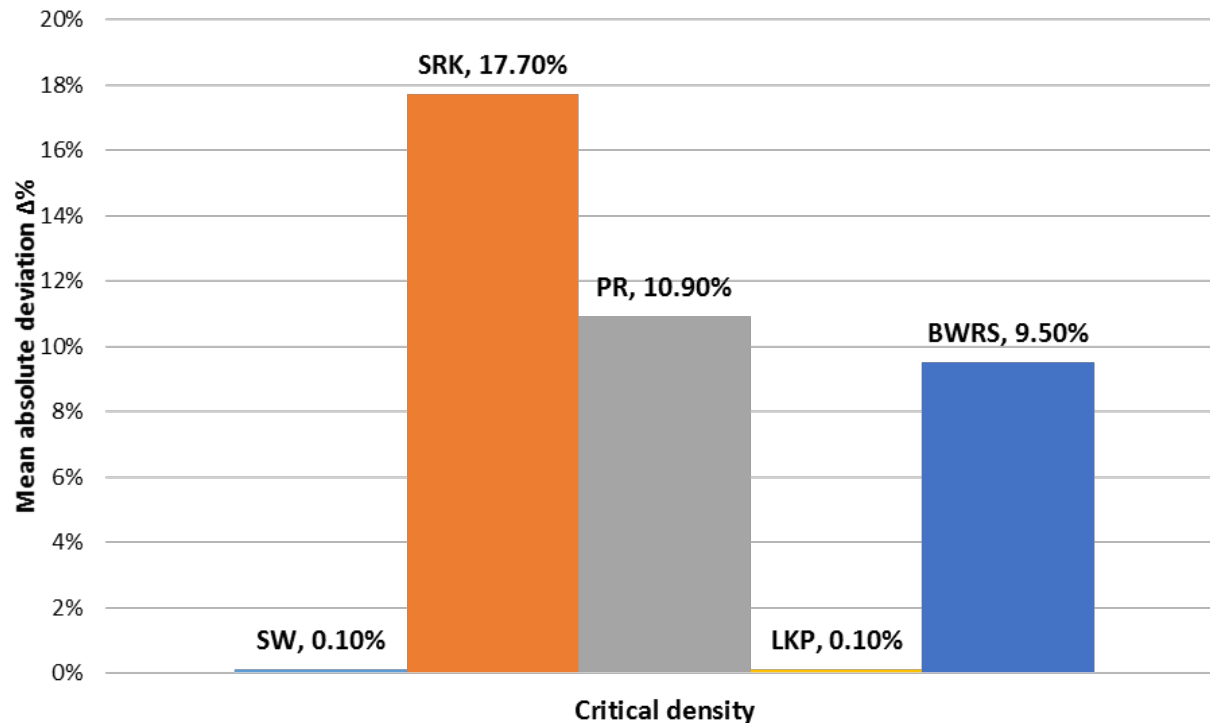
- Except for SW EoS

- $T_c=304.13$  K,  $P_c=7.3773$  MPa

- Critical density

- SW and LKP EoS exhibit 0.1% on  $\rho_c$

- SRK EoS shows the biggest deviation

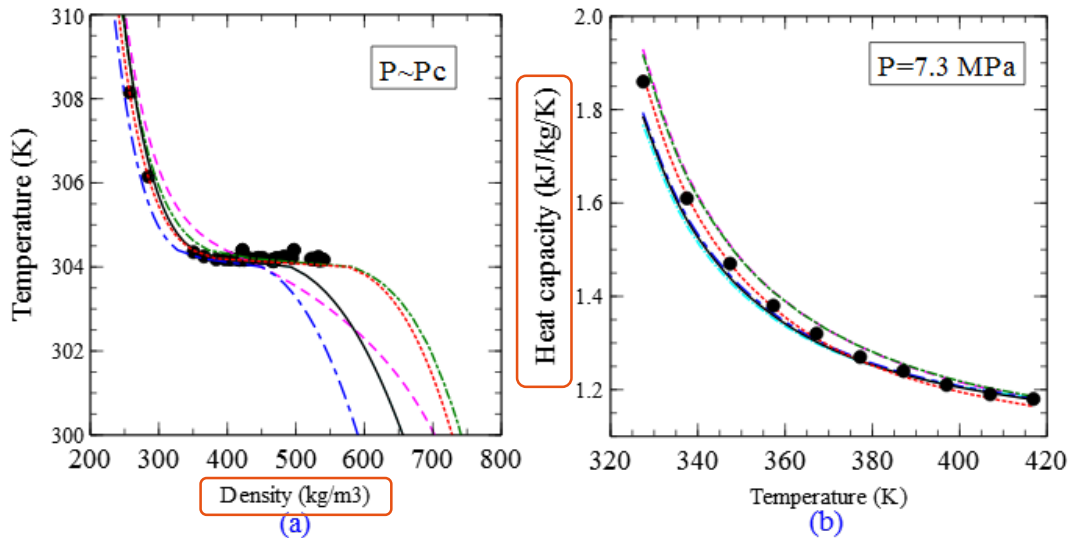


$\Delta$  is defined as the absolute mean average of  $(\text{Critical density}_{\text{experimental}} - \text{Critical density}_{\text{EoS calculated}}) / \text{Critical density}_{\text{experimental}}$

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# STEP 2) COMPARISON NEAR CRITICAL POINT



- **In the vicinity of the critical point**

- $300 \text{ K} < T < 310 \text{ K}$ ,  $P = 7.38 \text{ MPa}$
- $\omega$ :  $T = T_c$  and  $6 \text{ MPa} < P < 8 \text{ MPa}$

- **Density**

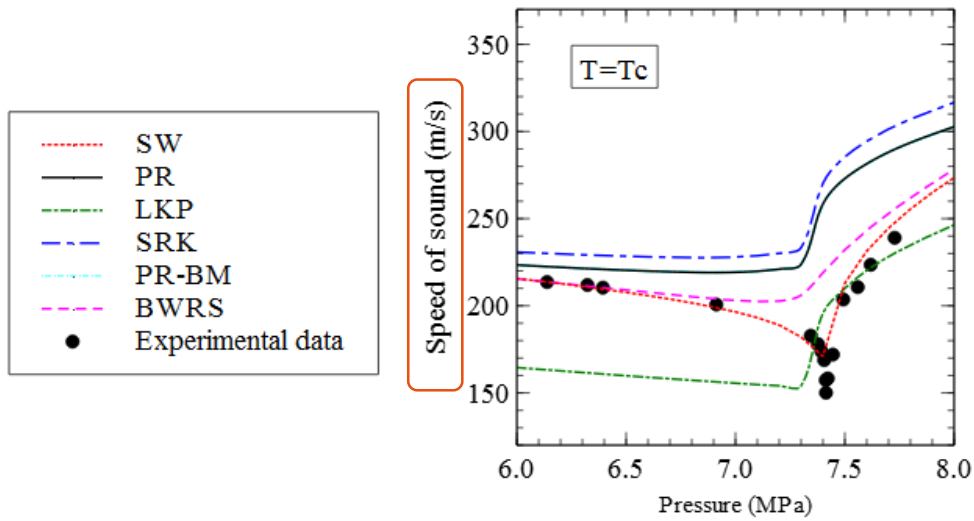
- SW:  $\Delta\rho$  around 10%

- **Heat capacity**

- SW:  $\Delta c_p$  around 2%

- **Speed of sound**

- SW:  $\Delta\omega$  around 7%
- Severe criteria for EoS validation



Representation of (a) isobaric density, (b) heat capacity, (c) isotherm speed of sound in the critical region of  $\text{CO}_2$

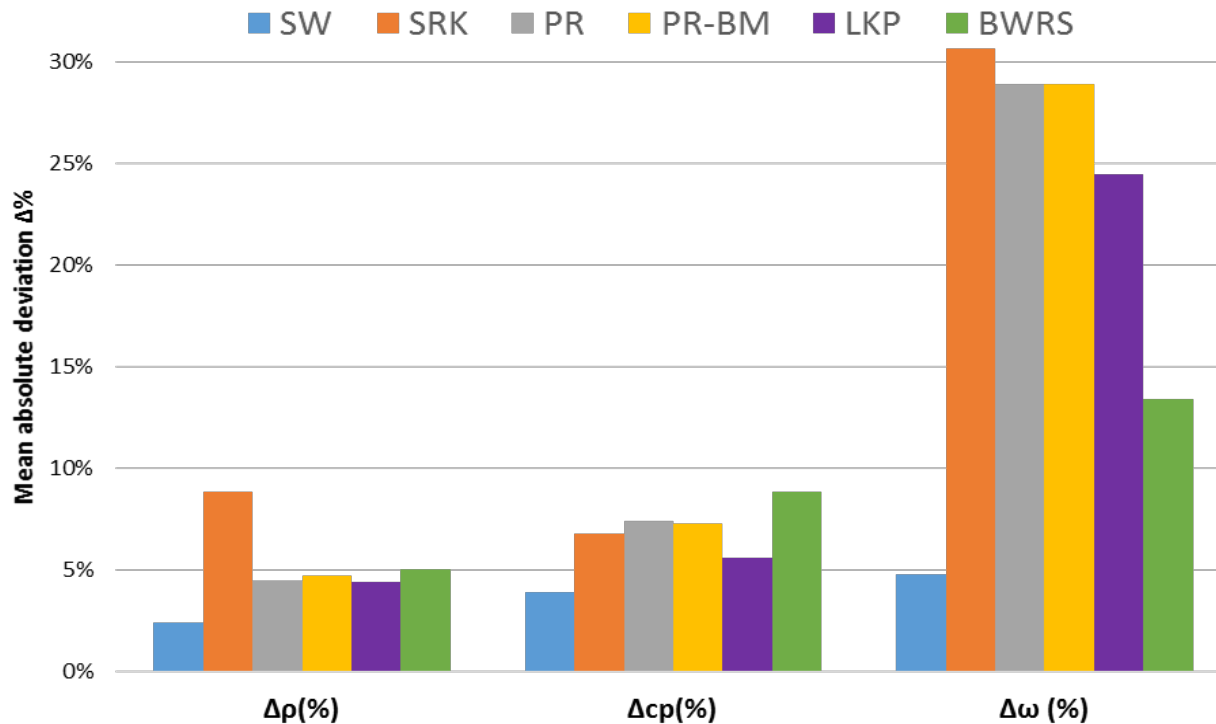
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# STEP 3) COMPARISON IN ENTIRE REGION OF INTEREST

- In the entire region of interest
  - 300K <T<900 K and 7 MPa <P<30 MPa
  - 2641 “density” pts; 359 “heat capacity” pts; 138 “speed of sound” pts



$\Delta$  is defined as the absolute mean average of  $(\text{property value}_{\text{experimental}} - \text{property value}_{\text{EoS calculated}}) / \text{property value}_{\text{experimental}}$

**SW** is the most accurate EoS in the entire region of interest

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# STEP 4) SENSITIVITY STUDY

## EoS sensitivity in **process** modeling simulation

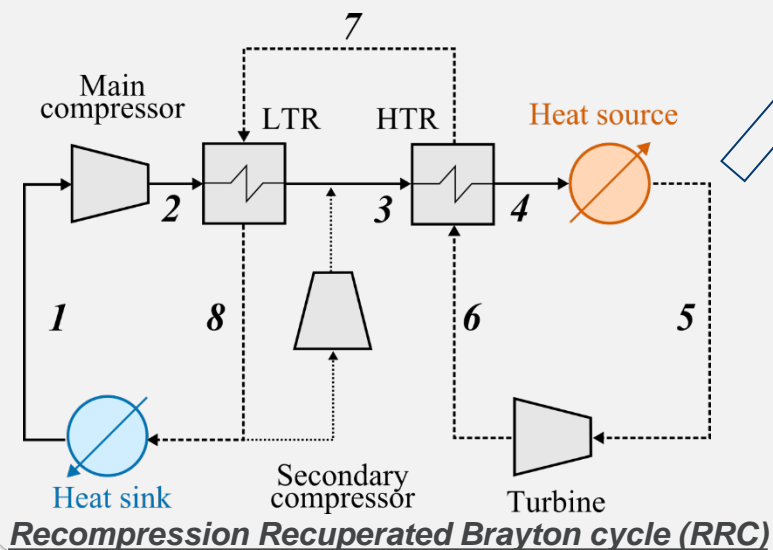
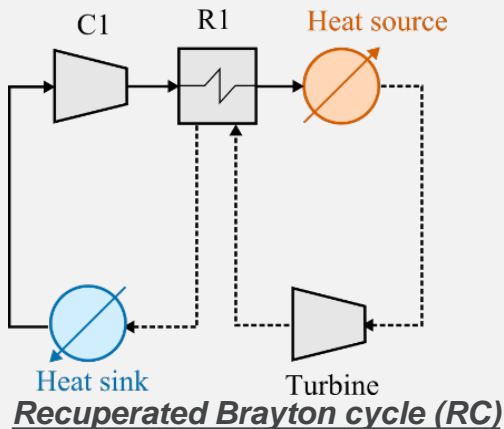
- Set SW EoS simulation as reference

EoS sensitivity: PR, PR-BM, SRK, LKP, BWRS

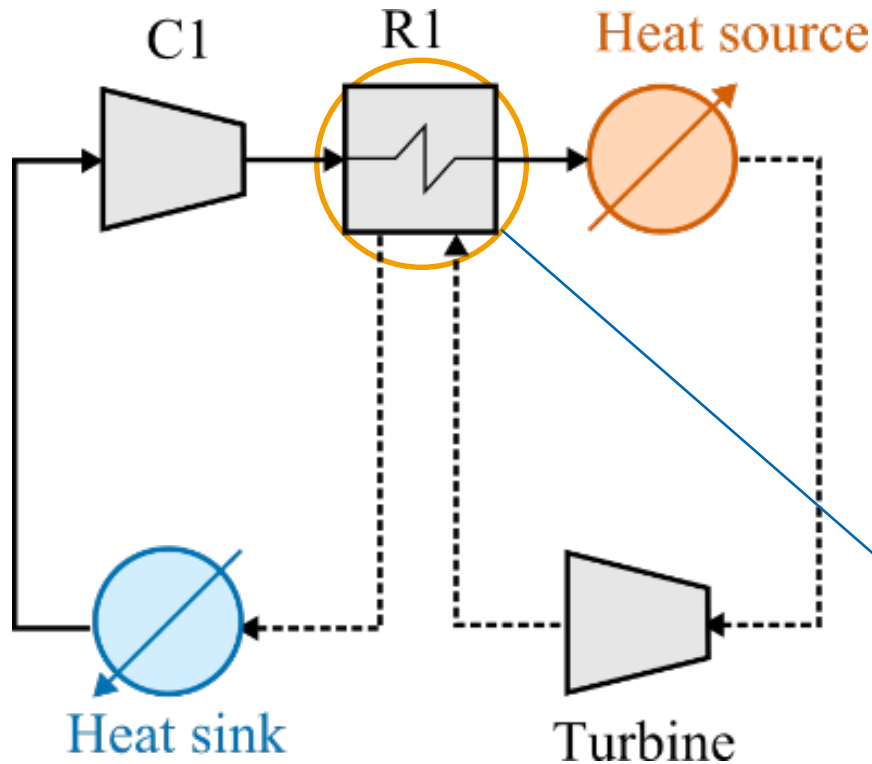
Industrial constraints

Process simulator  
(ProsimPlus)

Results Analysis:  
Design parameter, cycle performance,...



# STEP 4) SENSITIVITY STUDY: RC BRAYTON CYCLE

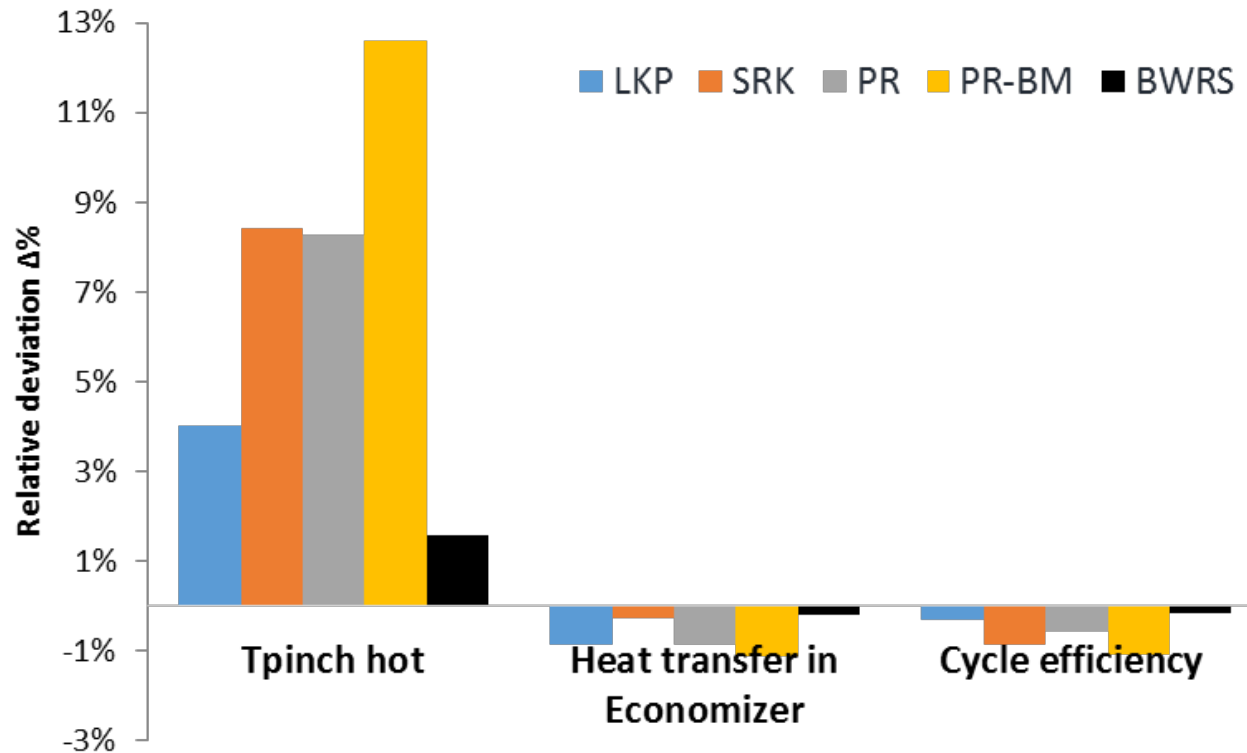


- CSP application reference to Mohagheghi and Kapat, 2013[1]
- Parameter and constraints set identical to reference
- 5 other EoS process simulation compared with SW EoS process simulation

- $T_{\text{pinch hot}}$
- $Q_{\text{economizer}}$
- Cycle efficiency

[1]M. Mohagheghi and J. Kapat, "Thermodynamic Optimization Of Recuperated S-CO<sub>2</sub> Brayton Cycles For Solar Tower Applications", *Proceedings of ASME Turbo Expo* , 2013

# STEP 4) SENSITIVITY STUDY: RC BRAYTON CYCLE



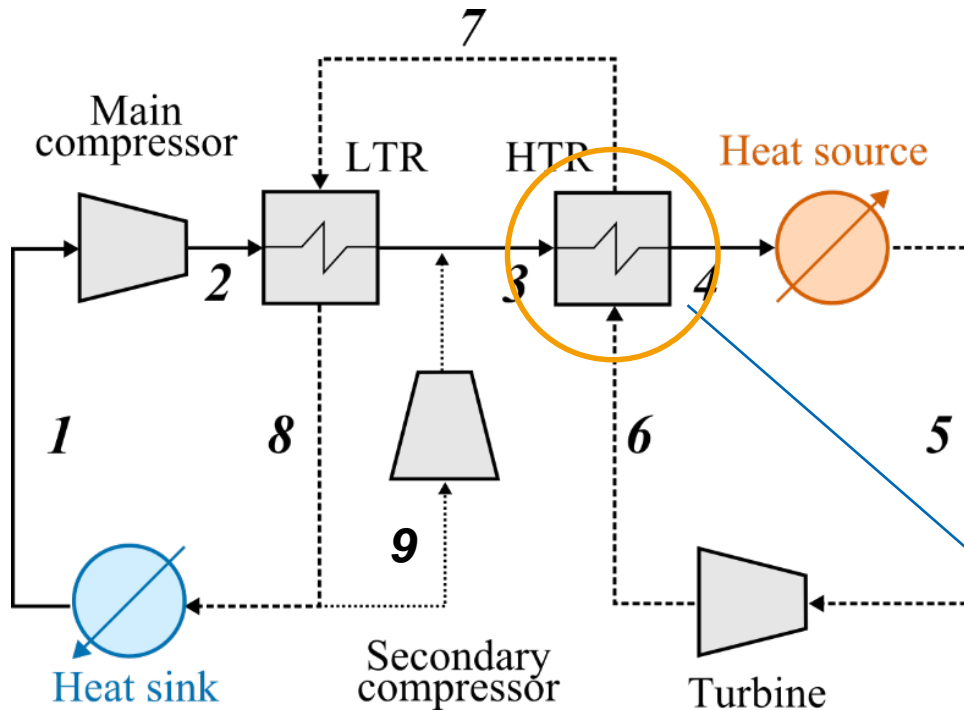
\*  $\Delta$  is defined as the relative deviation of ( result simulated by other EoS – result simulated by SW)/result simulated by SW

## Other EoS

- Hot Pinch temperature on economizer overestimated
- Heat in economizer underestimated
- Small impact on cycle efficiency

⇒ **Surface of economizer underestimated**

# STEP 4) SENSITIVITY STUDY: RRC BRAYTON CYCLE

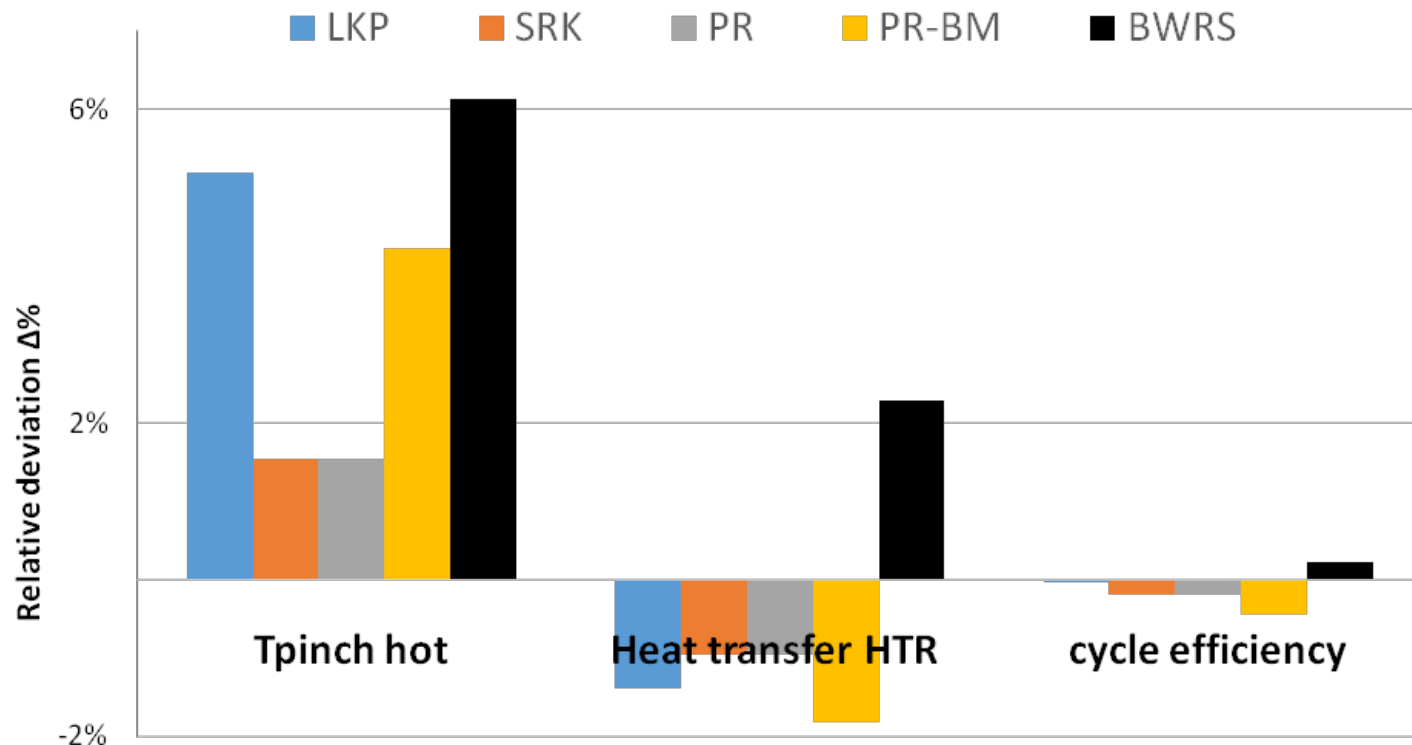


- Coal-fired application referenced to Mecheri and Le Moullec, 2016[2]
- Parameter and constraints set identical to reference
- 5 other EoS process simulation compared with SW EoS process simulation

- $T_{\text{pinch hot}}$
- $Q_{\text{economizer}}$
- Cycle efficiency

[2]M. Mecheri and Y. Le Moullec, "Supercritical CO<sub>2</sub> Brayton Cycles For Coal-fired Power Plants", accepted by *Energy* in 2016

# STEP 4) SENSITIVITY STUDY: RRC BRAYTON CYCLE

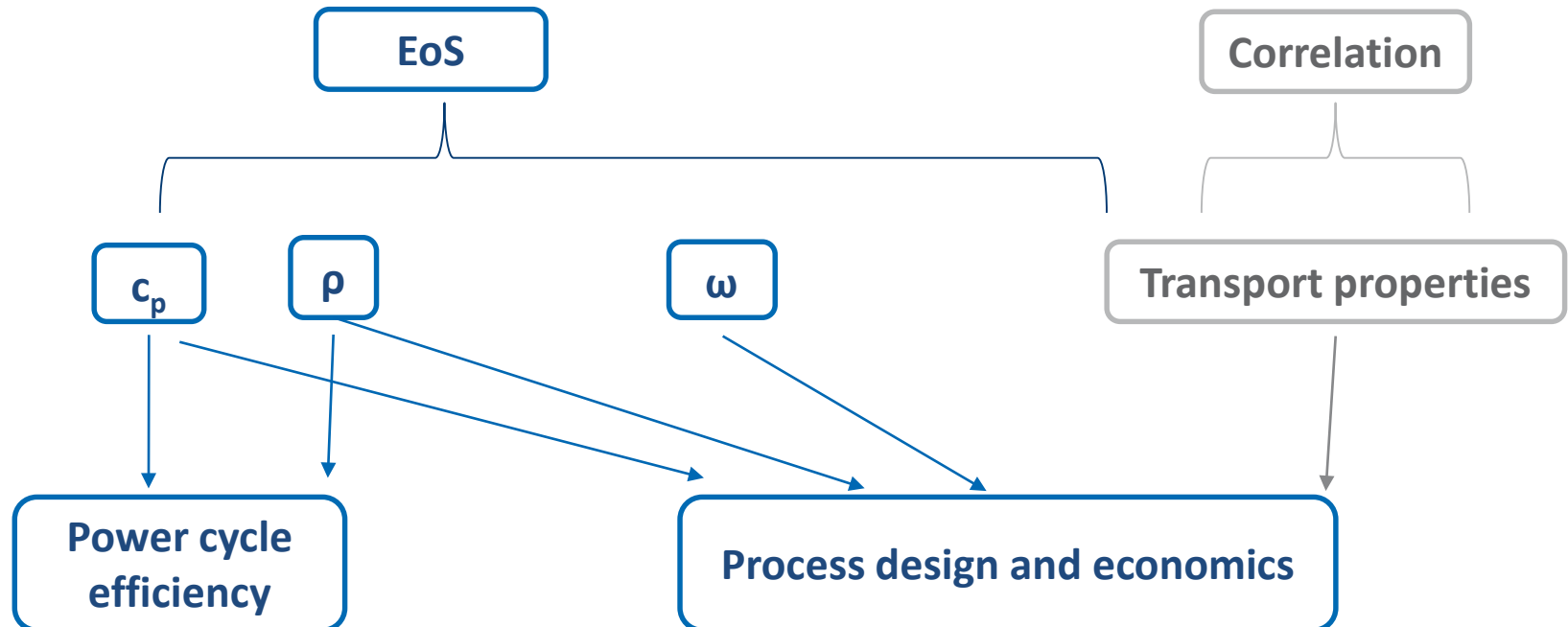


$\Delta$  is defined as the relative deviation of ( result simulated by other EoS – result simulated by SW)/result simulated by SW

- Hot Pinch temperature on economizer overestimated
- Heat in economizer underestimated (except for BWRS)
- Small impact on cycle efficiency
- Influence of EoS becomes more complex when layout is more **complicate** and **number(component)** ↗

# STEP 4) SENSITIVITY STUDY: DISCUSSION

- Small effect of EoS on power cycle efficiency
- No involvement of speed of sound in cycle efficiency calculation (strong involvement in machinery sizing)
- Predictable strong dependence of EoS on Process Design and Economical Assessment
- Foreseen effects on Brayton cycle optimization: maximize the cycle efficiency





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# Conclusion

- **SW EoS** is the most accurate model (among the 6 studied EoS) in both critical and supercritical region for CO<sub>2</sub>
- Small effects of EoS observed on power cycle efficiency
- However **process design** is expected to strongly depend on EoS
- Precision of EoS is required for complex cycle layout
- Accurate EoS is required for mixture of CO<sub>2</sub>

## Future Work

- Process optimization with respect to energy and economics (Non-Linear Programming)
- Propagation of thermodynamic model uncertainty to cycle output
- Optimization of process structure (Flowsheet)

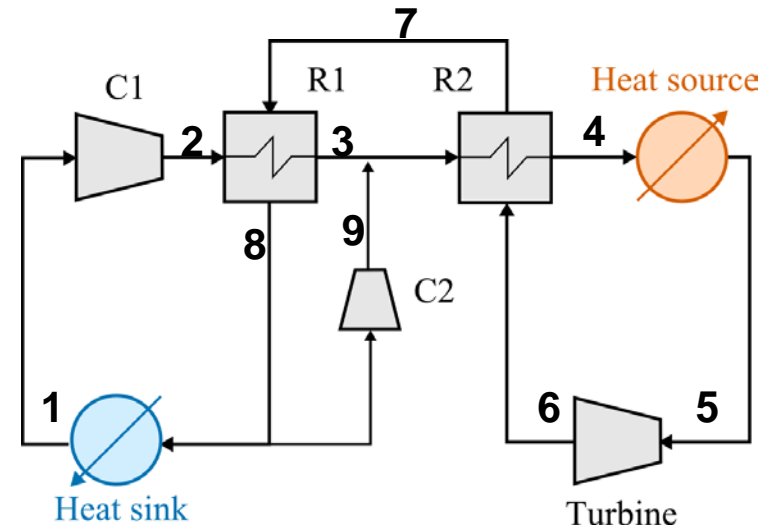
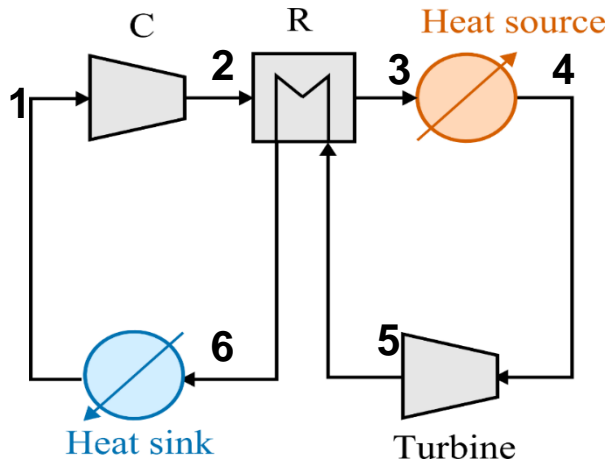
# Thank you for your attention

Contacts: [qiao.zhao@edf.fr](mailto:qiao.zhao@edf.fr)



# BACK UP

## 1) HYPOTHESIS AND CONSTRAINTS



Tin compressor (=Tcooling) (K)	320
Pin compressor (MPa)	3.274
Pout compressor (MPa)	12
T heater (K)	1373
Tpinch cold (K)	20
isentropic efficiency of turbine	0.9
isentropic efficiency of compressor	0.89
heat source (MW)	200
Pressure drop in every component (%)	1

Tin compressor (=Tcooling) (K)	308.15
Pin compressor (MPa)	75
Pout compressor (MPa)	20
Pout sec compressor (MPa)	19.9
T heater (K)	773
Tpinch cold (K)	10
isentropic efficiency of turbine	0.9
isentropic efficiency of compressor	0.89
Mechanical efficiency of compressor	0.981
heat source (MW)	200
Pressure drop in every component (MPa)	0.1

Temperature equality in Flow(9) and Flow(3)

Constant heat source (1187 MW)in the boiler

# BACK UP

## 2) THERMODYNAMICS BASIS (HEAT CAPACITY)

$$c_p^*(T^*, v^*) = c_p^\bullet(T^*, v^*) + c_p^{res}(T^*, v^*)$$

$$c_p^\bullet = A + B\left(\frac{C}{T}\right)^2 + D\left(\frac{E}{T}\right)^2$$

$$\left\{ \begin{array}{l} s^{var}(T, v) = - \left[ \frac{\partial a^{var}(T, v)}{\partial T} \right]_v \\ P^{var}(T, v) = - \left[ \frac{\partial a^{var}(T, v)}{\partial v} \right]_T \\ u^{var}(T, v) = a^{var}(T, v) + T \cdot s^{var}(T, v) \\ C_v^{var}(T, v) = \left[ \frac{\partial u^{var}(T, v)}{\partial T} \right]_v \\ C_p^{var}(T, v) = C_v^{var} - T \left[ \frac{\left( \frac{\partial P^{var}(T, v)}{\partial T} \right)_v}{\left( \frac{\partial P^{var}(T, v)}{\partial v} \right)_T} \right]^2 \end{array} \right. \left\{ \begin{array}{l} A = 29370 \\ B = 34540 \\ C = 1428 \\ D = 26400 \\ E = 588 \end{array} \right.$$

SW EoS:

$$\frac{c_p}{R} = \underbrace{-\tau^2(\varphi_{\tau\tau}^o + \varphi_{\tau\tau}^r)}_{\frac{c_v}{R}} + \frac{\overbrace{(1 + \delta\varphi_\delta^r - \delta\tau\varphi_{\delta\tau}^r)^2}^{\approx(\frac{\partial p}{\partial T})_p^2}}{\underbrace{1 + 2\delta\varphi_\delta^r + \delta^2\varphi_{\delta\delta}^r}_{\approx(\frac{\partial p}{\partial p})_T}}$$

# BACK UP

## 2) THERMODYNAMICS BASIS (SPEED OF SOUND)

$$w = \sqrt{\left(\frac{\partial P}{\partial \rho}\right)_s}$$

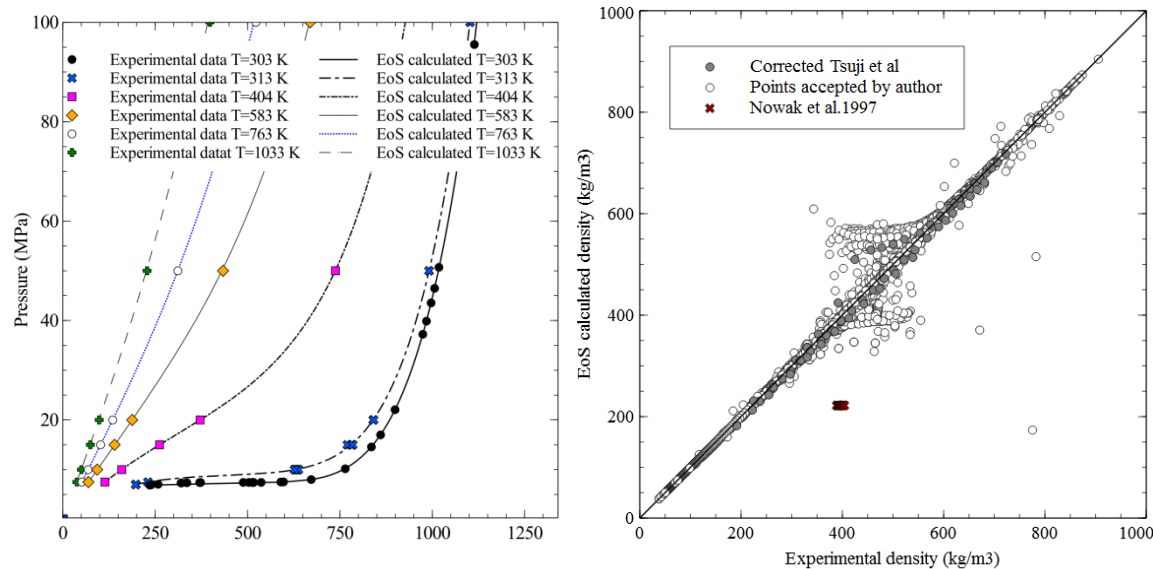
SW EoS:

$$\frac{w^2}{RT} = \underbrace{1 + 2\delta\varphi_\delta^r + \delta^2\varphi_{\delta\delta}^r}_{\approx (\frac{\partial p}{\partial \rho})_T} - \frac{\overbrace{(1 + \delta\varphi_\delta^r - \delta\tau\varphi_{\delta\tau}^r)^2}^{\approx (\frac{\partial p}{\partial T})_\rho^2}}{\underbrace{\tau^2(\varphi_{\tau\tau}^o + \varphi_{\tau\tau}^r)}_{-\frac{c_v}{R}}}$$

# BACK UP

## STEP 3) SW EoS IN ENTIRE REGION OF INTEREST

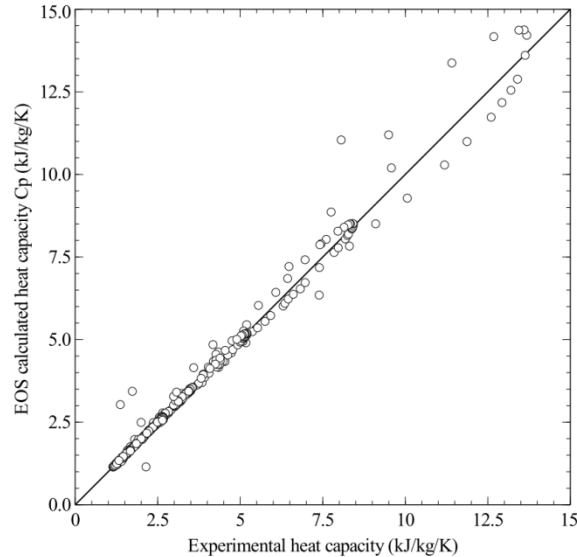
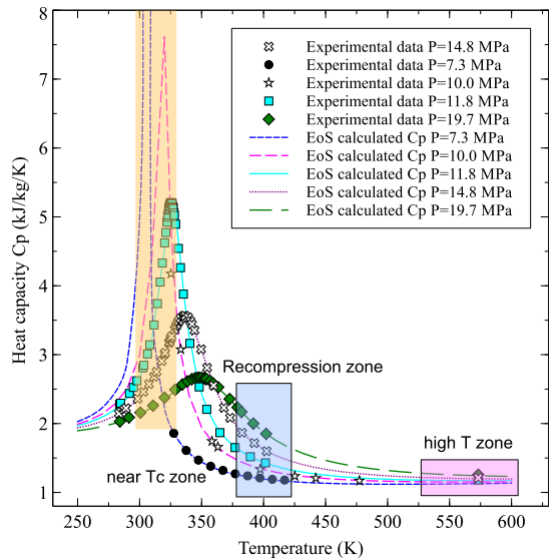
- Region of entire study:  $300 < T < 900$  K,  $7 < P < 30$  MPa



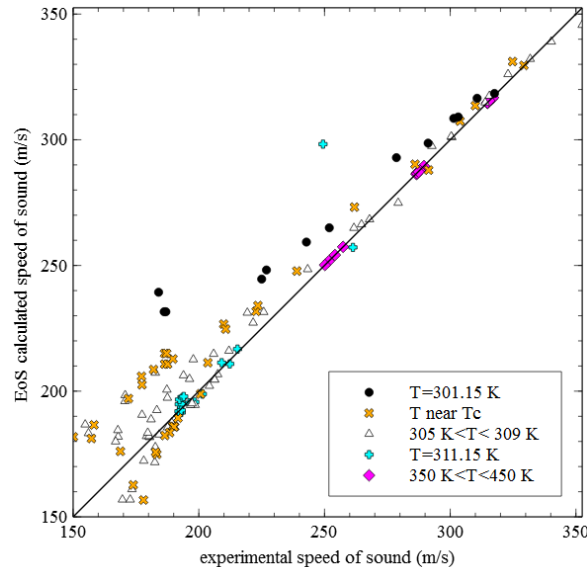
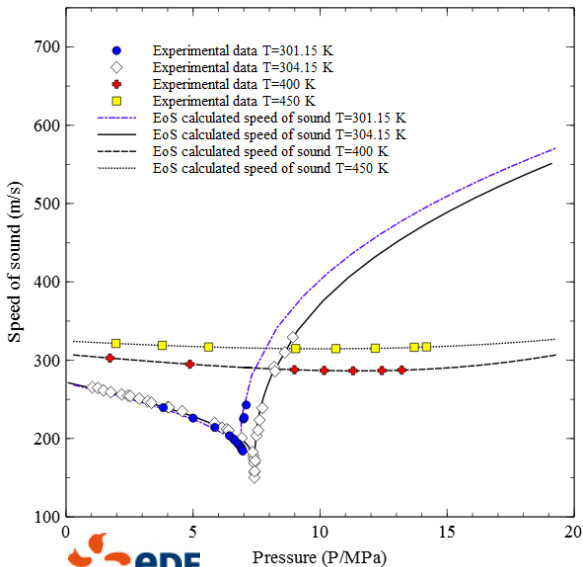
- Satisfactory agreement between  $\rho_{\text{SW EoS calculated}}$  and  $\rho_{\text{experimental}}$
- Parity curve with all accessed experimental data
  - $\Delta\rho=2.4$  %
  - Relative important deviations ( $>15\%$ ) in the vicinity of the critical point

# BACK UP

## STEP 3) SW EoS IN ENTIRE REGION OF INTEREST



- Satisfactory agreement between  $C_p$  SW EoS calculated and  $C_p$  experimental
- Parity curve with all accessed experimental data
- $\Delta C_p = 4.0\%$

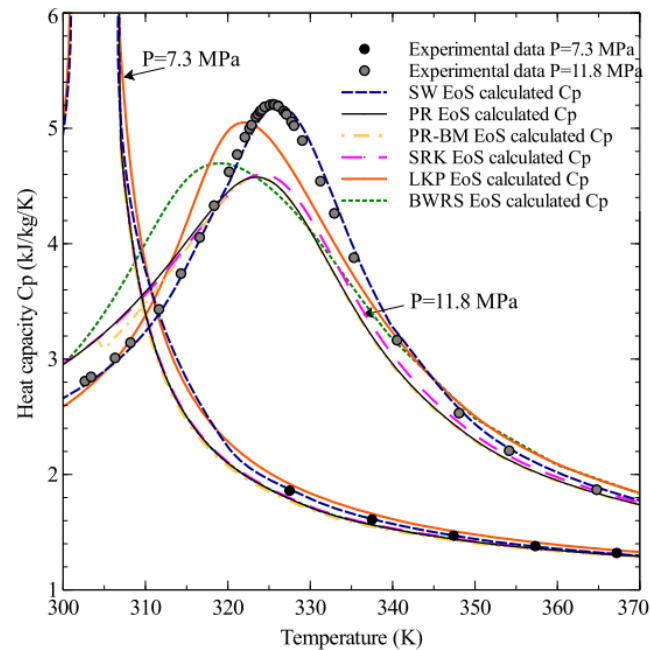


- Satisfactory agreement between  $\omega_{SW}$  EoS calculated and  $\omega_{experimental}$
- Parity curve with all accessed experimental data
- $\Delta \omega = 4.8\%$



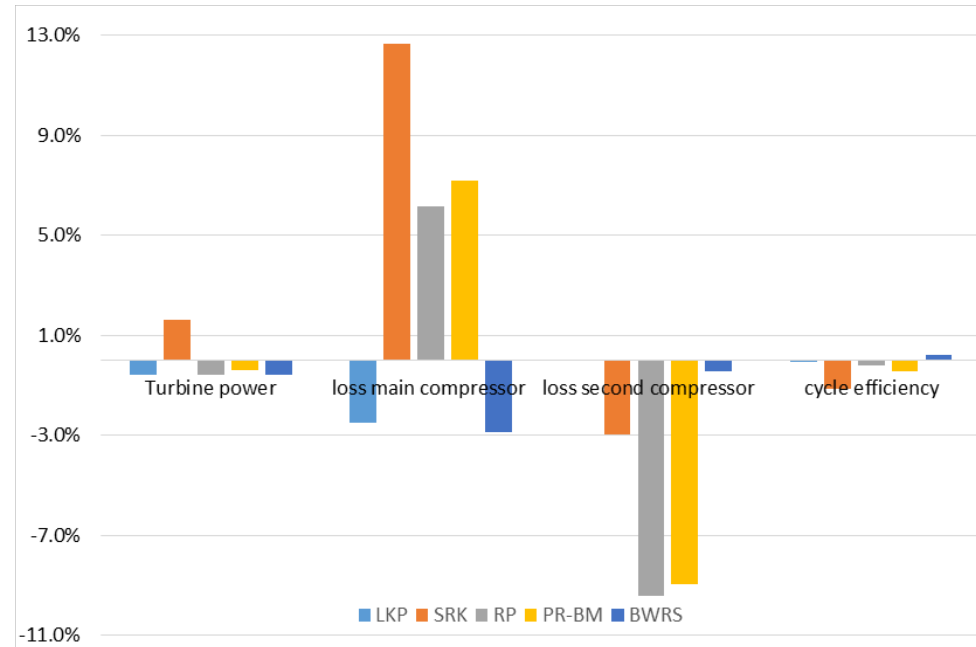
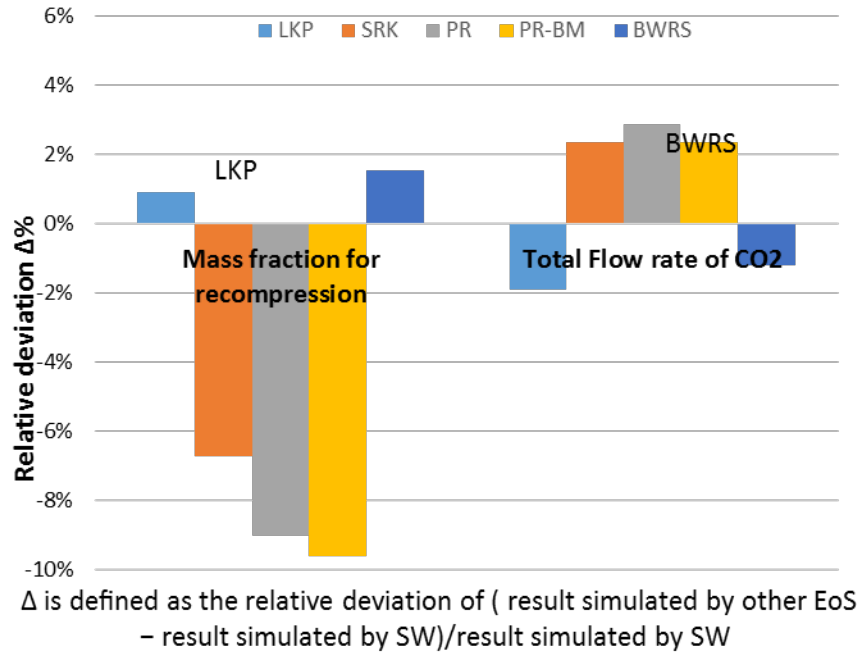
# BACK UP

## EoS IN ENTIRE REGION OF INTEREST

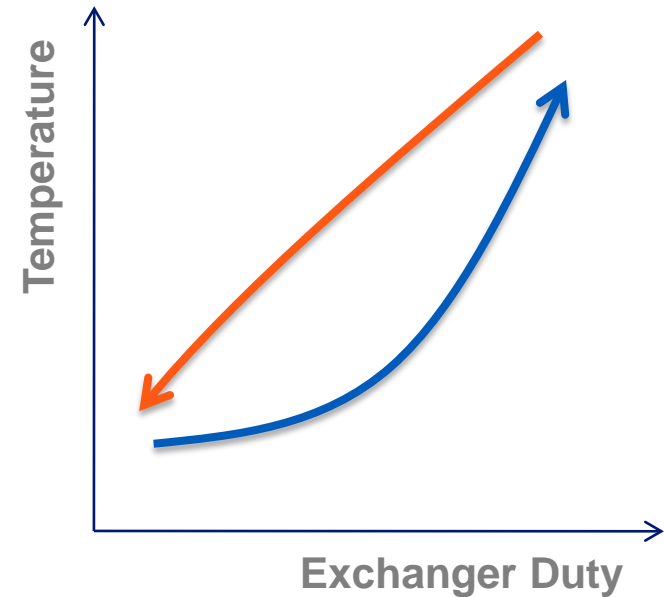
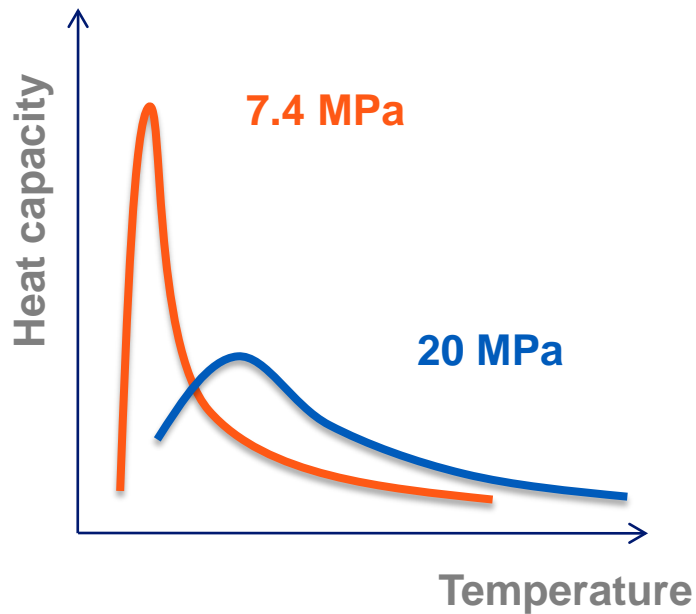
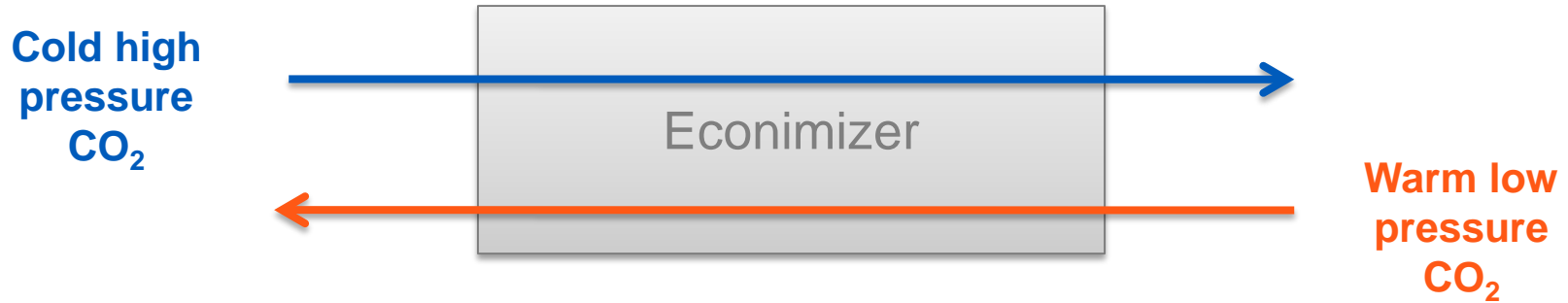


# BACK UP

## RRC BRAYTON CYCLE



# BACK UP ECONOMIZER PINCH PROBLEM



# BACK UP RESULTS – Cycle economizer configuration

- 3 studied cases (all other parameters being similar with reference case):
  - No recompression cycle
  - Single recompression cycle (ref. case)
  - Double recompression cycle
- Significant reduction of economizer temperature difference between heat and cold side
  - more heat is exchanged
  - cycle efficiency increases
- Double recompression cycle efficiency gains do not justify expected material additional costs

