

**Preliminary design study on a Multi-Megawatts  
Fossil-based Supercritical CO<sub>2</sub> Recompression and  
Reheat Integral Test Facility**

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- ◆ **Motivation**
- ◆ **What and Why is  $\text{SCO}_2$  Brayton Cycle**
- ◆ **Existing and Ongoing Integral Test Facility**
- ◆ **TPRI 5MWe Indirect  $\text{SCO}_2$  Integral Test Facility**
- ◆ **Turbomachinery Preliminary Design**
- ◆ **Heat Exchangers Preliminary Design**
- ◆ **Boiler Preliminary Design**
- ◆ **Conclusions**

# Motivation

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Advanced 620 °C Supercritical CO<sub>2</sub> Brayton Cycle  
28Mpa/620°C/620°C

**ASCBC at 620°C could achieve equivalent plant efficiency of SCW at 700 °C >50%?**

The most state of the art USCW coal based utility, ST600°C, **Plant efficiency 44.5%. How to improve?**

**Supercritical CO<sub>2</sub> Brayton Cycle**

**CSP and Nuclear high temperature sources; GTCC&IGCC bottoming cycle; Industrial Waste Heat recovery;**

Advanced 700 °C USCW  
36.65Mpa/700°C/720°C

Advanced 600 °C USCW with double Reheat  
33Mpa/600°C/620°C/620 °C

Advanced 600 °C USCW  
28Mpa/600°C/620°C

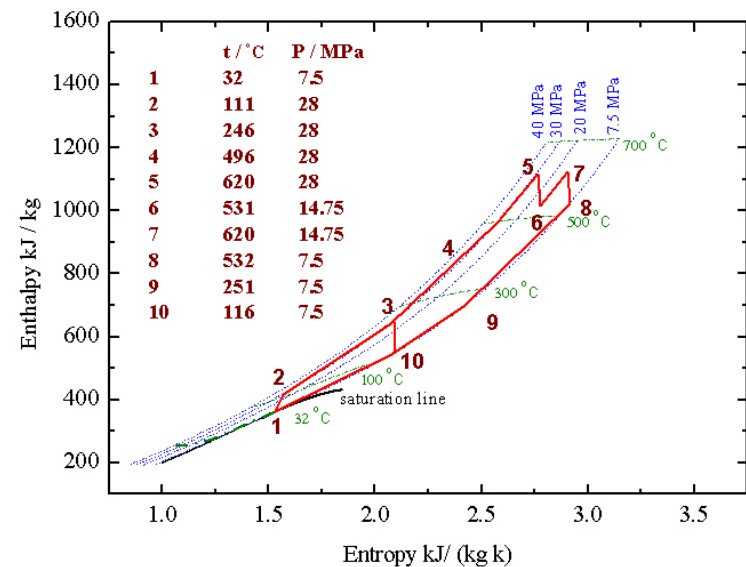
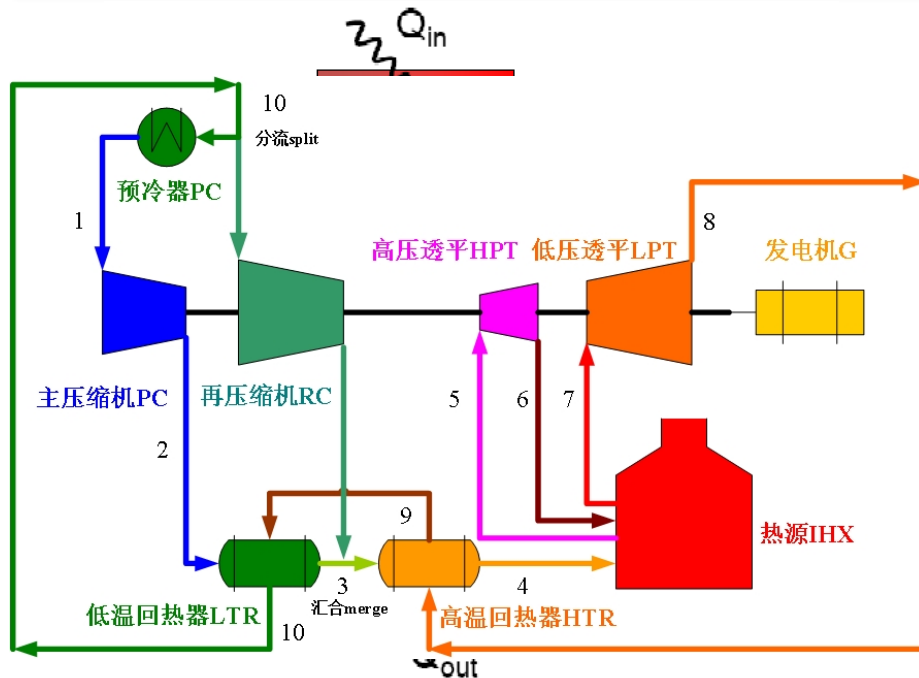
**Supercritical Steam Rankine Cycle**

**Nickel-based 700 °C Alloys**  
Capital and technology intensive; time-consuming ;  
Coupon tests failed in Europe layout of 700°C furnace and turbine.

# What is $\text{SCO}_2$ -Brayton Cycle?

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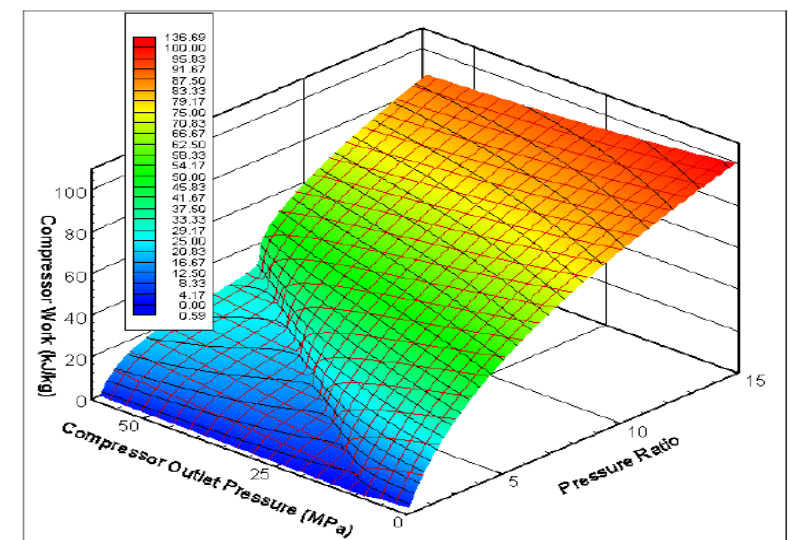
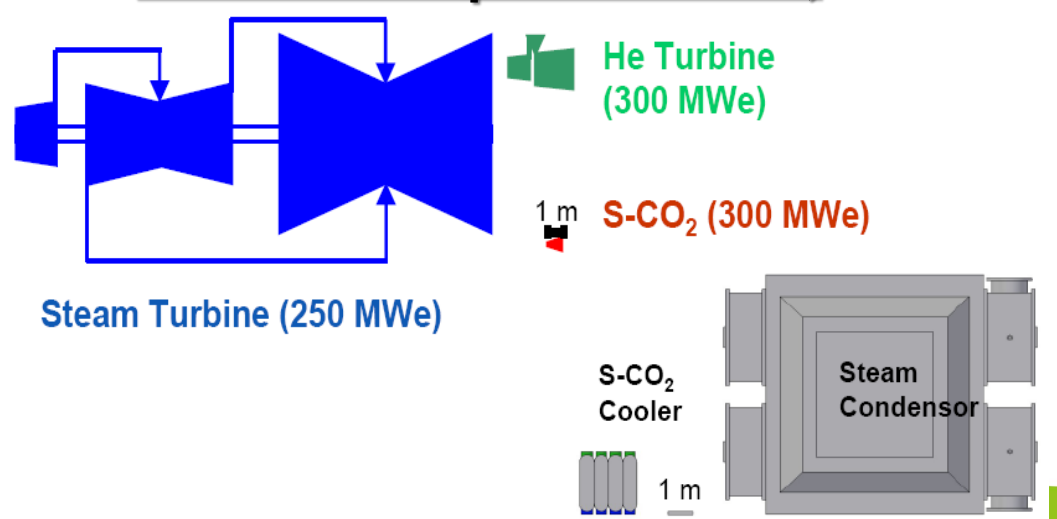
	Steam Rankine Cycle	IG Brayton Cycle	$\text{SCO}_2$ Brayton Cycle
Compress	Pump	Compressor	Compressor
Heating	Boiler	Combustion Chamber	IHX
Expand	Turbine	Gas turbine	$\text{SCO}_2$ turbine
Cooling	Condenser	Ambiance	Precooler / Recuperator



# Why $\text{SCO}_2$ ?

- ◆  **$\text{SCO}_2$  is an attractive working fluid**
  - moderate critical parameters  
7.29MPa, 30.98°C; accommodate a large range of temperatures;
  - **combined liquid and gas properties**  
**large density with relative low viscosity; condensed gas;**
  - less corrosive and environmentally friendly  
no need for water quality control and treatment support;
  - **higher power density**  
**significantly reduced component size,**
  - almost incompressible near critical point  
**reduced compressor work;**

## Why $\text{SCO}_2$ Can Displace Steam ?



# Why $\text{SCO}_2$ ?

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- ◆  **$\text{SCO}_2$  BC is a high efficiency and cost effective cycle**
  - high efficiency at moderate temperature  
Thermal efficiency > 50% possible @ 28MPa / 620 °C / 620 °C;
  - **no phase change**  
**simple cycle layout and small plant footprint;**
  - low pressure ratio and high power density  
small turbomachinery;
  - **High recuperative**  
**~2/3 of the cycle energy is recuperative heat;**

**Lower  
Capital cost**  
civil;  
equipment;  
installation;



**Lower  
O&M cost**  
fuel;  
personnel;  
Water treatment;



**Lower LCOE**  
15-20% off

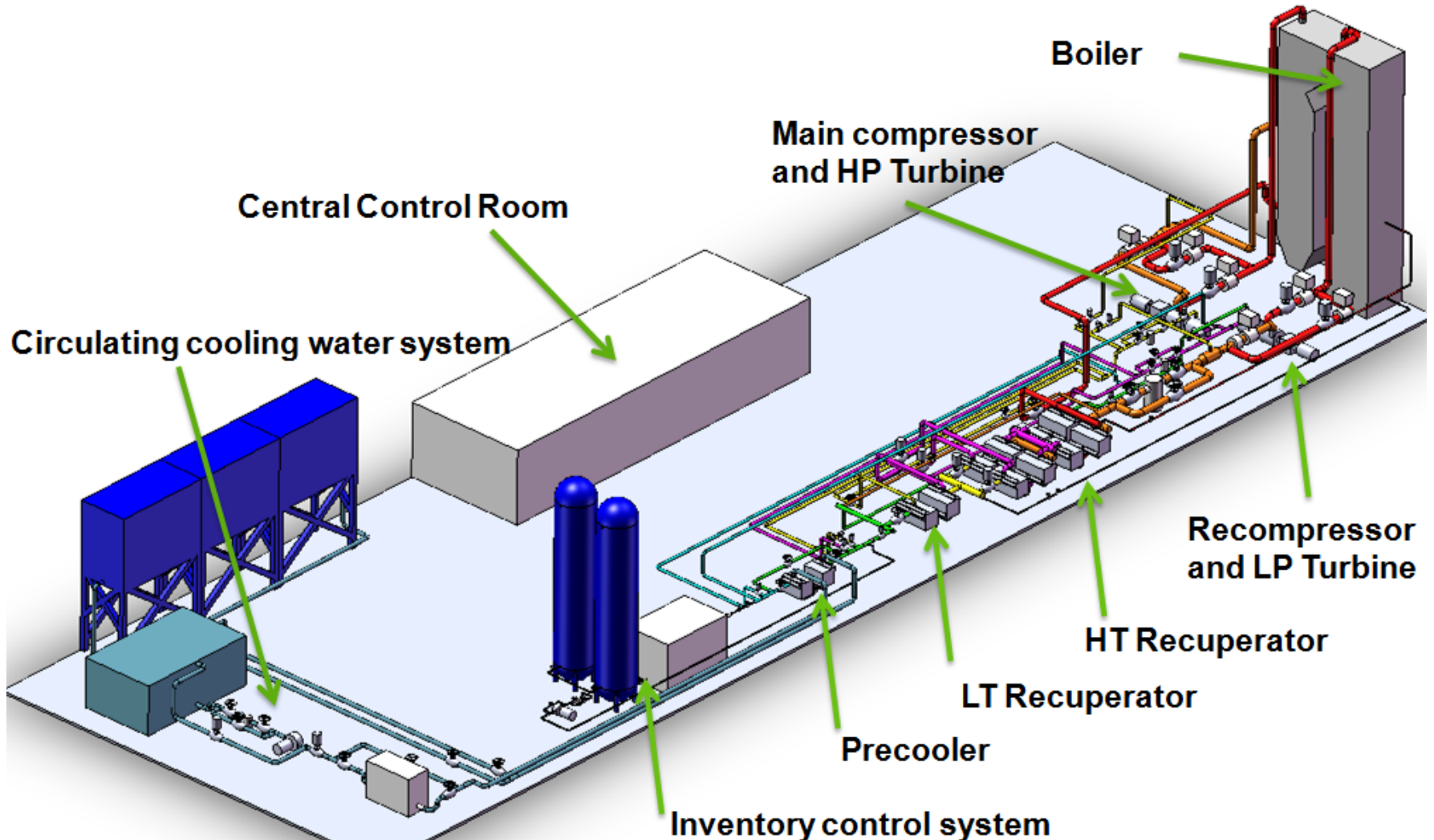
# Existing and Ongoing ITF

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1	<b>Sandia National Lab</b>	<b>7.68-13.84MPa; 32°C-342°C, 240kWe; 31.5%; 50000RPM; turbine efficiency 68%</b>
2	<b>Bechtel Marine Propulsion</b>	<b>9.03-13.5MPa; 36°C-299°C; 100kWe; cycle efficiency 14.7%; 60000RPM</b>
3	<b>Echogen</b>	<b>Waste heat 7MWe; TIT 275°C</b>
4	<b>Tokyo Institute Technology</b>	<b>30kWe small Test loop</b>
5	<b>DOE &amp; NREL &amp; SNL &amp; BNL &amp; UW &amp; Echogen &amp; EPRI &amp; AB SOLAR</b>	<b>CSP 10MWe; 8-28MPa; 45-700°C;</b>
6	<b>SWRI &amp; GE &amp; Thar Energy</b>	<b>1MWe simple loop;</b>
7	<b>KAIST/KAERI</b>	<b>33.2°C; 500°C; 7.78-20MPa</b>
8	<b>EDF/GE</b>	<b>20MWe coal based pilot plant</b>
9	<b>NetPower &amp; Toshiba</b>	<b>50MWe Allam cycle</b>

# TPRI 5MWe Integral Test Facility

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# System design

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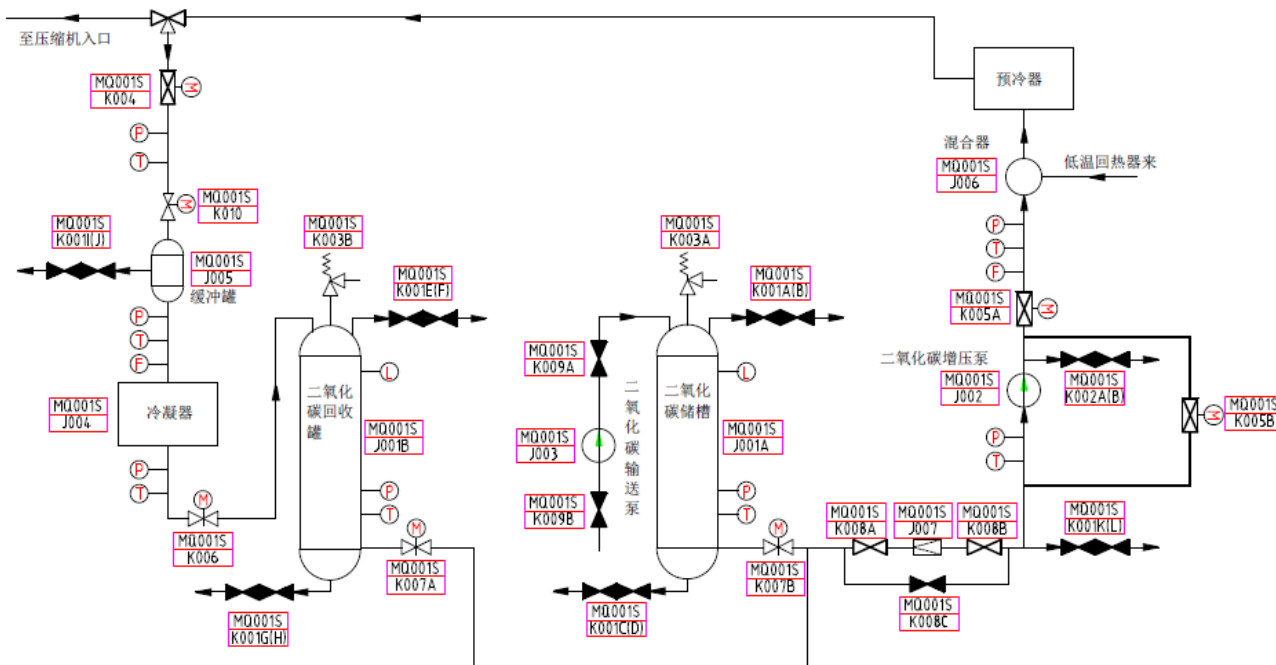
SR to Recompressor	/	0.384	HPT work	MW	4.687
SR to Economizer	/	0.08	LPT work	MW	4.75
HPT-IP	MPa	20	MC work	MW	1.588
HPT-IT	°C	600	RC work	MW	2.643
HP expansion ratio	/	1.527	Boiler duty	MW	14.557
LPT-IP	MPa	12.69	LTR duty	MW	12.011
LPT-IT	°C	600	HTR duty	MW	34.586
LP expansion ratio	/	1.527	PC duty	MW	9.351
MC-IP	MPa	7.6	Net capacity	MWe	5
MC-IT	°C	32	Boiler efficiency	%	94
MC PR	/	2.816	MC efficiency	%	70
RC-IP	MPa	7.71	RC efficiency	%	72
RC-IT	°C	80.085	LPT efficiency	%	82
RC PR	/	2.737	HPT efficiency	%	80
Mass Flow Rate	t/h	304.37	Cycle gross efficiency	%	32.29

# Inventory Control

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**Cryogenic storage for expansion tanks design widely used in industry**

**$P=2.16\text{MPa}$ ;  $T=-30^\circ\text{C}$ ;  $V=12\text{m}^3$**



# Turbomachinery

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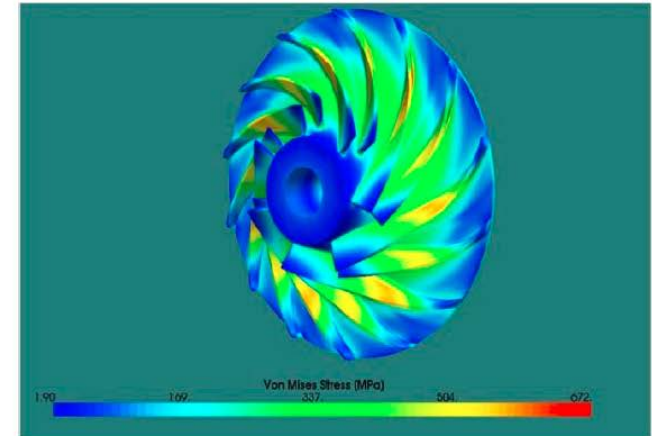
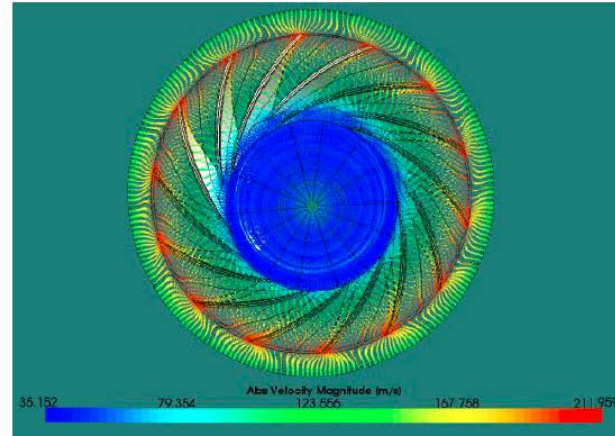
	Unit	MC	RC	HPT	LPT
mass flow rate	kg/s	52.08	32.47	84.55	84.55
work	MW	1.58	2.64	4.68	4.75
impeller diameter	mm	140	200	120	200
inlet pressure	MPa	7.6	7.7	20	12.7
inlet temperature	°C	32	80	600	600
inlet density	kg/m <sup>3</sup>	557.5	152.4	116.7	75.26
outlet pressure	MPa	21.4	21.1	13.09	8.31
outlet temperature	°C	70.1	187.3	551.3	551.1
outlet density	kg/m <sup>3</sup>	684.6	288.58	82.4	52.76
shaft speed	rpm	30000	30000	30000	30000
isentropic efficiency	%	70	72	80	82

# Turbomachinery

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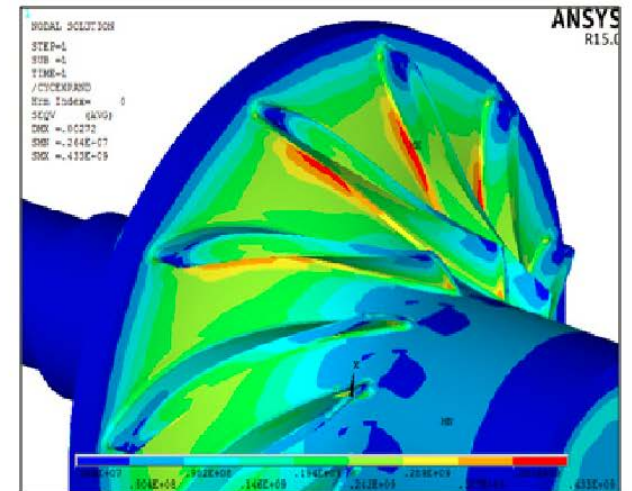
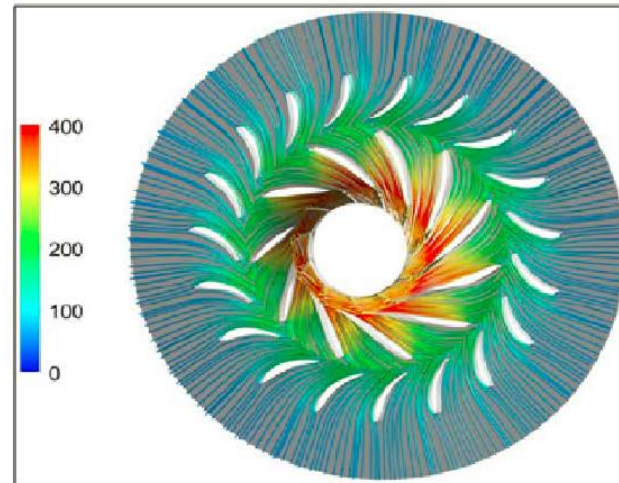
**Compressor:  
Titanium alloy**

**Max Von Mises  
stress is 622MPa**



**Turbine:  
Inconel 718**

**Max Von Mises  
stress is 433MPa**



# Recuperators and Precooler

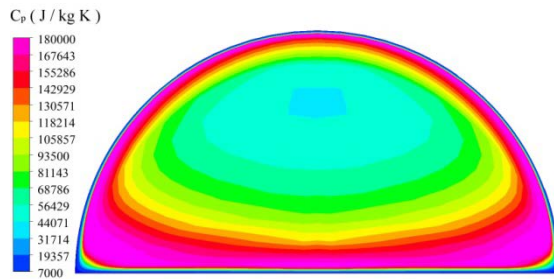
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		HT Recup		LT Recup		PC	
		Hot	Cold	Hot	Cold	Hot	Cold
heat duty	MW	34.58		12.01		9.5	
heat transfer area	m <sup>2</sup>	2460		837.4		360.59	
unit size	m	0.6×0.6×1.35		0.6×0.6×1.35		0.6×0.6×1.35	
number of unit	/	8		2		1	
U	W/(m <sup>2</sup> K)	978.6		1215.4		2463.6	
average DT	K	15.84		12.31		25.83	
Volume	m <sup>3</sup>	1.4		0.52		0.14	
Weight	t	38		10.6		2.25	
WF		CO2	CO2	CO2	CO2	CO2	H2O
MFR	kg/s	84.55	77.78	84.55	52.08	52.08	110
PI	MPa	8.31	21.1	8.01	21.4	7.71	0.2
PO	MPa	8.01	20.8	7.71	21.1	7.6	0.11
TI	°C	551.1	187.3	197.4	70.1	80.1	20
TO	°C	197.4	540.1	80.1	187.3	32	32.5

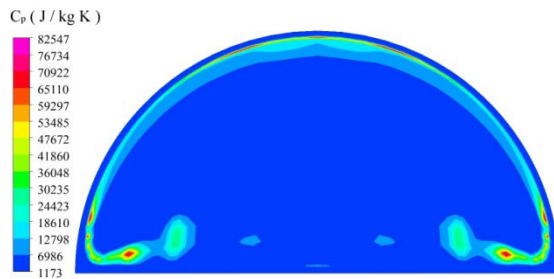
# SCO<sub>2</sub> heat transfer model

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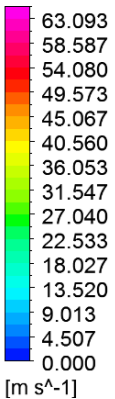
20 kW/m<sup>2</sup>



90 kW/m<sup>2</sup>



Velocity  
Contour 1



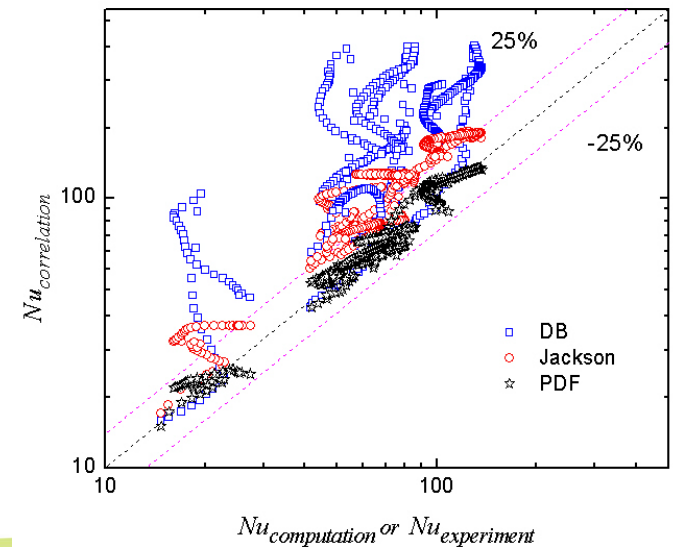
Acceleration effect  
“M-shaped” velocity profile



$$Nu_{b, pdf} = C Re_{b, pdf}^m Pr_{b, pdf}^n \left( \frac{\rho_{w, pdf}}{\rho_{b, pdf}} \right)^p \left( \frac{Cp_{pdf}}{Cp_{b, pdf}} \right)^q$$

	C	m	n	p	q
heating	0.0281	0.729	0.675	0.466	0.532
cooling	0.0937	0.627	0.608	0.203	0.522

$$\phi(T) = \frac{1}{\sqrt{2\pi\sigma^2}} e^{-\frac{(T-\bar{T})^2}{2\sigma^2}}$$



# Boiler

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		FWSH	FWRH	SH	RH	ECO	APH
Heat Duty	kW	4809	3983	1590	989	3005	1746
Heating surface Area	m <sup>2</sup>	39.6	32.8	63	89	315	1403
flue gas IT	°C			1012.7	854.6	733.8	351.1
flue gas OT	°C			854.6	733.8	351.1	118.7
CO <sub>2</sub> /air IT	°C	538.8	551.3	584.3	589.7	193.5	25
CO <sub>2</sub> /air OT	°C	584.3	589.7	600	600	538.7	290.8
flue gas velocity	m/s			14.89	13.27	12.57	10.7
CO <sub>2</sub> velocity	m/s			23.67	19.78	4.95	5.83
LMTD	°C			334.4	194.6	175.7	63.2
tube outside diameter	m	25	25	42	42	38	38
tube thickness	m	5	4	5	4	4	2
Outside wall temperature	°C	621	611	605	590	550	
volume	m <sup>3</sup>	0.212	0.225	0.384	0.612	1.865	/
weight	t	2.939	2.045	2.165	2.512	8.793	21.89

- **SCO<sub>2</sub> power conversion technology has been extensively investigated around the world due to its compact components, simple plant layouts and the potential to significantly increase the efficiency.**
- **The existing laboratory scale integral demonstration test loops well verified the concept of the SCO<sub>2</sub> power cycle. However there are numerous hurdles need to address before the commercial scale achieve the efficiency benefits and reliable operation.**
- **TPRI are planning to build a SCO<sub>2</sub> R&R power cycle test loop with larger capacity and higher parameters aiming at the utility scale coal-based power plant.**
- **The initial system modeling and scaling as well as the key components preliminary design has been made for 5MWe ITF. The whole project was expected to accomplish at the end of 2017.**



**Thanks for your  
attention!**

**Hongzhi Li, PhD.**

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